

1 Enzyme and Microbial Technology

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3 **Characterization and solvent engineering of wheat  $\beta$ -amylase for enhancing its**

4 **activity and stability**

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19 **ABSTRACT**

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21 The kinetic and thermodynamic parameters of wheat  $\beta$ -amylase (WBA) were  
22 characterized and various additives were evaluated for enhancing its activity and  
23 thermostability. WBA activity was examined by neocuproine method using soluble  
24 starch as substrate. The Michaelis constant ( $K_m$ ) and molecular activity ( $k_{cat}$ ) were  
25 determined to be  $1.0 \pm 0.1$  % (w/v) and  $94 \pm 3$  s<sup>-1</sup>, respectively, at pH 5.4 and at 25°C.  
26 The optimum reaction temperature ( $T_{opt}$ ) for WBA activity was 55°C and the  
27 temperature ( $T_{50}$ ) at which it loses half of the activity after 30-min incubation was  $50 \pm$   
28 1°C. Modifications of the solvent with 182 mM glycine and 0.18% (w/v) gelatin have  
29 increased the  $T_{50}$  by 5°C. Glycerol, ethylene glycol, dimethylformamide (DMF) and  
30 dimethyl sulfoxide have also slightly enhanced the thermostability plausibly through  
31 weakening the water structure and decreasing the water shell around the WBA protein.  
32 Ethanol and DMF activated WBA by up to 24% at 25°C probably by inducing favorable  
33 conformation for the active site or changing the substrate structure by weakening the  
34 hydrogen bonding. Its half-life in the inactivation at 55°C was improved from 23 to 48  
35 min by 182 mM glycine. The thermodynamic parameters indicate that WBA is  
36 thermo-labile and sufficient stabilization was achieved through solvent modification

37 with additives and that the heat inactivation of WBA is entropic-driven. It is suggested  
38 that WBA could be applied more widely in starch-saccharification industries with  
39 employing suitable additives.

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41 *Keywords:* activation; additives;  $\beta$ -amylase; thermostablility; solvent engineering, wheat

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## 55 1. Introduction

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57  $\beta$ -Amylase hydrolyses the  $\alpha$ -1, 4-glucan bonds in amylosaccharide chains from the  
58 non-reducing ends and generates maltose. It has considerable application in the  
59 production of high maltose syrups together with starch debranching enzymes and  
60  $\alpha$ -amylases.  $\beta$ -Amylase has been well characterized in higher plants [1-3] and  
61 micro-organisms [4-7]. However, the well-characterized  $\beta$ -amylases are neither active  
62 nor stable at higher temperatures  $> 65^{\circ}\text{C}$  [8]. In many findings,  $\alpha$ -amylase is more  
63 stable compared to  $\beta$ -amylase of the same origin [9-11]. Enzymes may easily be  
64 denatured by slight change of the environmental conditions such as temperature,  
65 pressure, pH, and ionic strength [9]. Nevertheless, stabilization of the enzymes could be  
66 achieved in several ways: screening for more stable ones (favorably from thermophiles  
67 and extremophiles), chemical modification, site-directed mutagenesis, immobilization  
68 and solvent engineering or modifying the enzyme reaction conditions with stabilizing  
69 additives [12-17]. In solvent engineering, selection of appropriate additives is dependent  
70 on the nature of the enzyme and there are no established rules to select effective  
71 additives for improving enzyme functions [18]. The thermostability of  $\beta$ -amylase has  
72 been substantially enhanced by modifying the solvent with additives [18, 19].

73 Different amylases give oligosaccharides with specific lengths of end products.  
74 For this reason, amylases with unique properties need to be studied for various  
75 applications in starch-saccharification for production of food and bio-ethanol [20].  
76 Unlike soybean, barely and sweet potato, wheat was not the common source of  
77  $\beta$ -amylase for starch-saccharification so far. However, the sources of  $\beta$ -amylase supply  
78 has drastically changed due to the escalating prices of the major sources like soybean.  
79 Wheat  $\beta$ -amylase (WBA) is prepared from wheat bran, which is an industrial  
80 by-product in the production of wheat starch and gluten. It is a cheaper alternative  
81 source of  $\beta$ -amylase for industries. Nevertheless, it is lower in thermostability as  
82 compared with  $\beta$ -amylases of other crops and microbes. For instance, the optimum  
83 temperature ( $T_{opt}$ ) of *Clostridium thermosuiphurogenes*  $\beta$ -amylase is 75°C [8]; the  
84 temperature at which it loses half of its activity after 30-min incubation ( $T_{50}$ ) of barely  
85  $\beta$ -amylase is 56.8°C and that of soybean  $\beta$ -amylase is 63°C [21] while the  $T_{opt}$  and  $T_{50}$   
86 after 30-min incubation of WBA are 55 and 50°C, respectively (Data obtained in this  
87 study).

88 Therefore, enhancing the activity and thermostability of WBA has an excellent  
89 prospect for starch-saccharification industries. In this study, we used a  
90 commercially-available WBA preparation, Himaltosin, without further purification

91 because it is already purified from other protein contaminants and utilized industrially.

92 In this paper, we describe the kinetic and thermodynamic properties of WBA and

93 improvement in its activity and thermostability via solvent engineering using various

94 additives. This suggests that WBA would be likely applicable to a wide range of

95 starch-saccharification industries.

96

## 97 **2. Materials and methods**

98

### 99 *2.1. Materials*

100

101 Himaltosin GS (Lot 2S24A), a commercial preparation of WBA, was

102 purchased from HBI Enzymes (Osaka, Japan). This preparation was filtered with a

103 Millipore membrane filter (Type HA; pore size: 0.45  $\mu\text{m}$ ) and used without further

104 purification. According to the manufacturer, the Himaltosin preparation contains 90%

105 starch as a stabilizer, and almost all of the protein is  $\beta$ -amylase and  $\alpha$ -amylase was not

106 detected. Himaltosin was suspended to 20 mM sodium acetate buffer (pH 5.4) at 25°C

107 to be 0.3 mg/ml. In this paper, this buffer was hereinafter referred to as buffer A. The

108 WBA protein content was expected to be 0.03 mg/ml in the suspension and it was

109 followed by filtration with the Millipore membrane filter. However, the protein  
110 concentration in the filtrate was less than 10% of the expected content, suggesting that >  
111 90% of the WBA protein was remained with starch on the filter. The WBA  
112 concentration was determined spectrophotometrically in buffer A using the absorptivity  
113 value ( $A$ ) of  $1.40 \pm 0.02$  at 281 nm with a 1.0-cm light-path for the WBA solution at the  
114 concentration of 1.0 mg/ml [22]. The molecular mass of 57.5 kDa for WBA was used to  
115 determine the molar concentration of WBA (see sections 2.3 and 3.1). Under the  
116 standard condition in this study, the concentration of WBA in the enzyme-reaction  
117 solution was set to 15.0-30.0 nM. The starch concentration due to the stabilizer starch  
118 (0.027%, w/v) was completely removed by filtration with the Millipore membrane filter.  
119 Soluble starch (Lot M7H1482) as substrate and maltose (Lot M1F7568) as standard for  
120 the activity assay were obtained from Nacalai Tesque (Kyoto, Japan). The substrate has  
121 a weight-average molecular weight of  $1.0 \times 10^6$  according to the manufacturer, and thus  
122 the average degree of polymerization of the glucose unit is estimated to be 6,000.  
123 Neocuproine-HCl (2, 9-dimethyl-1, 10-phenanthroline, Lot 032K2533) as coloring  
124 reagent B in the neocuproine method was from Sigma (St. Louis, MO, USA). Coloring  
125 reagent A (0.38 M  $\text{Na}_2\text{CO}_3$ , 1.8 mM  $\text{CuSO}_4$ , and 0.2 M glycine) in the neocuproine  
126 method and all other chemicals were purchased from Nacalai Tesque. All enzyme

127 reactions were carried out in buffer A, pH 5.4.

128

## 129 *2.2. Sodium dodecylsulfate-polyacrylamide gel electrophoresis (SDS-PAGE)*

130

131 SDS-PAGE was performed in a 10% polyacrylamide gel under reducing  
132 conditions [23]. The Himaltosin preparation was suspended in buffer A to the  
133 concentrations of 1, 2, and 5% (w/v). The solution was filtered with a Millipore  
134 membrane filter (Type HA) and reduced by treatment with 10 mM dithiothreitol (DTT).  
135 The solution was applied to SDS-PAGE with a constant voltage of 150 V for 80 min.  
136 Proteins were stained with Coomassie Brilliant Blue R-250. The molecular-mass marker  
137 kit consisting of rabbit muscle phosphorylase *b* (97.2 kDa), bovine serum albumin (66.4  
138 kDa), hen egg albumin (44.3 kDa), and hen egg white lysozyme (14.4 kDa) was a  
139 product of Takara Bio (Otsu, Japan).

140

## 141 *2.3. Measurement of enzyme activity*

142

143 Various initial concentrations of the soluble starch substrate [0.00, 0.09, 0.45,  
144 0.90, 1.13, 1.35, 1.80, 2.02, 2.25, 2.70, 2.93, and 3.15% (w/v)] in the reaction solution

145 were prepared in buffer A at 25°C. The WBA solution in the same buffer was filtered  
146 with a Millipore membrane filter (Type HA) and kept in ice water for immediate use.  
147 The various concentrations of starch were hydrolyzed by WBA (30.0 nM) for 0, 2.5, 5.0,  
148 7.5, and 10.0 min at 25°C. The reaction was stopped by adding 300 µl of 0.1 M NaOH  
149 into 100 µl of the enzyme-reaction solution. The amount of the reducing sugar in the  
150 enzyme-reaction solution was determined by the neocuploine method as follows [24].  
151 Reagent A and reagent B, 250 µl each, were mixed with 50 µl of the enzyme-reaction  
152 solution, boiled for 8 min, and diluted with 550 µl of water after cooling in ice water.  
153 The activity was measured at 450 nm using a Beckman-Coulter DU 800  
154 spectrophotometer (Batavia, IL, USA) [25, 26]. The enzyme activity was determined by  
155 measuring the velocity ( $v$ ) of reducing sugar production, and the reaction velocity was  
156 analyzed by the Michaelis-Menten kinetics. The maximum velocity ( $V_{\max}$ ) and  
157 Michaelis constant ( $K_m$ ) were obtained from the  $v$  vs. the substrate concentration ( $[S]$ )  
158 plots using KaleidaGraph 4.1 (Synergy Software, Reading, PA, USA). The molecular  
159 weight of WBA is 57,500 [27] and was used for the evaluation of the molecular activity  
160 ( $k_{\text{cat}}$ ) (see section 3.1).

161

162 *2.4. The optimum temperature*

163

164           Starch solution (900  $\mu$ l) in buffer A was mixed with the WBA solution (0.150  
165  $\mu$ M; 100  $\mu$ l) in the same buffer for 0, 2.5, 5.0, 7.5, and 10.0 min at 25°C after incubation  
166 at 15, 25, 35, 45, 55, 65, and 75°C in a water bath for 10 min. The initial concentrations  
167 of starch and WBA in the reaction solution were 1.80% and 15.0 nM, respectively. The  
168 reaction was stopped by adding 300  $\mu$ l of 0.1 M NaOH into the enzyme-reaction  
169 solution (100  $\mu$ l). Then the enzyme activity was determined by the neocuproine method  
170 (see above). The optimal reaction temperature at which WBA exhibited the highest  
171 activity was referred to as the optimal temperature ( $T_{opt}$ ).

172

### 173 *2.5. Thermal inactivation of WBA*

174

175           The substrate and WBA solutions were prepared in buffer A. The enzyme  
176 solution was incubated at 25, 35, 45, 55, and 65°C for 10, 20, and 30 min and cooled at  
177 25°C for 3 min in a water bath. The substrate solution (2.00%, w/v; 900  $\mu$ l) was mixed  
178 with the heat-treated WBA solution (0.300  $\mu$ M; 100  $\mu$ l) at 25°C and incubated for 0, 2.5,  
179 5.0, 7.5, and 10.0 min. The initial concentrations of substrate and enzyme in the reaction  
180 solution were 1.80% and 30.0 nM, respectively. The activity was assayed as

181    aforementioned by the neocuproine method and the first-order rate constant  $k$  of the  
182    thermal inactivation was determined assuming pseudo-first order kinetics by plotting  $\ln$   
183     $(v/v_0)$  against the heat-treatment time ( $t$ ) (Eq. 1), where  $v$  is the initial reaction velocity  
184    of the enzyme with heat treatment at each incubation temperature and  $v_0$  is that obtained  
185    without heat treatment and at 25°C. The activation energy  $E_a$  of the thermal inactivation  
186    was obtained by the Arrhenius plot (Eq. 2), and the standard Gibbs energy difference of  
187    activation for thermal inactivation ( $\Delta G^{o\ddagger}$ ), the standard enthalpy difference of activation  
188    ( $\Delta H^{o\ddagger}$ ), and the standard entropy difference of activation ( $\Delta S^{o\ddagger}$ ) were obtained from the  
189    Eyring plot according to Eqs. 3 and 4 [24, 28].

$$190 \quad \ln (v/v_0) = k t \quad (1)$$

$$191 \quad \ln k = - (E_a/R)(1/T) \quad (2)$$

$$192 \quad \Delta G^{o\ddagger} = - RT[\ln hk/ k_B T] \quad (3)$$

$$193 \quad \ln (hk/ k_B T) = (\Delta H^{o\ddagger}/RT) + (\Delta S^{o\ddagger}/R) \quad (4)$$

194    where  $k_B$ ,  $h$ , and  $R$  are the Boltzmann, Plank, and gas constants, respectively.  $T$  is  
195    temperature in Kelvin.

196

197    2.6. Activation and thermostablization of WBA using additives

198

199           The WBA solution in buffer A was mixed and incubated with equal volume of  
200 various additives in the same buffer at 25, 45, 55, and 65°C in a water bath for 30 min  
201 before hydrolyzing soluble starch. The initial concentrations of WBA and substrate in  
202 the reaction solution were 30.0 nM and 1.80%, respectively. The additive concentrations  
203 in the reaction solution were: 45.5, 91, 182, and 364 mM glucose, NaCl, and glycine;  
204 45.5 and 91 mM L-arginine; 0.9, 1.8, 3.6, and 45.5 mM of L-aspartate; 45.5 and 91 mM  
205 of L-cysteine and glutathione (GSH); 0.18 and 0.45% (w/w) gelatin; 0.91, 1.82, and  
206 5.5% (w/w) ethanol and 2-methyl-2-butanol (2M2B); 0.45 and 2.7% (w/w) dimethyl  
207 sulfoxide (DMSO) and dimethylformamide (DMF); and 0.91 and 5.5% glycerol,  
208 ethylene glycol (EG), and  $\beta$ -mercaptoethanol ( $\beta$ ME). Their effects on activation and  
209 thermal stabilization of WBA were examined. The enzyme-additive mixture solution  
210 (0.20 ml) was diluted with water (0.55 ml), and the enzyme activity was measured by  
211 the neocuproine method.

212

### 213 **3. Results**

214

#### 215 *3.1. Kinetic parameters of WBA*

216



235 (Fig. 2)

236

237 3.2. *Thermal inactivation of WBA*

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239 WBA at the concentration of 0.300  $\mu\text{M}$  was treated thermally as described in  
240 the Material and methods section, and the WBA concentration in the enzyme-reaction  
241 solution was fixed to 30.0 nM. The enzyme activity was decreased with the progress of  
242 the heat treatment at every temperature examined (Fig. 3). The enzyme activity in the  
243 hydrolysis of soluble starch was evaluated by measuring the initial velocity ( $v$ ) in the  
244 same buffer at 25°C. The  $v$  value measured in the 0-min incubation at each temperature  
245 was designated as  $v_0$ . The relative activity ( $v/v_0$ ) observed after incubation at various  
246 temperature decreased progressively with increasing the incubation time. The semi-log  
247 plots of  $v/v_0$  against incubation time showed linear relationship at the respective  
248 incubation temperatures (Fig. 3), indicating that the thermal inactivation process of  
249 WBA follows the first-order kinetics. The first-order rate constant ( $k$ ) at the indicated  
250 incubation temperature was evaluated from the slope of the plot.

251

252 (Fig. 3)

253

254 The activation energy  $E_a$  value of the thermal inactivation of WBA in buffer A was  $36 \pm$   
255  $1 \text{ kJ mol}^{-1}$  from the slope of the Arrhenius plot (Fig. 4). The  $\Delta G^{o\ddagger}$ ,  $\Delta H^{o\ddagger}$ , and  $T\Delta S^{o\ddagger}$   
256 values for the thermal inactivation were found to be  $90 \pm 1$ ,  $33 \pm 1$ , and  $-59 \pm 1 \text{ kJ mol}^{-1}$   
257 respectively, at  $25^\circ\text{C}$  from the slope of the Eyring plot (Fig. 5). As  $E_a$  is defined  
258 theoretically as  $\Delta H^{o\ddagger} + RT$ , the  $\Delta H^{o\ddagger}$  value is calculated to be  $34 \pm 1 \text{ kJ mol}^{-1}$ , which is  
259 in good agreement with the value obtained from the Eyring plot.

260

261 (Fig. 4)

262 (Fig. 5)

263

### 264 3.3. *The optimum temperature of WBA*

265

266 WBA activity was measured at various reaction temperatures (Fig. 6). The  
267 maximal activity in starch hydrolysis was obtained at  $55^\circ\text{C}$ , being the optimal  
268 temperature ( $T_{\text{opt}}$ ) of this enzyme in buffer A, pH 5.4.

269

270 (Fig. 6)

271

#### 272 3.4. *The $T_{50}$ of WBA*

273

274 The heat inactivation of WBA was studied by incubating the enzyme at various  
275 temperatures for 30 min before hydrolyzing the substrate. The enzyme activity was  
276 observed to decline with heat treatment even at moderate temperatures (45 and 55°C).  
277 The  $T_{50}$  of WBA, which is the temperature at which the enzyme loses half of its activity  
278 with thermal treatment for 30 min was determined to be  $50 \pm 1^\circ\text{C}$  (Fig. 7) by plotting  
279 the residual activities (%) against temperature of incubation. WBA has lost 30% of its  
280 activity at 45°C, 76% at 55°C, and 95% at 65°C after 30 min of incubation.

281

282 (Fig. 7)

283

#### 284 3.5. *Effect of additives on WBA activity*

285

286 The catalytic activity of WBA in starch hydrolysis was examined in the  
287 presence of various additives at 25°C without heat treatment. Majority of the evaluated  
288 additives did not enhance the enzyme activity (Fig. 8). However, it is noted that ethanol

289 at the concentration of 0.91-5.5%, w/w (or 0.20-1.20 M) enhanced the activity by 24%  
290 and lower concentration (1.8%) of DMF by 11%. On the other hand, the activity was  
291 not much affected with the addition of NaCl and glycine up to 364 mM; and DMF,  
292 DMSO, and EG up to 5.5%. The addition of cysteine up to 91 mM and aspartate up to  
293 45.5 mM showed no substantial effect on the activity, and gelatin (0.18-0.45%, w/w)  
294 had no effect either. The other additives inhibited the activity to varying degrees.  
295 Especially, the activity was reduced to almost 10% with the addition of 0.91-5.5%, w/w  
296 (or 0.11-0.71 M)  $\beta$ ME; and to zero with 45.5-91 mM arginine. The activity decreased  
297 with increasing the glucose and GSH concentrations, and 50% of the activity was lost  
298 with 182 mM glucose; and 75% was with 91 mM GSH.

299

300

(Fig. 8)

301

302 *3.6. Effect of additives on the thermostabilty of WBA*

303

304 The rate of starch hydrolysis by heat treated WBA was examined in modified  
305 solvent by various additives. Glycine was found to be the best in improving the thermal  
306 stability of WBA followed by gelatin. The  $T_{50}$  of WBA was improved by 6°C with 182

307 mM glycine and by 4°C with 0.18% (w/w) gelatin (Fig. 9). The half-life times of the  
308 enzyme were enhanced by 25 min and 17 min with glycine and gelatin, respectively, at  
309 55°C (Table 1). It should be noted that the enzyme activities remained after the thermal  
310 treatment at 45°C was 97% and 92% in the presence of 0.18% (w/w) gelatin and 182  
311 mM glycine although it was only 75% in the absence of additives. Aspartate (45.5 mM)  
312 and DMSO (5.5%, w/w) had no effect on the stability of WBA.  $\beta$ ME (0.91%); ethanol  
313 (0.91%); NaCl (182 mM); and arginine (45.5 mM) slightly decreased the stability of  
314 WBA, and the  $T_{50}$  values were 46-47°C. Glucose (182 mM), cysteine (46 mM), and  
315 GSH (91 mM) considerably decreased the stability with the  $T_{50}$  values of 35-45°C.

316

317 (Fig. 9)

318 (Table 1)

319

#### 320 **4. Discussion**

321

322 In general, depending on the nature and concentration of the additives, they  
323 affect the protein conformation in: (a) screening effect, where the electrostatic repulsion  
324 between similarly charged groups of proteins is reduced by cosolvent ions; (b)

325 solvophobic effect, where ion pair formation occurs, favoring protein folding; and (c)  
326 modification of water structure leading to hydrophobic interactions in proteins [10, 29].  
327 The catalytic activity and thermostability of various enzymes were considerably  
328 enhanced through solvent engineering [17-19, 30, 31].

329           The Michaelis constant ( $K_m = 1.0 \pm 0.1$  %, w/v) and molecular activity ( $k_{cat} =$   
330  $94 \pm 3$  s<sup>-1</sup>) of WBA was evaluated at pH 5.4 and at 25°C using soluble starch as  
331 substrate (Fig. 2). Similarly, the  $K_m$  of glutenin-adsorbed WBA was reported to be  
332 0.15% (w/v) using soluble starch substrate [32], indicating that WBA (which is free in  
333 the reaction solution) used in our study has lower affinity to soluble starch as compared  
334 with WBA adsorbed on glutenin. The other available reports on the kinetic parameters  
335 of WBA were using maltotriose, maltoheptaose, amyloextrin, and amylopectin  
336 substrates under various reaction conditions [27, 33]. The  $K_m$  values of plant  $\beta$ -amylases  
337 have been reported to be in the range of 0.2-0.7 % (w/v) for soluble starch. The value  
338 obtained in this study is apparently higher than those. However, the kinetic parameters  
339 for WBA and other plant  $\beta$ -amylases have not yet examined under the same reaction  
340 conditions using the same soluble starch preparation. Therefore, it is not suitable to  
341 discuss the enzyme functions by comparing the kinetic parameters so far reported. In  
342 this paper, we have reported the kinetic parameters ( $K_m$  and  $k_{cat}$ ) of WBA obtained under

343 the fixed conditions with the WBA and soluble starch preparations in the same lot. It  
344 should be noted that the activity and stability of WBA are affected easily by additives  
345 added in the reaction solution. This means that the kinetic parameters of WBA must be  
346 evaluated with the data collected from the experiments conducted carefully under the  
347 same conditions.

348           Thermodynamic parameters for the heat inactivation of WBA showed that the  
349  $T\Delta S^{o\ddagger}$  value ( $59 \pm 1 \text{ kJ mol}^{-1}$ ) was greater than the  $\Delta H^{o\ddagger}$  value ( $33 \pm 1 \text{ kJ mol}^{-1}$ ), and  
350 thus it can be inferred that the heat inactivation of the enzyme is entropic-driven. The  
351 optimum reaction temperature ( $T_{\text{opt}}$ ) of WBA is  $55^\circ\text{C}$  (Fig. 6). It has been reported that  
352 the  $T_{\text{opt}}$  of Sorghum bicolor cv  $\beta$ -amylase is  $50^\circ\text{C}$  [11, 20, 34], while  $\alpha$ -amylase from  
353 the same cereal crop has  $T_{\text{opt}}$  of  $70^\circ\text{C}$  corresponding with the fact that  $\beta$ -amylases in  
354 most of the cases are lower in thermostability than their respective  $\alpha$ -amylases of the  
355 same origin [10, 11]. The  $T_{50}$  of WBA was determined to be  $50 \pm 1^\circ\text{C}$  (Fig. 6), which is  
356 lower than those of soybean  $\beta$ -amylase,  $63.2^\circ\text{C}$ , and of barely  $\beta$ -amylase,  $56.8^\circ\text{C}$  [21].

357           In the present study, we have examined the effects of additives on the kinetic  
358 parameters and thermostability of WBA. The additives are supposed to have effects on  
359 the structures of WBA, soluble starch substrate, and bulk water. For example, when we  
360 observed decrease in activity by the addition of an additive, there might be some

361 reasons considered such as inhibition of the enzyme by the additive, conformational  
362 changes of the enzyme and/or starch substrate by the additive, etc. Therefore, strict  
363 interpretation of the molecular effects of the additives on the activity and stability of  
364 WBA seems to be difficult, and further studies must be needed. Thus in this paper we  
365 tried to present the effects of the additives without describing the molecular-mechanistic  
366 insights of the cause for the effects, although some possible comments have been made  
367 with references to other enzymes. The molecular-mechanistic study for the effects of the  
368 representative additives is underway.

369           Ethanol and low concentration of DMF have enhanced the activity of WBA by  
370 up to 24% (Fig. 8). The activation of acetylcholinesterase (AChE) by ethanol was  
371 reported and explained as that it non-competitively alters the hydrophobic-interaction  
372 site and subsequently induces favorable conformation to the active center [35]. However,  
373 higher concentration of ethanol had a destabilization effect on WBA (Fig. 9B). This  
374 agrees with a finding that a high concentration of ethanol (> 800 mM) can perturb the  
375 structure of water around hydrophilic area of AChE causing instability to the  
376 conformation of the enzyme [35]. This might be the case for the effects of ethanol on  
377 WBA. These effects should be considered also from the viewpoint of solvent polarity  
378 (see below). The effects of various alcohols on the enzyme structure and activity have

379 been extensively studied with thermolysin, a thermophilic and halophilic  
380 metalloproteinase produced by *Bacillus thermoproteolyticus*. Thermolysin is  
381 remarkably activated and stabilized by neutral salts such as NaCl, and is inhibited by  
382 increasing concentration of alcohols and the degree of inhibition is dependent on the  
383 size of alcohols [36]. It is interesting to note that alcohol such as 2-methyl-1-propanol  
384 (2MP) which binds tightly to the active site inhibits thermolysin strongly, whereas the  
385 alcohols with the sizes larger or smaller than 2MP bind weakly to the active site and  
386 inhibit thermolysin weakly [37]. This suggests that the enzyme activity could be  
387 controlled intentionally using additives with suitable sizes. These lines of evidence have  
388 provided information for the optimal conditions for thermolysin-catalyzed synthesis of a  
389 precursor of the sweetener, aspartame [14]. As shown with thermolysin to find the  
390 optimal conditions for its inhibition by alcohols, it should be possible to find the optimal  
391 conditions for industrial application of WBA by examining the effects of alcohols on the  
392 activity and stability of WBA by changing systematically the size of alcohols.

393           Contrary to the effect of ethanol, the  $T_{50}$  of WBA is slightly improved by  
394 polyols, indicating that polyols are WBA stabilizer. Our finding agrees with reports that  
395 solvent modification by sugars and polyols had marked thermal stabilization in various  
396 enzymes [9, 30]. Polyols were explained to preferentially be excluded from the surface

397 layer of the protein and form a water shell around the protein, so that the protein is  
398 preserved and the conformation becomes more rigid or stable [9, 30]. Similar  
399 mechanism of stabilization by polyols was also reported for organic polar solvents  
400 (DMSO and DMF) [31], and actually polar organic solvents have conferred a slight  
401 thermostabilization to WBA. However, sugars, which are classified also as polyols,  
402 interestingly had no stabilizing effect on WBA in our study.

403           The activation and thermostabilization of WBA were tested using different  
404 additives with various values of empirical parameters of solvent polarity,  $E_T(30)$  [38]  
405 In particular, ethanol ( $E_T(30) = 217 \text{ kJ mol}^{-1}$ ), DMSO ( $189 \text{ kJ mol}^{-1}$ ), DMF ( $183 \text{ kJ}$   
406  $\text{mol}^{-1}$ ), glycerol ( $238 \text{ kJ mol}^{-1}$ ), EG ( $235 \text{ kJ mol}^{-1}$ ),  $\beta$ ME ( $224 \text{ kJ mol}^{-1}$ ), and 2M2B ( $172$   
407  $\text{kJ mol}^{-1}$ ) were examined at different temperatures. According to the results, the half-life  
408 time of WBA was enhanced at  $55^\circ\text{C}$  with ethanol. It is suggested that  
409 thermostabilization by additives could be induced by reducing the degree of  
410 water-solvation or deformation of a water shell around the protein. However, a solvent  
411 2M2B with a low  $E_T(30)$  value decreased the activity and stability of WBA (Figs. 8B  
412 and 9B), suggesting that the effects of additives on the enzyme activity and stability are  
413 complicated and that the effect on the water-solvation might not be the main one [39].

414           Glycine was the most favorable among the evaluated additives in stabilizing

415 WBA followed by gelatin (Table 1) and the stabilization effects of various additive  
416 concentrations were presented in Fig. 9. It should be noted that the thermostability of  
417 WBA in the presence of favorable additives such as glycine and gelatin is almost  
418 comparable with that of soybean  $\beta$ -amylase widely used in starch-saccharification  
419 industry. This suggests that WBA could be applied more widely in food and bio-ethanol  
420 industries with employing suitable additives. A good empirical correlation between the  
421 relative stabilizing effects of glycine with the change in solvent-accessible hydrophobic  
422 surface area of the folded protein was reported [40]. The possible protective effect of  
423 gelatin on penicillinase was stated that it combines with enzyme and form a  
424 thermostable complex [41]. The molecular mechanism of glycine and gelatin on  
425 stabilizing WBA should be examined in the next step from these lines.

426           Arginine was found to destabilize WBA in our study. Similarly,  
427 chloroperoxidase was confirmed to be inactivated by arginine mainly by the binding of  
428 a guanidinium group with the catalytic site [42]. This inactivation effect might be the  
429 same as that given by the denaturant, guanidine hydrochloride; namely, arginine might  
430 cleave the hydrogen bonds in the protein structure and increase the solubility of  
431 hydrophobic residues of the protein. On the other hand, arginine is known to work  
432 effectively in recovering human matrix metalloproteinase 7 from inclusion bodies [43].

433 This suggests that arginine promotes unfolding the misfolded protein structure to lead it  
434 into the correctly folded form. While arginine seems to show multiple effects on protein  
435 stability depending on target proteins, it could be a good tool to increase the stability of  
436 WBA by selecting suitable conditions.

437 We tried to modify thiol groups of WBA using reducing agents like  $\beta$ ME and  
438 GSH, whereas they destabilized WBA. This is because they attack disulfide bonds and  
439 expose proteins to heat denaturation and, hence reduces their thermostability [44].

440 Plausible involvement of thiol groups in the catalytic activity of amylases has been  
441 suggested, although it is not known currently with WBA. The effects of  $\beta$ ME and GSH  
442 should be considered from this point in the next step.

443 Various concentrations of NaCl exhibited destabilizing effect on WBA in our  
444 study. Three possible reasons were suggested for salt-induced inactivation or  
445 destabilization effect on enzymes: (a) break weak hydrogen-bonds and disrupt the  
446 protein conformation; (b) attract water molecules and the enzyme coagulates by  
447 protein-protein hydrophobic interaction; and (c) high concentration of salt makes the  
448 enzyme more likely to bind with the salt ions instead of the substrate by electrostatic  
449 interaction [45]. However, high concentration of neutral salts remarkably improves  
450 thermolysin activity [14, 15]. The catalytic activity of thermolysin is enhanced by 4

451 times with the substitution of the active-site zinc with cobalt and further exponentially  
452 by NaCl up to 13-15 times [29].

453           It is well known that enzyme activity is controlled by the factors of enzyme  
454 structure and reaction environment. The structural factors and environmental factors are  
455 sometimes independent and sometimes closely connected. With their optimal  
456 combination, the optimal catalytic activity should be realized. Protein engineering  
457 (namely, site-directed mutagenesis and chemical modification) is a tool for changing the  
458 enzyme structure in a predictable and precise manner to effect a change on the catalytic  
459 process. Since the enzyme is even improved in only one side of a reaction, any changes  
460 in the rest of the reaction may also alter the catalytic process [46]. Solvent engineering  
461 is a powerful tool in rational control of enzyme activity. In reality, both approaches are  
462 still somewhat difficult to confirm their effects, whereas they have been used  
463 successfully to alter the protein properties [47]. At last, it should be reminded that the  
464 protein-engineered enzymes are strictly limited to use for food processing in many  
465 countries in order to avoid unpredictable harms. Thus solvent engineering must be an  
466 inevitable alternative to find the optimal conditions from the viewpoints of enhancing  
467 enzyme catalytic efficiency, guaranteeing safeness of the products, reducing the costs  
468 for production, etc. When the enzyme activity in its industrial application is increased

469 by solvent engineering, the cost of the additive should be considered in the total cost,  
470 although it is generally much cheaper than that of the enzyme, and the improved  
471 enzyme activity and stability by the additive should decrease the enzyme amount  
472 needed and thus shortened the reaction time, which results in decreasing the running  
473 costs, utility, labor, etc.

474

## 475 **5. Conclusion**

476

477 From the thermodynamic parameters evaluated in this study, it is eminent that  
478 WBA is not stable at temperatures higher than 55°C. The thermal stability of WBA was  
479 improved by the addition of glycine and gelatin explicable through convening  
480 conformation of the enzyme and reducing the interaction of the protein with the solvent.  
481 Polyols and organic polar solvents (DMSO and DMF) also conferred slight stability to  
482 the enzyme while some evaluated additives have exhibited destabilizing effect. The  
483 thermodynamic parameters indicate that WBA is thermo-labile and sufficient  
484 stabilization was achieved by solvent engineering with additives and that the heat  
485 inactivation of WBA is entropic-driven. On the other hand, it was shown that WBA  
486 activity was enhanced by the addition of ethanol and DMF persuasively by altering the

487 hydrophobic interaction and inducing favorable conformation to its active center. It is  
488 suggested that WBA would be applicable to a wide range of saccharification industries  
489 such as food and bio-ethanol production with employing suitable additives.

490

491

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493

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611

612 **Figure legends**

613

614 **Fig. 1.** SDS-PAGE of the Himaltosin preparation. Molecular marker proteins (lane 1);

615 Himaltosin preparation: 1% (w/v) (lane 2), 2% (w/v) (lane 3), and 5% (w/v) (lane 4).

616 The experimental conditions were given in the text (Materials and methods).

617

618 **Fig. 2.** Dependence of the initial reaction velocity ( $v$ ) in the hydrolysis of soluble starch

619 catalyzed by wheat  $\beta$ -amylase (WBA) on substrate concentration. The hydrolysis was

620 carried out in 20 mM sodium acetate buffer (buffer A), pH 5.4, at 25°C. The WBA

621 concentration in the reaction solution was 30.0 nM.

622

623 **Fig. 3.** Progress of the decrease in WBA activity with the time of thermal treatment.

624 WBA (0.300  $\mu$ M) was treated at 25, 35, 45, 55, and 65°C for 0-30 min in buffer A, pH

625 5.4. WBA activity in the hydrolysis of soluble starch was evaluated by measuring the

626 initial velocity ( $v$ ) in the same buffer at 25°C (see Materials and methods). The WBA

627 concentration in the enzyme-reaction solution was 30.0 nM. The  $v$  value measured in

628 the 0-min incubation at each temperature was designated as  $v_0$ . The logarithm of the

629 relative activity [ $\log (v/v_0)$ ] was plotted against the thermal-treatment time. The markers

630 are (temperature in °C): 25, ○; 35, ◇; 45, △; 55, □; and 65, ●. From these semi-log plots,  
631 the first-order rate constant for the thermal inactivation of WBA was evaluated at the  
632 specified temperature of the thermal treatment.

633

634 **Fig. 4.** Arrhenius plot of WBA for the first-order rate constant ( $k$ ) of thermal  
635 inactivation. The rate constants were evaluated from the semi-log plots as shown in Fig.  
636 3 obtained by thermal treatment of the enzyme at various temperatures. The reaction  
637 conditions were given in the text (Materials and methods).

638

639 **Fig. 5.** Eyring plot of WBA for the first-order rate constant ( $k$ ) of thermal inactivation.  
640 The rate constants were evaluated as described in the legend of Fig. 4.

641

642 **Fig. 6.** Effect of temperature on the initial velocity ( $v$ ) of WBA in hydrolyzing soluble  
643 starch. The enzyme reaction was carried out at the temperature indicated. The initial  
644 concentrations of starch and WBA in the reaction solution were 1.80% and 15.0 nM,  
645 respectively. The optimal temperature  $T_{\text{opt}}$  was determined to be 55°C.

646

647 **Fig. 7.** Effect of thermal inactivation of WBA on the enzyme activity. The activity was

648 assayed in buffer A (pH 5.4) in hydrolyzing starch after incubation at various  
649 temperatures indicated for 30 min. The reaction conditions are given in the text  
650 (Materials and methods). The  $T_{50}$  was determined to be  $50 \pm 1^\circ\text{C}$ .

651

652 **Fig. 8.** The effects of various concentrations of additives on the activity of WBA at  $25^\circ\text{C}$ .

653 Symbols for additives (mM): (A) Gly, o; NaCl,  $\diamond$ ; Asp,  $\square$ ; Cys,  $\Delta$ ; glucose,  $\bullet$ ; GSH,  $\blacklozenge$ ;

654 and Arg,  $\blacktriangle$ . Symbols for additives (% w/w): (B) ethanol, o; DMF,  $\diamond$ ; DMSO,  $\Delta$ ; EG,

655  $\square$ ; gelatin,  $\bullet$ ; glycerol,  $\blacklozenge$ ; BME,  $\blacktriangle$ ; and 2M2B,  $\nabla$ . The relative activity (%) of the

656 enzyme obtained without additive was set as 100%.

657

658 **Fig. 9.** Effects various additives on the thermostabilization of WBA after incubation

659 with the additives at various temperatures for 30 min. Symbols for concentrations (mM)

660 of additives: (A) buffer, o; 182 glycine,  $\diamond$ ; 45.5 Arg,  $\square$ ; 45.5 Asp,  $\Delta$ ; 182 NaCl,  $\bullet$ ; 182

661 glucose,  $\blacklozenge$ ; 45.5 Cys,  $\blacktriangle$ ; and 91 GSH,  $\blacksquare$ . Symbols for concentrations (% w/w) of

662 additives: (B) buffer, o; 5.5 EG,  $\diamond$ ; 0.18 gelatin,  $\Delta$ ; 5.5 glycerol,  $\square$ ; 0.91  $\beta$ ME,  $\bullet$ ; 2.7

663 DMF,  $\blacklozenge$ ; 0.91 ethanol,  $\blacktriangle$ ; 5.5 DMSO,  $\blacksquare$ ; and 5.5 2M2B,  $\nabla$ . Low concentrations of some

664 additives were evaluated because of their solubility limit in buffer A (pH 5.4) at  $25^\circ\text{C}$ .

665 The residual activity of WBA without additive was depicted in broken lines.

666

667 Table 1. Effects of selected additive concentrations on thermostabilization of wheat

668  $\beta$ -amylase (WBA) after incubation at 55°C with the additives for 30 min prior

669 to starch hydrolysis

<b>Additives</b>	<b><math>T_{50}</math> (°C)</b>	<b><math>k</math> (<math>\text{min}^{-1}</math>)</b>	<b><math>t_{1/2}</math> at 55°C (min)</b>	<b><math>\Delta G^{o\ddagger}</math> (<math>\text{kJ mol}^{-1}</math>)</b>
none	50 ± 1	0.030 ± 0.004	23 ± 2	90 ± 1
0.18% gelatin	54 ± 1	0.017 ± 0.003	40 ± 1	92 ± 1
0.45% gelatin	54 ± 1	0.018 ± 0.001	39 ± 2	92 ± 1
91 mM glycine	54 ± 1	0.017 ± 0.003	41 ± 1	92 ± 1
182 mM glycine	56 ± 2	0.014 ± 0.006	48 ± 3	92 ± 1

670  $T_{50}$  is the temperature at which WBA loses half of its activity after 30 min of incubation;

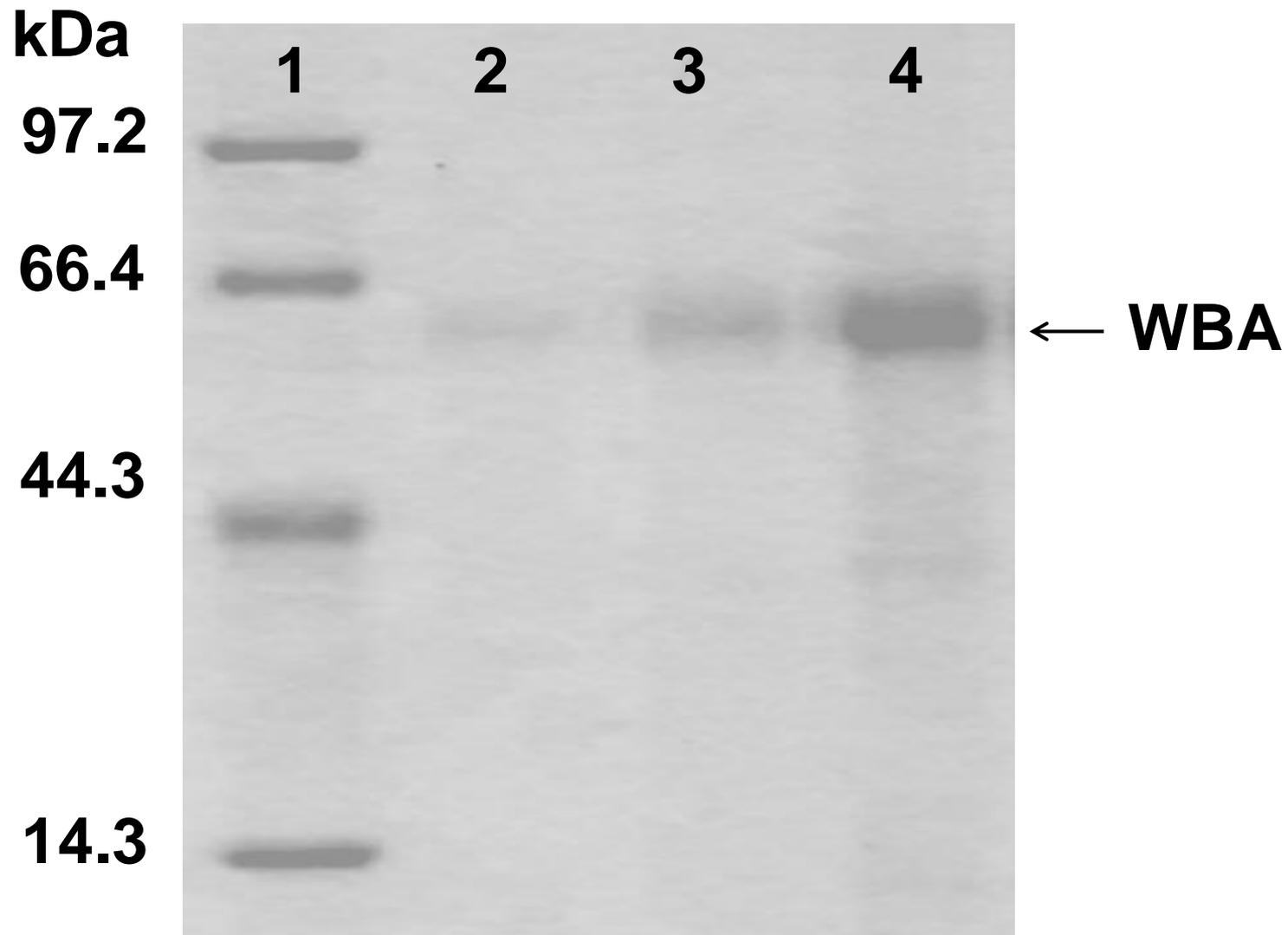
671  $k$  is the first-order rate constant of the thermal inactivation;  $t_{1/2}$  (at 55°C) is the time at

672 which WBA loses half of its activity at 55°C; and  $\Delta G^{o\ddagger}$  is the standard Gibbs energy

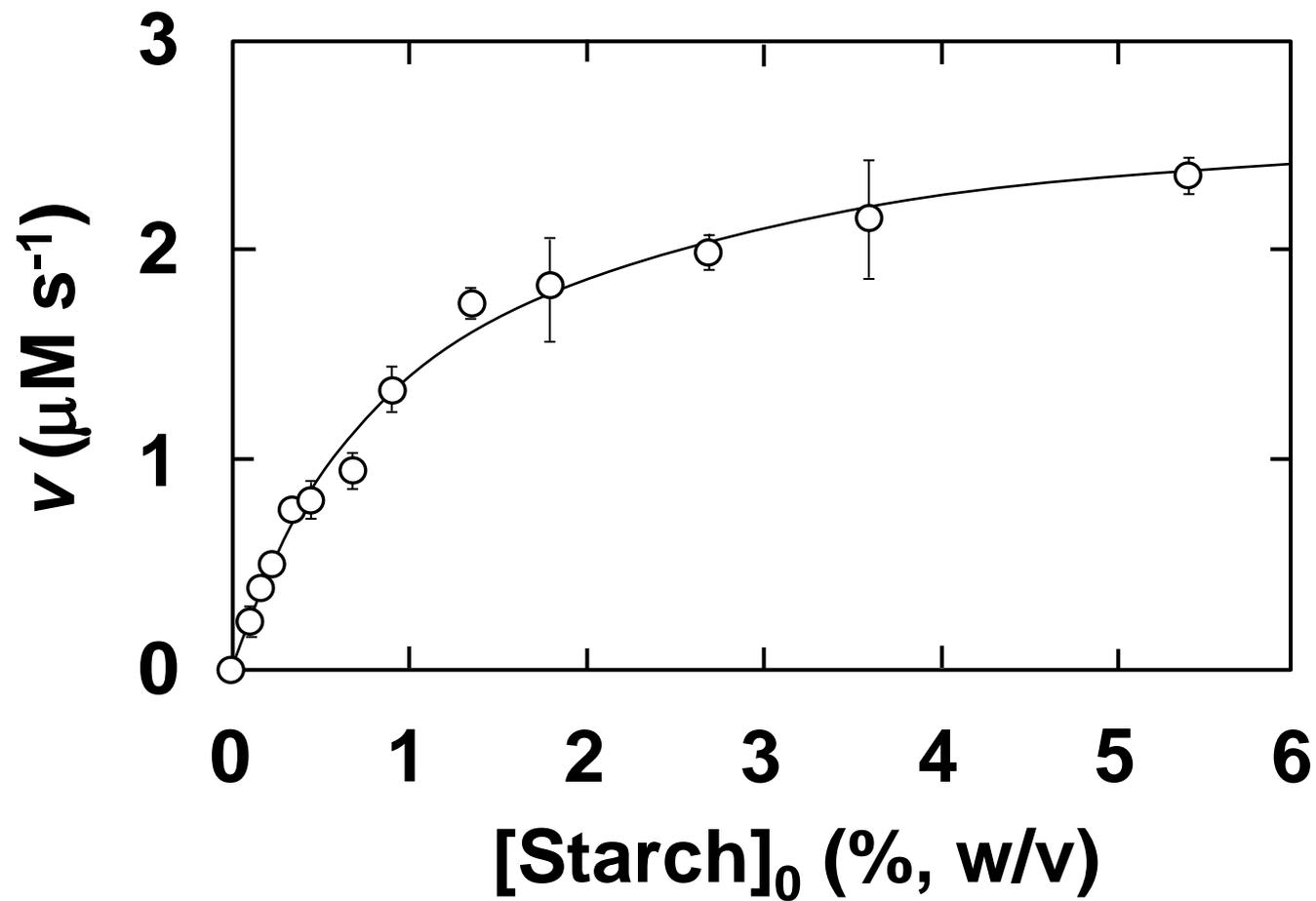
673 difference of activation. Each value is a mean of triplicate analysis ± standard deviation.

674 The initial concentrations of starch and WBA in the reaction solution were 1.80% and

675 30.0 nM, respectively.



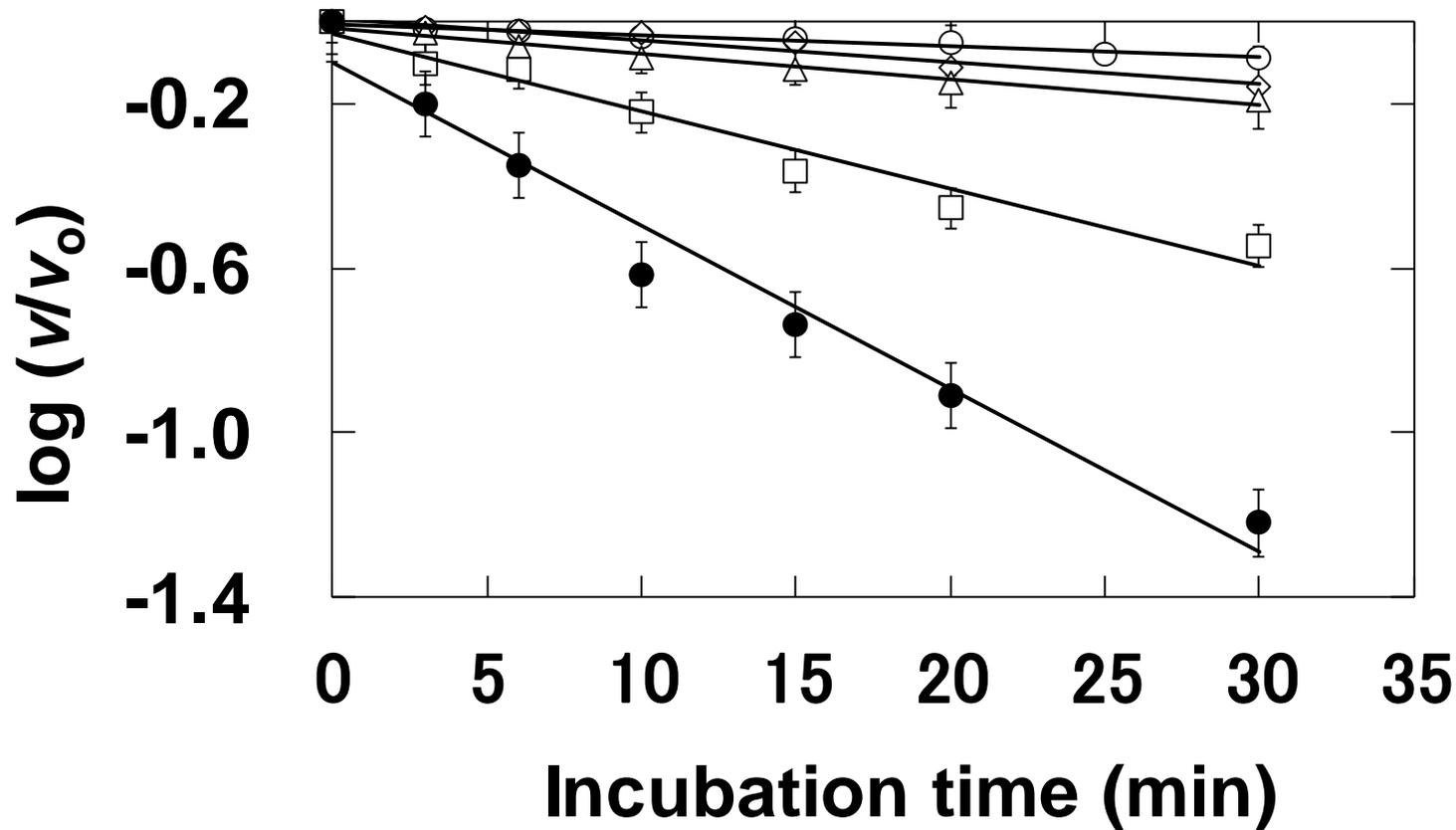
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Fig. 1



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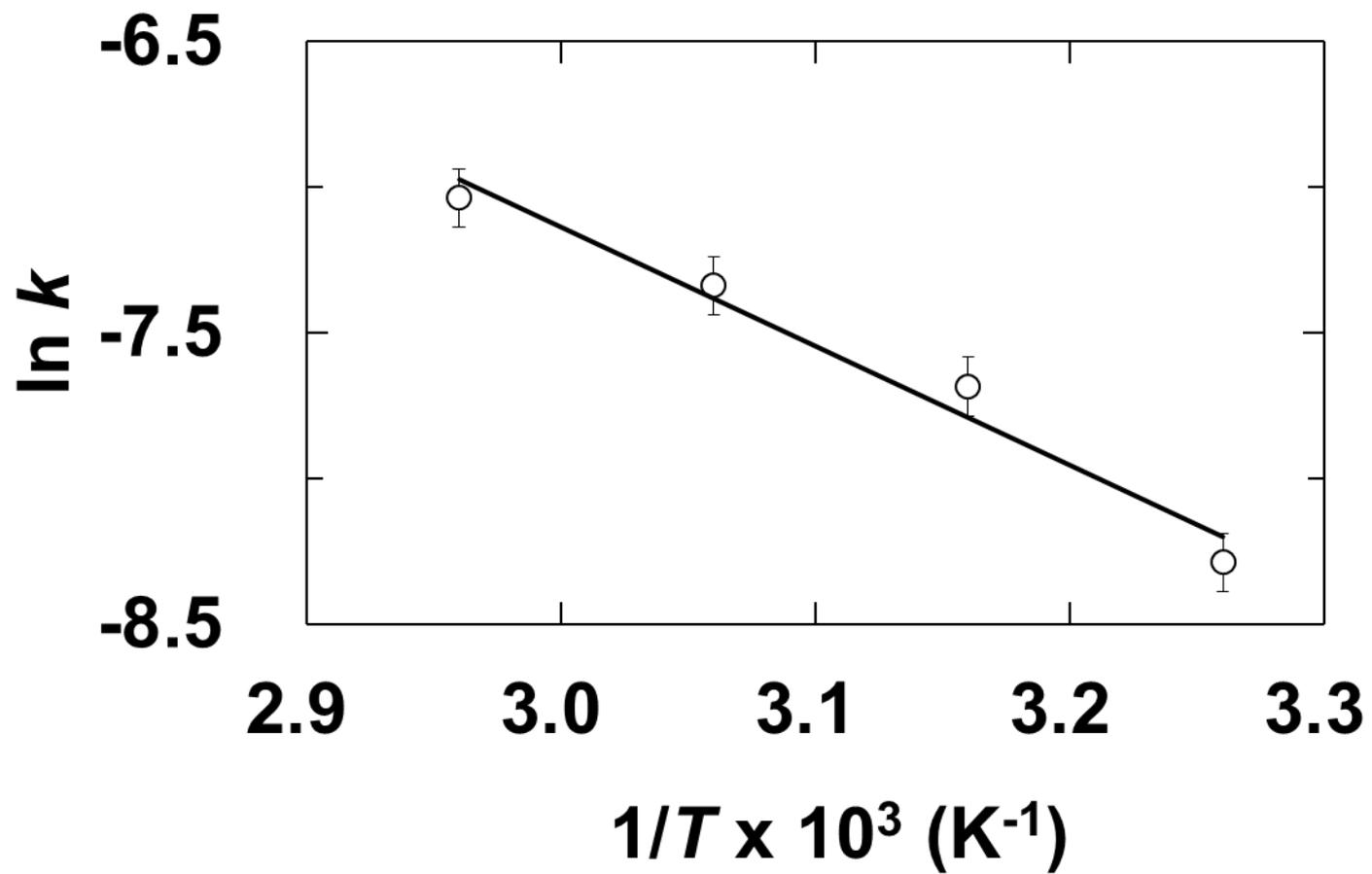
Fig. 2



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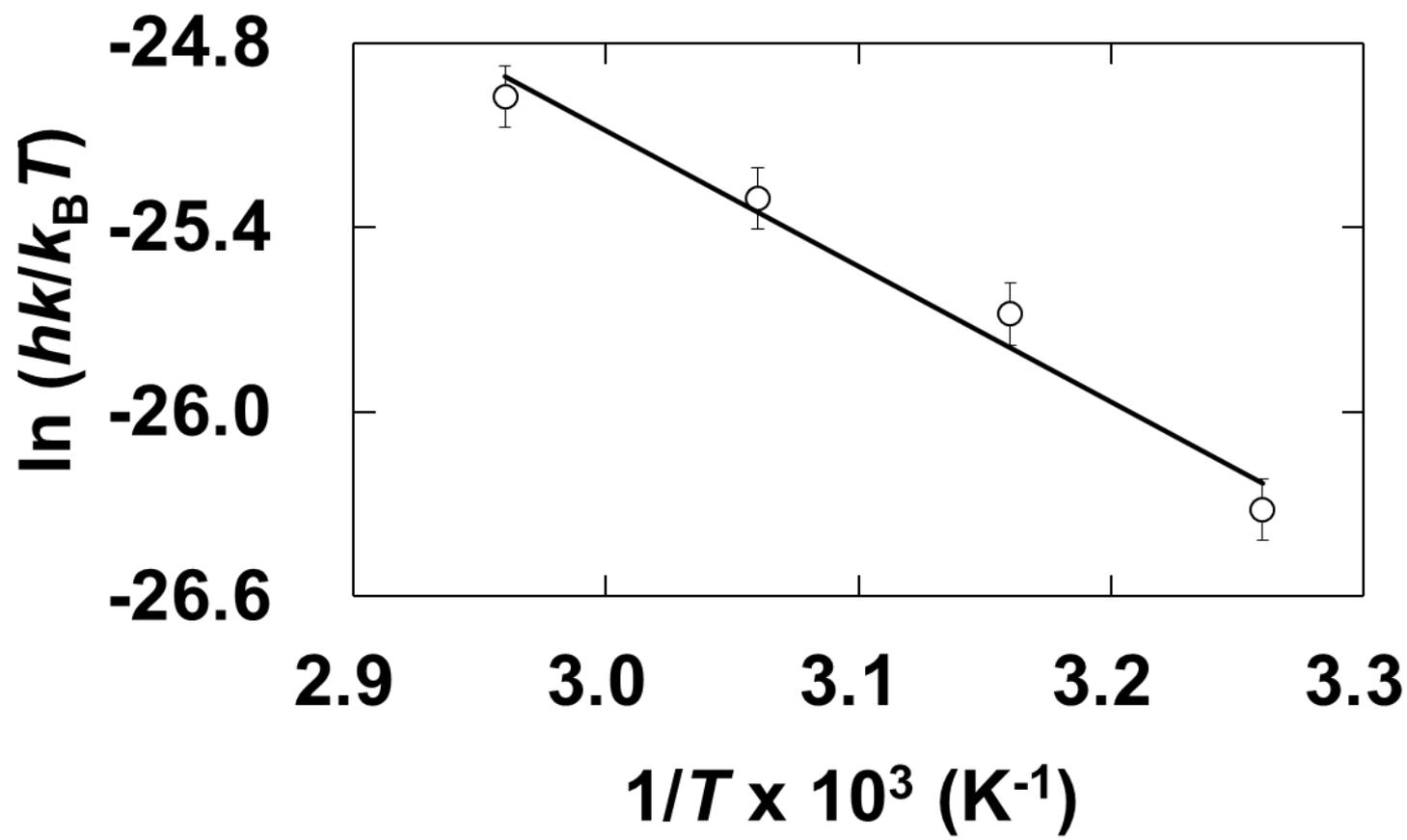
Fig. 3



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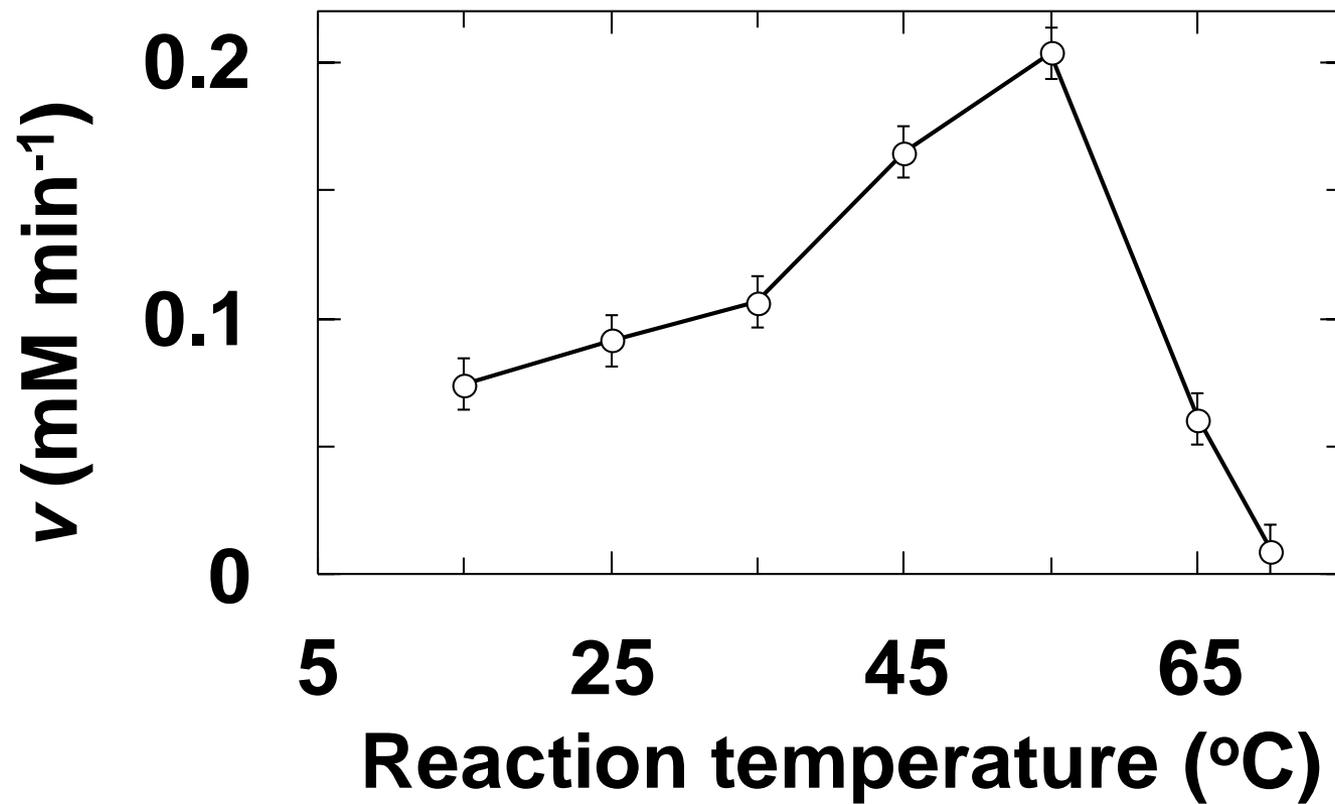


Fig. 4



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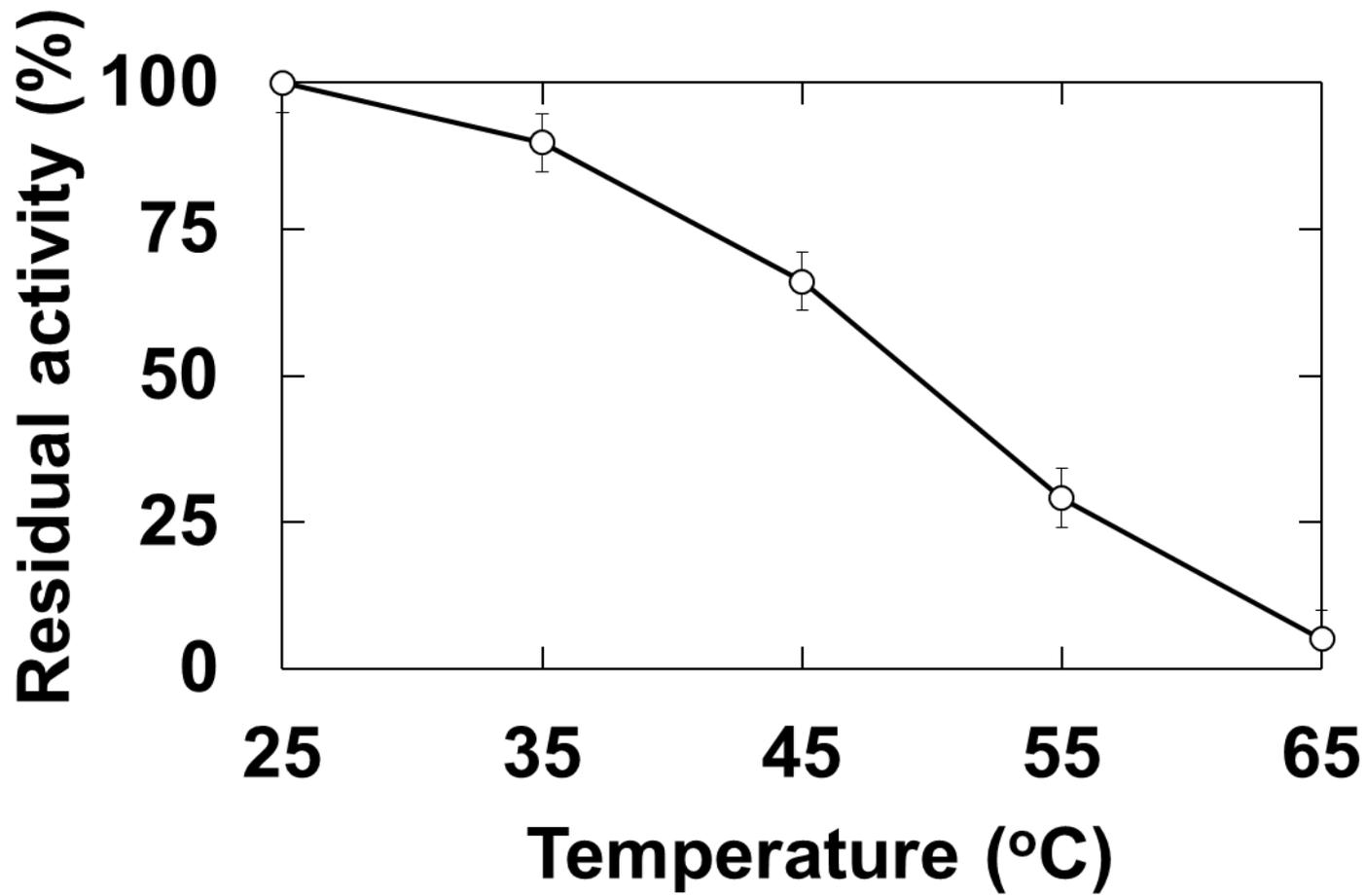
Fig. 5



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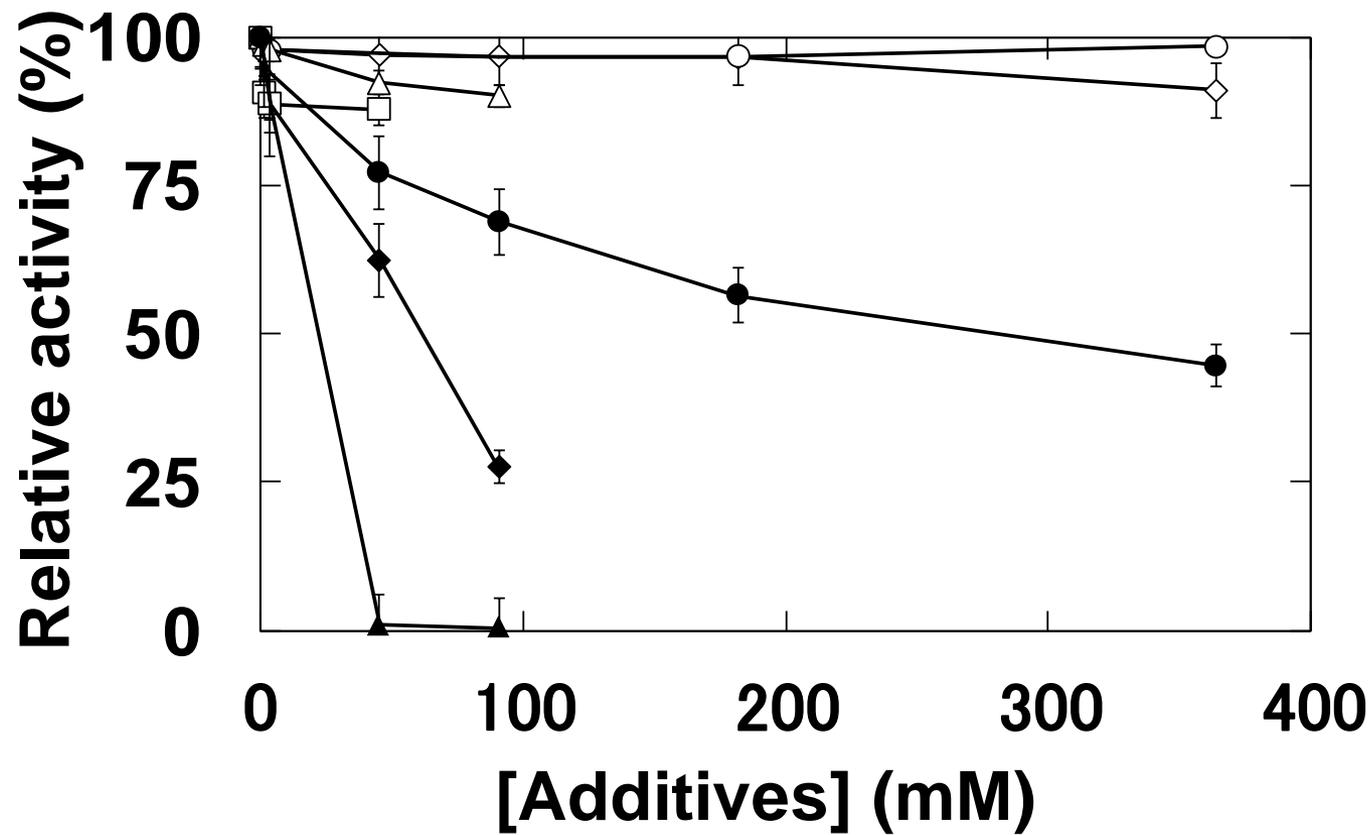
Fig. 6



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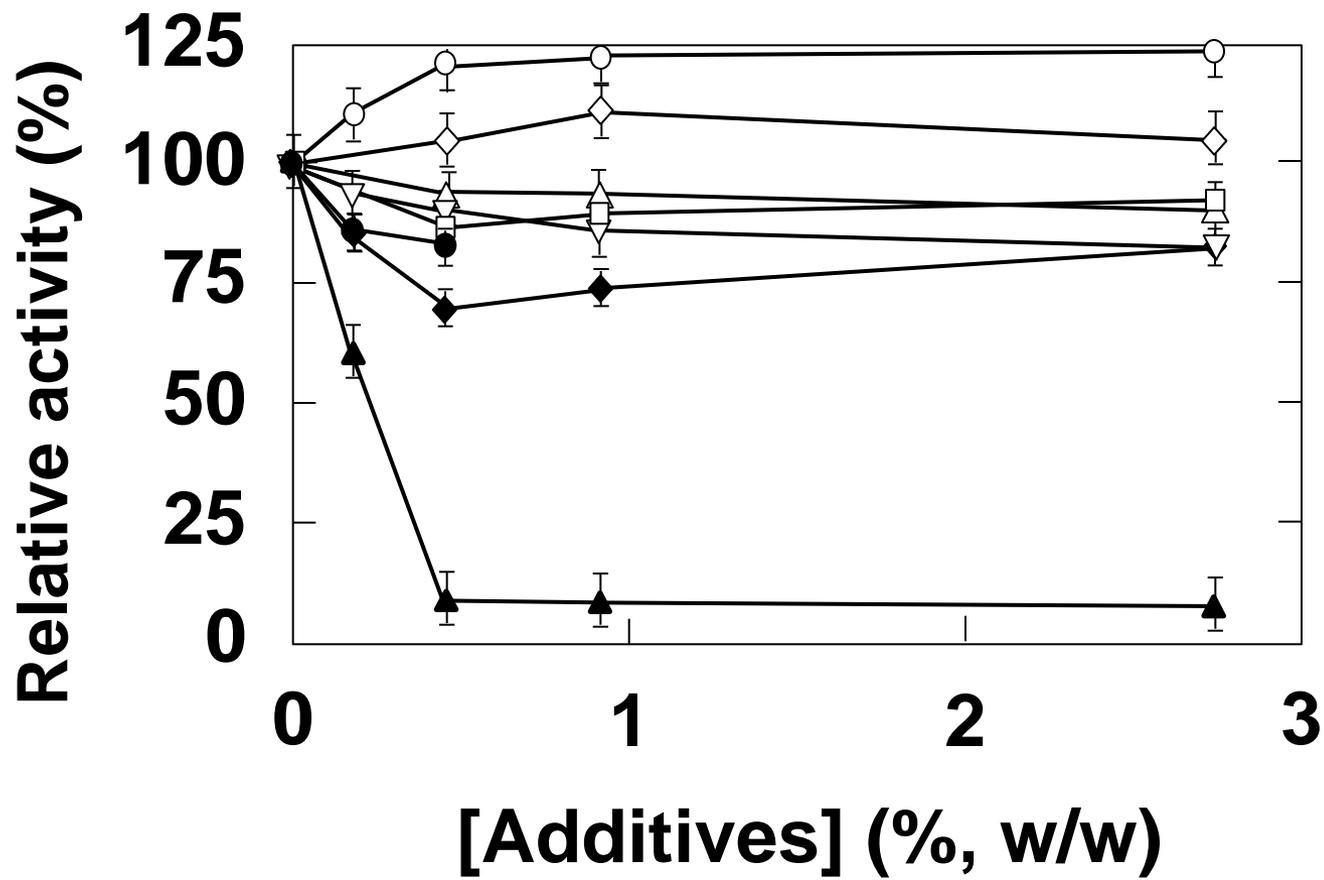
Fig. 7



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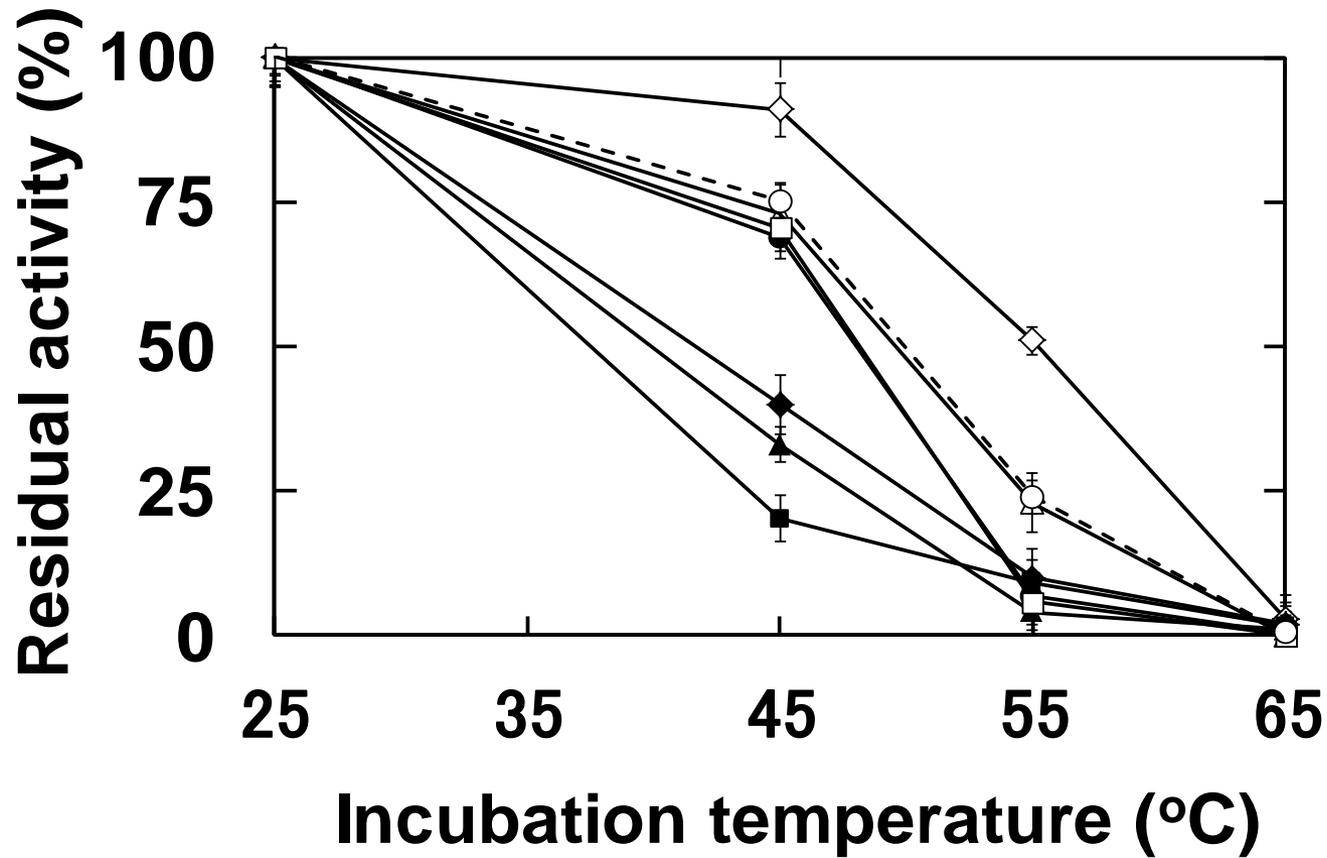
Fig. 8A



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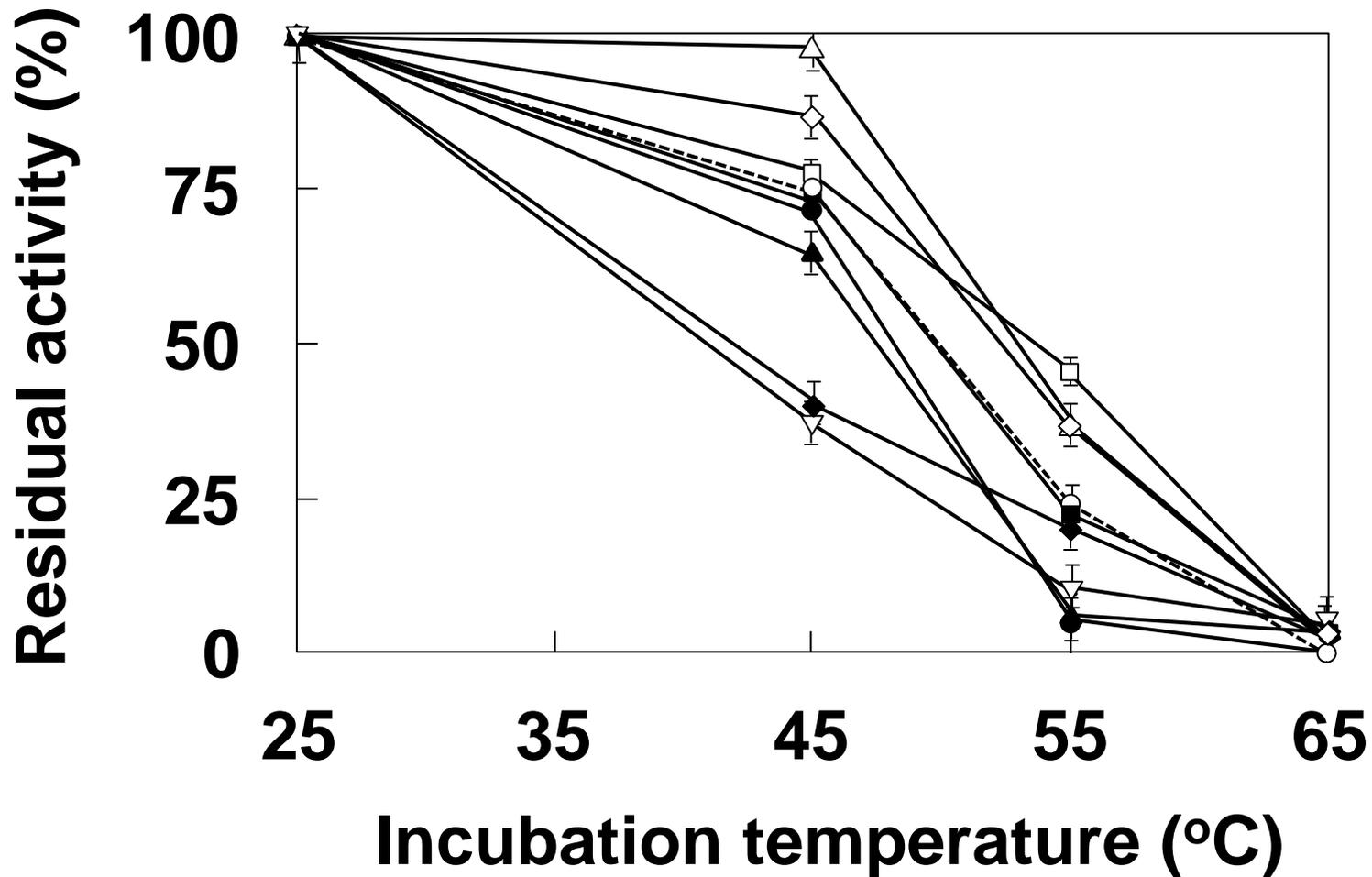
Fig. 8B



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Fig. 9A



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Fig. 9B