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3 **Title:** Production of polyhydroxybutyrate and alginate from glycerol by
4 *Azotobacter vinelandii* under nitrogen-free conditions

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6 **Running title:** Production of biopolymers from glycerol

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22
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25 **ABSTRACT**

26 Glycerol is an interesting feedstock for biomaterials such as biofuels and bioplastics
27 because of its abundance as a by-product during biodiesel production. Here we
28 demonstrate glycerol metabolism in the nitrogen-fixing species *Azotobacter vinelandii*
29 through metabolomics and nitrogen-free bacterial production of biopolymers, such as
30 poly-D-3-hydroxybutyrate (PHB) and alginate, from glycerol. Glycerol-3-phosphate was
31 accumulated in *A. vinelandii* cells grown on glycerol to the exponential phase, and its
32 level drastically decreased in the cells grown to the stationary growth phase. *A.*
33 *vinelandii* also overexpressed the glycerol-3-phosphate dehydrogenase gene when it
34 was grown on glycerol. These results indicate that glycerol was first converted to
35 glycerol-3-phosphate by glycerol kinase. Other molecules with industrial interests, such
36 as lactic acid and amino acids including γ -aminobutyric acid, have also been
37 accumulated in the bacterial cells grown on glycerol. Transmission electron microscopy
38 revealed that glycerol-grown *A. vinelandii* stored PHB within the cells. The PHB
39 production level reached 33% per dry cell weight in nitrogen-free glycerol medium.
40 When grown on glycerol, alginate-overproducing mutants generated through chemical
41 mutagenesis produced two-fold the amount of alginate from glycerol than the parental
42 wild-type strain. To the best of our knowledge, this is the first report on bacterial
43 production of biopolymers from glycerol without addition of any nitrogen source.

44

45

46 INTRODUCTION

47 *Azotobacter vinelandii* is a free living, nitrogen-fixing bacterium.^{1,2} One of the
48 remarkable characteristics of this species is that it can grow sufficiently in a
49 nitrogen-free minimal medium.³ In *A. vinelandii*, nitrogenases prerequisite for nitrogen
50 fixation catalyze the reduction of nitrogen to ammonia using a large amount of energy
51 derived from ATP hydrolysis.^{4,5} In the recently determined genome sequence of *A.*
52 *vinelandii*, three different types of nitrogenases have been identified.² In addition, it has
53 been established that *A. vinelandii* has the potential to produce industrially useful
54 biopolymers, including extracellular alginate and intracellular poly-D-3-hydroxybutyrate
55 (PHB).⁶⁻⁹ Alginate is a linear polysaccharide consisting of (1-4)- β -D-mannuronic acid
56 and α -L-guluronic acid. Commercially available alginate is classically derived from
57 seaweed, although two bacterial genera, *Pseudomonas* and *Azotobacter*, are expected to
58 be potential alginate producers.⁸ PHB belongs to the polyhydroxyalkanoate (PHA)
59 family of polyesters, and many bacterial species accumulate PHAs as intracellular
60 granules for energy storage.¹⁰ PHAs are also promising alternatives to plastics because
61 of their biodegradability, biocompatibility, and thermoplasticity.^{6,11} Hence, *A. vinelandii*
62 is considered to be an attractive bacterium for production of two industrially useful
63 biopolymers, alginate and PHB, in the absence of nitrogen sources.^{6,9,12-14}

64 The biosynthetic pathways for alginate and PHB production in *A. vinelandii* have
65 previously been reviewed by Galindo *et al.*⁶ As shown in Fig. 1, alginate is synthesized
66 from fructose 6-phosphate by many enzymes encoded by the *alg* cluster,^{8,15} whereas
67 PHB is synthesized in three steps from acetyl-CoA and three *phb* genes are essential for
68 synthesis.¹⁶ The regulatory mechanisms for the production of these biopolymers have
69 been analyzed.¹⁶⁻²⁵ Thus, the biopolymers are expected to be produced from excess

70 and/or unused resource by *A. vinelandii*.

71 *A. vinelandii* is known to assimilate various carbon sources. Sucrose, glucose,
72 fructose, mannose, sorbitol, mannitol, glycerol, gluconate, and acetate can all be used as
73 the sole carbon source for cell growth.^{26,27} Furthermore, some of them are also used for
74 biopolymer production.²⁶ However, little information exists on bacterial glycerol
75 metabolism including biopolymer production in a nitrogen-free environment. Glycerol
76 is generated as a major by-product during biodiesel production, and its efficient
77 utilization is now sought in various areas of food, pharmaceutical, agricultural, and
78 environmental research. Moreover, microorganism-mediated conversion of glycerol to
79 other valuable materials is being developed worldwide. Production of hydrogen, ethanol,
80 butanol, 1,3-propanediol, propionic acid, and PHAs has previously been undertaken
81 using bacteria.^{28,29}

82 To the best of our knowledge, no report exists on glycerol utilization in a
83 nitrogen-free environment. Moreover, glycerol metabolism and production of
84 biopolymers from glycerol in *A. vinelandii* remain to be clarified. The present study
85 involves metabolomics-based identification of the glycerol metabolic pathway in *A.*
86 *vinelandii* and the bacterial production of biopolymers from glycerol in a nitrogen-free
87 environment.

88

89 **RESULTS AND DISCUSSION**

90 **Sucrose and glycerol metabolism.** Metabolites in *A. vinelandii* cells grown on sucrose
91 or glycerol were analyzed by a capillary electrophoresis time-of-flight mass
92 spectrometry (CE-TOFMS) (Tables 1 and 2). Small amounts of glucose-, fructose-, and
93 glycerol-related metabolites, but not glycerol-3-phosphate accumulated in the cells

94 (Table 1). Considerable amounts (400 pmol/OD₆₀₀ ml) of glycerol-3-phosphate were
95 detected in the glycerol-grown cells collected at the exponential growth phase, whereas
96 its level drastically decreased (82 pmol/OD₆₀₀ ml) in cells collected at the stationary
97 growth phase. Moreover, the dihydroxyacetone phosphate level in the glycerol-grown
98 cells was much higher than that in the sucrose-grown cells. These results suggest that
99 glycerol was first catabolized to glycerol-3-phosphate, then to dihydroxyacetone
100 phosphate, and finally converged into the glycolytic pathway. Because cell growth on
101 glycerol was slower than that on sucrose as described later, accumulation of
102 glycerol-3-phosphate was considered to be a rate-limiting step.

103 In the recently determined genome sequence of *A. vinelandii* strain DJ,² putative
104 genes for glycerol uptake and degradation were found at a locus containing four genes,
105 *glpF*, *glpK*, *glpR*, and *glpD*. GlpF and GlpR are annotated as putative glycerol-uptake
106 and -repressor proteins, respectively, whereas GlpK and GlpD are annotated as glycerol
107 kinase and glycerol-3-phosphate dehydrogenase, respectively. Although GlpK and GlpD
108 are classified into a group involved in phospholipid metabolism according to genome
109 annotation, metabolomics in the present study demonstrated that glycerol and
110 glycerol-3-phosphate were substrates of GlpK and GlpD, respectively, and that both
111 enzymes were necessary for glycerol metabolism.

112 Two pathways were postulated for the conversion of glycerol to dihydroxyacetone
113 phosphate. One is through glycerol-3-phosphate and the other through dihydroxyacetone.
114 A number of microorganisms can use glycerol as the sole carbon source through
115 dihydroxyacetone.²⁹⁻³¹ Furthermore, the genome sequence of *A. vinelandii* revealed the
116 presence of glycerol dehydrogenase- and dihydroxyacetone kinase-like genes (Fig. 1).
117 Hence, a dehydrogenase for glycerol and one for glycerol-3-phosphate were assayed to

118 determine the main glycerol assimilation pathway. However, no activity of either
119 enzyme was detected in the bacterial cell extract, possibly due to their low protein
120 expression level. Hence, transcription levels of the genes of the two dehydrogenases
121 were monitored by quantitative PCR (Fig. 2). As shown in Fig. 2A, the total RNA of
122 bacteria grown in all conditions was extracted without degradation. In the case of the
123 glycerol-3-phosphate dehydrogenase gene (Fig. 2B left), the cells grown to the
124 exponential growth phase showed higher gene expression than those grown to the
125 stationary growth phase. In bacteria grown to the exponential growth phase, gene
126 expression in the glycerol medium was 38-fold higher than that of bacteria grown in the
127 sucrose medium. In contrast, the glycerol dehydrogenase gene was transcribed at basal
128 levels in bacteria grown to the exponential growth phase in media (Fig. 2B right). The
129 expression of glycerol dehydrogenase in all cases tested was extremely low, but near the
130 detectable limit for our experimental conditions (data not shown). These metabolomic
131 and quantitative PCR results demonstrate that the glycerol-3-phosphate pathway is
132 predominant in *A. vinelandii*.

133 Sucrose metabolites, such as fructose 6-phosphate, mannose 6-phosphate, mannose
134 1-phosphate, and GDP mannose, were detected even in glycerol-grown *A. vinelandii*
135 (Table 1). This result indicates that gluconeogenesis, which involves the conversion of
136 fructose 1,6-biphosphate to fructose 6-phosphate, occurred in the bacteria. In addition,
137 occurrence of gluconeogenesis in *A. vinelandii* demonstrates its potential for producing
138 alginate concomitantly with PHB from glycerol, which is described later.

139 No conspicuous rate-limiting metabolites were identified between fructose
140 1,6-biphosphate and acetyl CoA (Table 1). However, accumulation of pyruvic acid (42.5
141 pmol/OD₆₀₀ ml) was observed in glycerol-grown cells collected at the exponential

142 growth phase. Pyruvic acid is an important precursor for many metabolites, including
143 ethanol, acetyl CoA, and lactic acid.³² In the present study, *A. vinelandii* produced large
144 amounts of lactic acid in all cases, especially in glycerol-grown cells (Table 2), and
145 levels of several amino acids accumulated in glycerol-grown cells were higher than
146 those in sucrose-grown cells. Both glutamine and glutamic acid were considerably
147 produced in all cases, especially in glycerol-grown cells collected at the exponential
148 growth phase. Arginine, lysine, and proline are synthesized from glutamic acid in most
149 bacteria. A similar accumulation profile of these amino acids was observed in *A.*
150 *vinelandii*, as shown in Table 2. Thus, *A. vinelandii* demonstrated the potential for
151 amino acid production under nitrogen-free conditions. Furthermore, γ -aminobutyric acid
152 (GABA), a neurotransmitter of clinical interest,³³ was stored in the cells grown to the
153 exponential growth phase in sucrose and glycerol. Because bacteria-produced GABA is
154 known as a molecule of intracellular pH management due to decarboxylation of
155 glutamic acid,³⁴ this molecule is suggested to play an important role in the
156 neutralization of organic acids accumulated in the cells.

157 Metabolomic analysis performed in the present study supported the role of the
158 metabolic pathway predicted previously, as shown in Fig. 1. In addition, based on
159 results of the present study, *A. vinelandii* is promising as a potential producer of many
160 useful materials, such as amino acids, GABA, lactic acid, and biopolymers, in a
161 nitrogen-free environment.

162

163 **PHB production.** PHB accumulation was investigated in wild-type (WT) *A. vinelandii*
164 grown on sucrose or glycerol. In addition, the mutant $\Delta algD$ cells, which have a
165 disrupted alginate synthetic gene *algD*, were also subjected to the PHB assay because

166 PHB and alginate productions are thought to be competitive. First, intracellular PHB
167 granules were monitored by transmission electron microscopy (TEM) (Fig. 3). Similar
168 to many PHB-producing bacteria, WT cells produced white and globular PHB granules,
169 which were found in both sucrose- and glycerol-grown cells. On the other hand,
170 globular PHB granules were scarcely observed and apparently degraded in $\Delta algD$ cells.

171 The time course of cell growth and PHB production are shown in Fig. 4. In the
172 sucrose medium, WT and $\Delta algD$ cells showed similar growth profiles (Fig. 4A). Cell
173 growth of both strains exceeded an OD₆₀₀ of 14. However, the lag phase of both strains
174 grown on glycerol was longer than that on sucrose. WT growth reached an OD₆₀₀ of
175 6.12, whereas that of $\Delta algD$ reached an OD₆₀₀ of 16.8.

176 Figure 4B indicates the time course of intracellular PHB accumulation (per dry cell).
177 The intracellular PHB level in WT cells grown on sucrose as well as glycerol reached
178 approximately 33%. Interestingly, the PHB level of $\Delta algD$ cells grown on either source
179 initially increased, but subsequently decreased. As shown in Fig. 4A, PHB was
180 degraded in $\Delta algD$ cells. *A. vinelandii* is known to convert from vegetative cells to cysts
181 under unfavorable environments for growth, and PHB has been observed in the
182 cyst-forming cells as a probable energy and carbon storage material.¹⁴ Although the
183 reasons for PHB degradation have yet to be determined, the necessity for PHB might
184 waver due to the lack of alginate production following cyst formation. Production of
185 PHB and alginate is closely regulated in *A. vinelandii*.¹⁰ The results obtained herein may
186 provide valuable hints on the relationships among alginate, PHB, and cyst formation.

187 Although *A. vinelandii* grown on glucose together with nitrogen sources synthesizes
188 much PHB (74% per dry cell),³⁵ and some bacteria such as *Burkholderia cepacia*,³⁶
189 *Chelatococcus daeguensis*,³⁷ *Cupriavidus necator* (formerly *Ralstonia eutropha*),^{38,39}

190 *Paracoccus denitrificans*,⁴⁰ *Pseudomonas oleovorans*,⁴¹ and *Zobellella denitrificans*,⁴²
191 have also been known to produce PHB from glycerol with nitrogen sources, the
192 bacterial production of PHB from glycerol without a nitrogen source contributes to
193 green chemistry.

194

195 **Alginate production.** The alginate production level was determined in *A. vinelandii*
196 grown on sucrose or glycerol. The sucrose-grown cells obtained at the stationary phase
197 produced alginate at 0.3–0.4 mg/ml, whereas those grown in the glycerol medium
198 produced enhanced levels of approximately 0.5 mg/ml. To elevate the alginate
199 production level, a random NTG-treated mutation library was used to screen
200 alginate-overproducing mutants. Unlike for PHB, it was easy to select
201 alginate-overproducing mutants because these mutants seemed to form high mucoid
202 colonies. More than 100 mutants were isolated as high mucoid colonies in comparison
203 with WT colonies.

204 One of the mutants (MT1) was subjected to TEM analysis after preparation of cell
205 thin section (Fig. 5A). Recently, *A. vinelandii* cells were demonstrated to be equipped
206 with a special secretion system for alginate through formation of cell-surface blebs.
207 These blebs containing alginate are formed on the bacterial cell surface and are
208 subsequently released around the cells.⁴³ MT1 cells formed a large number of blebs on
209 the cell surface (Fig. 5A). On the other hand, few blebs were observed on WT cells (Fig.
210 5B). Thus, WT cells were subjected to scanning electron microscopy (SEM) analysis. A
211 few blebs were observed on the cell surface (Fig. 5C). The time course of alginate
212 secretion for WT and MT1 cells grown on glycerol is characterized in Fig. 6. Cell
213 growth (3.97 at OD₆₀₀) of MT1 at 96 h was lower than that (6.64 at OD₆₀₀) of WT (Fig.

214 6A). In contrast, alginate secretion by MT1 cells (0.87 mg/ml) was higher than that by
215 WT cells (0.52 mg/ml) (Fig. 6B). This result indicates that MT1 cells have the potential
216 for more alginate production through improvement in their growth conditions.

217 In conclusion, this is the first report on glycerol metabolism in *A. vinelandii* analyzed
218 through the metabolomic approach. The results indicate that *A. vinelandii* grown on
219 glycerol, but in the absence of any nitrogen source, may be useful for producing many
220 substances, including amino acids and biopolymers (especially PHB and alginate), with
221 industrial interests.

222

223 MATERIALS AND METHODS

224 **Bacteria and culture conditions.** The bacterial strains used in the present study are
225 listed in Table 3. Cells of WT *A. vinelandii* ATCC 12837 and an alginate-deficient
226 mutant with a disruption of *algD* ($\Delta algD$)⁴³ were grown aerobically in a minimal
227 glycerol medium, i.e., modified Burk's medium (G-MB; 20 mg/ml glycerol, 200 µg/ml
228 NaCl, 50 µg/ml CaSO₄, 200 µg/ml MgSO₄ 7H₂O, 2.9 µg/ml Na₂MoO₄ 2H₂O, 27 µg/ml
229 FeCl₃, 0.66 mg/ml K₂HPO₄, and 0.16 mg/ml KH₂PO₄) at 30°C with agitation of 120
230 strokes per min. Sucrose (20 mg/ml) was also used for a carbon source instead of
231 glycerol in G-MB (S-MB).

232

233 **Metabolome analysis.** Metabolome analysis was supported by Human Metabolome
234 Technologies (Tsuruoka, Japan). Precultured WT cells were inoculated in 50 ml fresh
235 S-MB or G-MB, and grown to the exponential or stationary growth phase. To reach the
236 stationary growth phase, cells were grown in each medium for 84 h. To reach the
237 exponential growth phase, cells were grown in S-MB and G-MB for 40 and 60 h

238 (approximately 1.2 at OD₆₀₀), respectively. The cells were harvested by centrifugation
239 (5700 ×g, 4°C, 5 min), and were washed twice with 10 ml pure water. Each cell pellet
240 was homogenized in 2 ml methanol. After homogenization, chloroform (1.6 ml) was
241 added to 1.6 ml of cell extract, and the mixture was well agitated. Aqueous and
242 chloroform layers were separated by centrifugation (2300 ×g, 4°C, 5 min), and the
243 aqueous layer was subjected to ultrafiltration (9100 ×g, 4°C, 120 min) using the
244 Ultrafree-MC UFC3 LCC (molecular weight cut-off, 5000; Millipore, Bedford, MA).
245 The filtrate was dried and resolved in 50 µl of pure water. Metabolites were identified
246 and quantified using CE-TOFMS system (Agilent Technologies, Santa Clara, CA).

247

248 **Enzyme assay.** Dehydrogenases for glycerol and glycerol-3-phosphate were assayed
249 according to a previously described method.⁴⁴ Briefly, WT cells were inoculated in 50
250 ml of fresh S-MB or G-MB, and cultured to the exponential or stationary growth phase.
251 The cells were washed twice with 10 mM potassium phosphate buffer (pH 7.0), and
252 resuspended in 2 ml of the same buffer. The cells were ultrasonically disrupted at 4°C
253 and 9 kHz for 10 min (Insonator model 201M; Kubota, Tokyo, Japan). Insoluble
254 substances were removed by centrifugation (20,000 ×g, 4°C, 15 min), and the
255 supernatant was used as the cell extract for analysis. The cell extract (20 µl) was mixed
256 with 10 mM (final concentration) potassium phosphate buffer (pH 7.0), 5 mM substrate
257 (glycerol or glycerol-3-phosphate), and 0.5 mM coenzyme (NAD⁺ or NADP⁺). The
258 change in the absorbance of the reaction mixture at a wavelength of 340 nm was
259 monitored at 30°C for 10 min.

260

261 **Quantitative PCR.** Total RNA extraction, *in vitro* cDNA synthesis, and quantitative

262 PCR were performed to monitor the expression levels of specific genes in the bacterial
263 samples. *A. vinelandii* grown in S-MB or G-MB was harvested at the exponential and
264 stationary growth phases. Total RNA was extracted using the standard hot phenol
265 method. DNA degradation and subsequent RNA purification were performed using the
266 RNase-Free DNase Set (Qiagen, Tokyo, Japan) and an RNeasy Mini Kit (Qiagen),
267 respectively. cDNA, synthesized from a 200 ng RNA sample as using the ReverTra Ace
268 qPCR RT Kit (Toyobo, Osaka, Japan) according to the manufacturer's instructions, was
269 used as a template. Quantitative PCR was performed using the SYBR Premix Ex Taq
270 GC (Takara Bio, Shiga, Japan) and the LineGene instrument (Toyobo).

271

272 **Electron microscopy.** TEM and SEM analyses were entrusted to Tokai Electron
273 Eicroscopy Analysis Co. (Nagoya, Japan). *A. vinelandii* was grown in S-MB or G-MB
274 media (30 ml of working volume) for 72 h. In the case of TEM analysis, the culture and
275 fixing solution A (2% paraformaldehyde, 2% glutaraldehyde, and 0.1 M potassium
276 phosphate buffer, pH 7.4) were mixed in a ratio of 1:1 (total 1 ml), and stored at 4°C for
277 60 min. Cell pellets were collected by centrifugation (5000 ×g, 4°C, 5 min). Fixing
278 solution B (2% osmium tetroxide and 0.1 M potassium phosphate buffer, pH 7.4) was
279 added to each cell pellet and agitated. Preparation of an ultrathin section and TEM
280 analysis using a JEM-1200EX instrument (JEOL, Tokyo, Japan) were carried out as
281 described previously.⁴³ In the case of SEM analysis, the bacterial cells were prefixed at
282 4°C for 1 h by mixing the culture with an equal volume of fixative consisting of 4%
283 paraformaldehyde and 4% glutaraldehyde in 100 mM cacodylate buffer (pH 7.4). After
284 centrifugation, the bacterial cells were fixed at 4°C for 24 h with 2% glutaraldehyde in
285 0.1 M cacodylate buffer (pH 7.4), additionally fixed at 4°C for 2 h with 1% tannic acid

286 in 0.1 M cacodylate buffer (pH 7.4), and washed at 4°C with the same buffer. The fixed
287 cells were treated at 4°C for 3 h with 2% OsO₄ in 0.1 M cacodylate buffer (pH 7.4) and
288 dehydrated in a series of ethanol (50%, 70%, 90%, and 100%, each 30 min). After
289 dehydration, the cells were continuously dehydrated with 100% ethanol at room
290 temperature overnight. The cells were substituted into tert-butyl alcohol at room
291 temperature, followed by freeze drying under vacuum. The cells were coated with a thin
292 layer (60 nm) of osmium by an osmium plasma coater (NL-OPC80NS, Nippon Laser &
293 Electronics Laboratory, Nagoya, Japan). The cells were observed using a scanning
294 electron microscope (JSM-6340F, JEOL, Tokyo, Japan) at an acceleration voltage of 5.0
295 kV.

296

297 **PHB detection.** Intracellular PHB was detected according to a previously described
298 procedure with slight modification.^{45,46} Dried cells were treated at 100°C for 140 min
299 with 1 ml chloroform containing 0.5% (w/v) benzoic acid as an internal standard and 1
300 ml methanol containing 3% sulfuric acid. After addition of 1 ml distilled water, each
301 solution was agitated for 1 min and centrifuged (1000 ×g, 4°C, 5 min). The lower
302 organic solvent layer of each sample was subjected to gas chromatography (GC)
303 analysis using a GC-2014 instrument (Shimadzu, Kyoto, Japan) and a DB-5 column (30
304 m × 0.25 mm × 0.25 μm; Agilent Technologies). Helium was used as the carrier gas.
305 Detector and injector temperatures were set to 275 and 230°C, respectively. Initial and
306 end temperatures were set to 60 and 200°C, respectively, with a gradient of 8°C/min. An
307 authentic sample of PHB (Sigma, St. Louis, MO) was also treated as described above
308 and was used for the identification and quantitative determination of PHB.

309

310 **Isolation of alginate-overproducing mutant.** *A. vinelandii* was grown in G-MB to the
311 exponential growth phase (approximately 0.8 at OD₆₀₀), and the harvested cells
312 obtained by centrifugation were washed with MB buffer (i.e., MB without a carbon
313 source). To create random mutation in the species, the cells were treated with 50 µg/ml
314 *N*-methyl-*N'*-nitro-*N*-nitrosoguanidine (NTG; Sigma) at 30°C for 30 min. The NTG
315 solution was removed from the sample by centrifugation, and the cells were incubated
316 overnight in S-MB. After colony formation on an S-MB plate, the highly mucoid cells
317 were selected as candidates for alginate-overproducing mutants.

318

319 **Alginate assay.** Alginate was assayed according to the method of Knutson and Jeanes.⁴⁷
320 Briefly, the culture broth (200 µl) was mixed with 0.5 M EDTA (12 µl) and 5 M NaCl (4
321 µl). Cells were removed from the mixture by centrifugation (7000 ×g, room temperature,
322 5 min). The supernatant (87.5 µl) was mixed with an ice-chilled mixture of sulfuric acid
323 (732.5 µl) and boric acid solution (17.5 µl; 45 mM KOH and 1 M boric acid) as well as
324 0.1% (w/v) carbazol (25 µl). The mixture was incubated at 55°C for 30 min, and its
325 absorbance 530 nm was subsequently measured. The alginate concentration in the
326 culture broth was determined based on the calibration using seaweed alginate as a
327 standard.

328

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334

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1 **FIGURE LEGENDS**

2 **Figure 1.** Putative synthetic pathway for PHB and alginate from glycerol in *A.*
3 *vinelandii*. The genes involved in glycerol metabolism are also indicated.

4

5 **Figure 2.** Gene expression of glycerol-3-phosphate and glycerol dehydrogenases. (A)
6 Total RNA from *A. vinelandii* grown in G-MB or S-MB to the exponential and
7 stationary growth phases. (B) Relative gene expression of glycerol-3-phosphate (left)
8 and glycerol dehydrogenases (right). For quantitative PCR, cDNA synthesized from was
9 used as a template in all samples. The expression levels of both genes in S-MB at the
10 stationary phase were standardized as the relative expression of 1.

11

12 **Figure 3.** PHB granules in *A. vinelandii* cells revealed by TEM. Bacteria were cultured
13 for 72 h in S-MB or G-MB as indicated.

14

15 **Figure 4.** Time course of PHB production by *A. vinelandii*. (A) Cell growth. (B) PHB
16 accumulation in dry cells. Open circles, WT grown on sucrose; closed circles, WT
17 grown on glycerol; open triangles, $\Delta algD$ grown on sucrose; closed triangles, $\Delta algD$
18 grown on glycerol.

19

20 **Figure 5.** Alginate-overproducing mutants of *A. vinelandii*. (A) TEM observation of
21 MT1 cells grown on glycerol. (B) TEM observation of WT cells grown on glycerol. (C)
22 SEM observation of WT cells grown on glycerol. Panels A' B', and C' are magnified
23 views of the regions of interest indicated in panels A, B, and C, respectively.

24

- 1 **Figure 6.** Alginate production from glycerol-grown *A. vinelandii*. (A) Cell growth. (B)
- 2 Extracellular alginate. Circles, WT; triangles, alginate-overproducing mutant.
- 3

Figure 1.

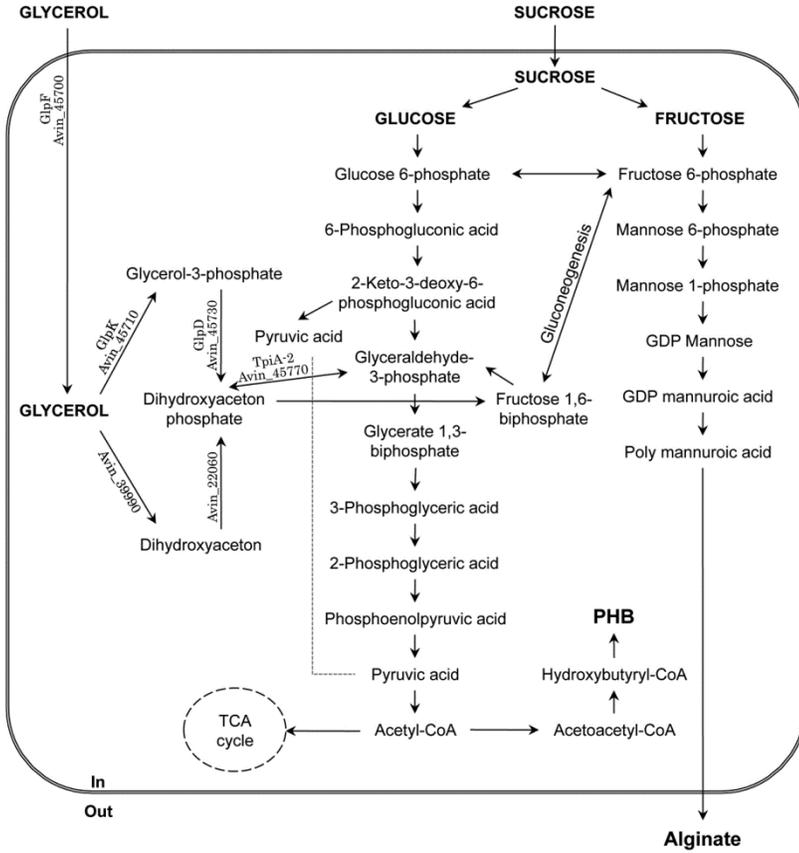


Figure 2.

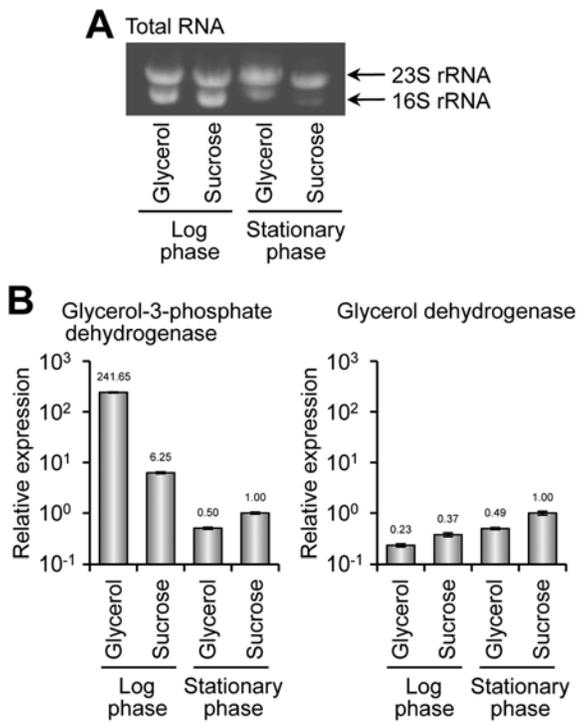


Figure 3.

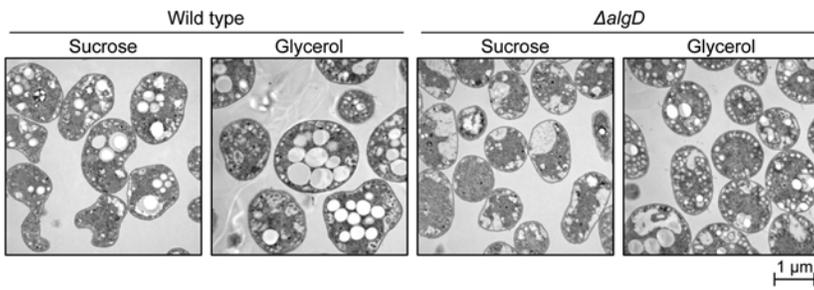


Figure 4.

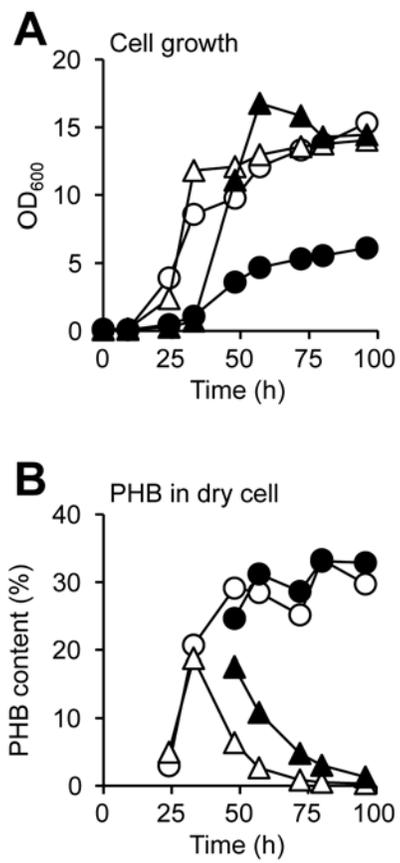


Figure 5.

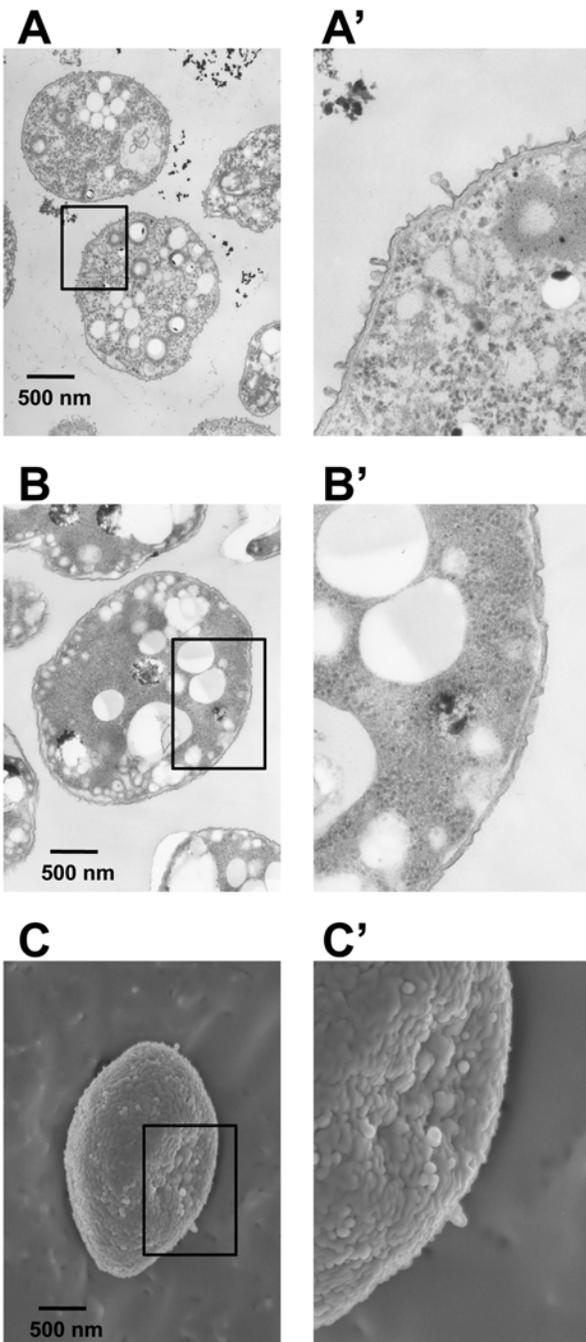
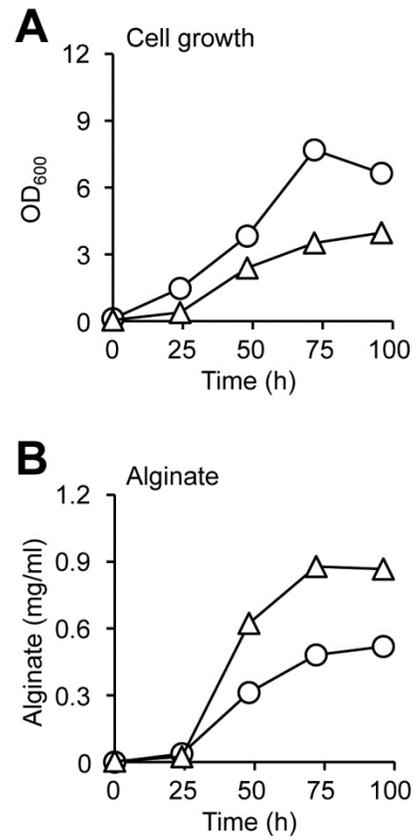


Figure 6.



1 Table 1. Intracellular metabolites determined through metabolomics.

Metabolite	Concentration (pmol/OD ₆₀₀ ml)			
	Sucrose		Glycerol	
	Log phase	Stationary phase	Log phase	Stationary phase
Glucose 6-phosphate ^{*1}	18.7 (±4.2)	22.5 (±29.3)	22.6 (±5.2)	61.0 (±25.4)
6-Phosphogluconic acid	U. L.	U. L.	U. L.	U. L.
2-Keto-3-deoxy-6-phosphogluconic acid	N. D.	N. D.	N. D.	N. D.
Fructose 6-phosphate ^{*2}	8.3 (±1.7)	8.2 (±11.6)	13.9 (±6.3)	29.4 (±13.1)
Mannose 6-phosphate ^{*1}	18.7 (±4.2)	22.5 (±29.3)	22.6 (±5.2)	61.0 (±25.4)
Mannose 1-phosphate ^{*2}	8.3 (±1.7)	8.2 (±11.6)	13.9 (±6.3)	29.4 (±13.1)
GDP Mannose	0.3 (±0.1)	1.0 (±0.2)	2.1 (±0.6)	5.5 (±1.3)
GDP Mannuroic acid	N. D.	N. D.	N. D.	N. D.
Glycerol-3-phosphate	11.0 (±4.4)	4.6 (±3.1)	400.3 (±186.4)	82.0 (±61.9)
Dihydroxyacetone phosphate	0.8 (±0.2)	2.0 (±1.9)	12.6 (±5.3)	8.5 (±2.5)
Fructose 1,6-biphosphate	0.5 (±0.1)	1.3 (±0.1)		2.3 (±0.4)
Glyceraldehyde-3-phosphate	2.4 (±0.4)	1.7 (±1.0)	6.2 (±2.0)	7.6 (±0.6)
Glycerate 1,3-biphosphate	N. D.	N. D.	N. D.	N. D.
3-Phosphoglyceric acid	0.8 (±0.2)	5.0 (±4.1)	1.4 (±0.1)	10.3 (±5.5)
2-Phosphoglyceric acid	N. D.	N. D.	N. D.	N. D.
Phosphoenolpyruvic acid	U. L.	7.3 (±0.1)	U. L.	14.4 (±4.0)
Pyruvic acid	11.5 (±3.7)	9.7 (±3.7)	42.5 (±24.8)	12.7 (±14.2)
Acetyl CoA	2.5 (±1.5)	4.8 (±3.8)	2.3 (±0.2)	9.1 (±4.6)

2 U. L., undetectable level; N. D., not detectable under this experimental condition. ^{*1},
3 summation of glucose 6-phosphate and mannose 6-phosphate; ^{*2}, summation of fructose
4 6-phosphate and mannose 1-phosphate. Data are averages (± SD) of three experiments.

5

1 Table 2. Intracellular amino acids and other organic acids.

Metabolite	Concentration (pmol/OD ₆₀₀ ml)			
	Sucrose		Glycerol	
	Log phase	Stationary phase	Log phase	Stationary phase
Ala	121.9 (±18.1)	95.0 (±61.3)	220.9 (±88.1)	114.1 (±35.9)
Arg	55.3 (±13.4)	19.7 (±26.0)	51.6 (±26.0)	93.7 (±16.4)
Asn	1.7 (±1.1)	U. L.	1.9 (±1.4)	5.9 (±7.4)
Asp	14.2 (±4.1)	4.9 (±3.8)	24.5 (±4.1)	24.3 (±28.1)
Cys	U. L.	U. L.	U. L.	U. L.
Gln	134.3 (±8.8)	146.3 (±180.5)	217.1 (±158.1)	184.1 (±73.3)
Glu	85.7 (±25.4)	75.4 (±112.6)	368.6 (±127.6)	134.3 (±106.9)
Gly	45.5 (±22.1)	9.5 (±5.4)	65.1 (±9.3)	70.3 (±84.6)
His	4.4 (±1.6)	1.4 (±0.8)	4.3 (±1.9)	13.3 (±12.8)
Ile	18.8 (±5.1)	1.1 (±0.5)	30.3 (±13.3)	8.9 (±11.7)
Leu	45.1 (±11.5)	1.7 (±0.7)	76.8 (±45.6)	13.0 (±17.3)
Lys	47.4 (±7.6)	13.1 (±12.9)	69.1 (±21.1)	83.5 (±32.1)
Met	7.8 (±1.8)	0.3 (±0.1)	8.5 (±5.9)	2.3 (±2.4)
Phe	7.5 (±2.9)	1.0 (±0.3)	14.9 (±8.1)	7.8 (±7.4)
Pro	15.4 (±3.3)	4.1 (±4.2)	28.2 (±5.7)	31.3 (±12.8)
Ser	58.5 (±36.7)	14.3 (±9.7)	68.1 (±23.7)	115.2 (±137.9)
Thr	39.3 (±9.8)	4.3 (±3.1)	65.0 (±25.8)	34.9 (±29.8)
Trp	2.0 (±1.0)	0.4 (±0.3)	2.0 (±1.0)	0.8 (±0.8)
Tyr	22.0 (±5.2)	3.5 (±3.2)	44.3 (±29.7)	20.7 (±10.3)
Val	121.6 (±37.6)	3.4 (±1.6)	168.8 (±100.8)	22.8 (±24.4)
γ-Aminobutyric acid (GABA)	113.9 (±39.6)	0.8 (±0.2)	238.9 (±278.8)	1.7 (±2.1)
Lactic acid	501.0 (±61.1)	530.5 (±309.1)	1239.3 (±507.3)	719.2 (±646.8)

2 U. L., undetectable level. Data are averages (± SD) of three experiments.

3

1 Table 3. Bacterial strains used in the present study.

Bacterial strains (abbreviation)	Characteristics or sequences	References
<i>Azotobacter vinelandii</i> ATCC 12837 (WT)	Wild type strain	ATCC
<i>A. vinelandii</i> $\Delta algD$ ($\Delta algD$)	Alginate-deficient strain with an insertion of the tetracycline resistance gene in chromosomal <i>algD</i> .	43
<i>A. vinelandii</i> MT1 (MT1)	Alginate-overproducing strain derivatized from WT by NTG treatment.	Present study

2 ATCC, American Type Culture Collection.