

Comparative Study of $M[N(\text{SO}_2\text{F})(\text{SO}_2\text{CF}_3)]-$
 $[N\text{-butyl-}N\text{-methylpyrrolidinium}][N(\text{SO}_2\text{F})(\text{SO}_2\text{CF}_3)]$ (M
= Li, Na, K, Rb, Cs) Ionic Liquid Electrolytes

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ABSTRACT

We systematically evaluated the physicochemical properties of a series of M[FTA]–[C₄C₁pyrr][FTA] ionic liquids (ILs) (M = alkali metal, FTA = (fluorosulfonyl)(trifluoromethylsulfonyl)amide, C₄C₁pyrr = *N*-butyl-*N*-methylpyrrolidinium) as electrolytes for alkali metal-ion batteries. First, the viscosity (η), ionic conductivity (σ), and density (ρ) of the M[FTA]–[C₄C₁pyrr][FTA] ILs (molar fraction of M[FTA]: $x(\text{M[FTA]}) = 0.20$) were measured. The σ values ranged from 1–3 mS cm⁻¹ at 298 K and increased as follows: Na < Li < K < Rb < Cs, which indicated that the Li-based IL did not obey the trend predicted by the charge densities of alkali metal cations. Second, the Li-based IL exhibited slightly lower vertical intercept values than the other FTA-based ILs in the Walden plots obtained using the results of η , σ , and ρ measurements. Third, the electrochemical stability of the ILs was investigated by cyclic voltammetry, and the redox potentials of the alkali metals ($E(\text{M}^+/\text{M})$) were determined. The $E(\text{M}^+/\text{M})$ values of the FTA-based ILs increased as follows: Cs < Rb < K < Li < Na. Subsequently, we compared the obtained $E(\text{M}^+/\text{M})$ values with those of other general electrolytes, such as propylene carbonate (PC)-based electrolytes and aqueous solutions. The trend in $E(\text{M}^+/\text{M})$ values of the FTA-based ILs was similar to that of PC-based electrolytes and was significantly different from that of aqueous solutions. In particular, the FTA- and FSA-based ILs (FSA = bis(fluorosulfonyl)amide) presented the most negative $E(\text{Na}^+/\text{Na})$ and $E(\text{K}^+/\text{K})$ values among various electrolytes, which indicated that utilization of these IL electrolytes for the development of Na- and K-ion batteries would present significant advantages.

1. INTRODUCTION

The establishment of a low-carbon society is one of our final goals toward achieving a sustainable energy supply and demand cycle and solving various environmental problems. Renewable energy resources present lower greenhouse gas emissions than the conventional large power plants based on fossil fuels and nuclear power, and are feasible for small-scale electricity production in microgrids. Although renewable energy resources are promising next-generation primary energy sources, their electricity production largely depends on the weather and climate. Thus, energy storage devices are indispensable for a stable power supply. Li-ion batteries (LIBs) are potential candidates as stationary power storage devices in microgrids and also for electric vehicles because they possess high energy densities and have been widely used for portable electric devices, such as mobile phones and laptops. Although upsizing the current LIBs is needed to further expand their applications for microgrids, two main drawbacks should be overcome: the scarcity and uneven distribution of lithium and cobalt resources, which could cause steep price increases depending on the political situation, and the use of flammable and volatile organic solvent-based electrolytes. Therefore, our group has focused on Na- and K-ion batteries (NIBs and KIBs, respectively) with ionic liquid (IL) electrolytes as next-generation energy storage devices.¹⁻
³ Sodium and potassium resources are abundant in the Earth's crust, which facilitates the construction of many batteries using inexpensive raw materials.⁴⁻⁷

ILs consist only of cations and anions and present unique properties, such as negligible volatility, nonflammability, and high electrochemical and thermal stability. Thus, ILs have been used as safe and high-performance electrolytes for various electrochemical devices, including batteries, capacitors, and fuel cells.^{1,8,9} We have recently reported FSA-based IL electrolytes (FSA = bis(fluorosulfonyl)amide) for KIBs,² and compared the physicochemical and electrochemical

properties of the ILs with alkali metal cations (Li^+ , Na^+ , and K^+) as charge carriers. The redox potential of potassium is more negative than that of lithium in these ILs. On the other hand, it is well known that the redox potential of lithium is the most negative in aqueous solutions.¹⁰ Thus, to analyze the operating voltages of alkali metal-ion batteries, comprehensive studies should be performed to determine the properties of the electrolytes, including the redox potentials of the alkali metals in IL electrolytes and other typical liquid electrolytes.

In this study, we focused on IL electrolytes that consists of FTA^- anions ($\text{FTA}^- = (\text{fluorosulfonyl})(\text{trifluoromethylsulfonyl})\text{amide}$). The FTA -based ILs exhibit higher thermal stability and lower melting points than the FSA -based ILs,¹¹⁻¹³ and thus confer wider operation temperature windows to electrochemical devices. Despite these advantages, few studies have been conducted on FTA -based ILs as battery electrolytes.¹⁴⁻¹⁶ Thus, we investigated the physicochemical and electrochemical properties of $[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ ($\text{C}_4\text{C}_1\text{pyrr} = N\text{-butyl-}N\text{-methylpyrrolidinium}$) and $\text{M}[\text{FTA}]-[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ ($\text{M} = \text{Li, Na, K, Rb, Cs}$) ILs, and analyzed the effects of the alkali metal cations on their properties. Lastly, we compared the obtained redox potentials of the alkali metals with those of other common electrolytes, such as PC -based electrolytes and aqueous solutions.

2. EXPERIMENTAL

All reagents were handled under a dry Ar atmosphere. $[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ IL and $\text{M}[\text{FTA}]$ ($\text{M} = \text{Li, Na, K, Rb, and Cs}$) salts were purchased from Provisco CS Ltd., and were dried at 333 K for 24 h prior to use. The water contents of the reagents were tested to be less than 100 ppm using the Karl Fisher titration method. $\text{M}[\text{FTA}]-[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ binary ILs (molar fraction of $\text{M}[\text{FTA}]$: $x(\text{M}[\text{FTA}]) = 0.20$) were prepared by mixing the two salts in a dry Ar-filled glove box. The thermal behaviors of the ILs were analyzed using a differential scanning calorimetry (DSC)

instrument (DSC8230, Rigaku Co.). The viscosities (η) of the ILs were measured using an electromagnetically spinning viscometer (EMS-1000, Kyoto Electronics Manufacturing Co., Ltd.) in the temperature range of 273–388 K at 5 K intervals. The ionic conductivities (σ) of the ILs were obtained via AC impedance spectroscopy as follows. First, the cell constant of a T-shaped polytetrafluoroethylene cell (K_{cell}) was determined using a standard 0.1 mol dm⁻³ KCl aqueous solution. Subsequently, the bulk impedance of the FTA-based ILs (R_{IL}) was measured, and lastly, the ionic conductivities (σ_{IL}) of the ILs were calculated by dividing K_{cell} by R_{IL} ($\sigma_{\text{IL}} = K_{\text{cell}}/R_{\text{IL}}$). The densities (ρ) of the ILs were determined using a vibration-type density meter (DA-650, Kyoto Electronics Manufacturing Co., Ltd.) in the temperature range of 273–368 K at 5 K intervals.

Cyclic voltammetry measurements were conducted at ~298 K using an electrochemical measurement system (HZ-7000, Hokuto Denko Corp.). A three-electrode cell was used to determine the electrochemical windows (EWs) of the FTA-based ILs. A Cu or glassy carbon disk was used as the working electrode for the negative and positive potential regions, respectively; a Pt mesh was used as the counter electrode; and the reference electrode was a Ag wire immersed in [C₃C₁pyrr][FSA] IL (C₃C₁pyrr = *N*-methyl-*N*-propylpyrrolidinium) which contained 50 mmol dm⁻³ silver trifluoromethanesulfonate. The scan rate was set at 5 mV s⁻¹.

3. RESULTS AND DISCUSSION

3.1 Physicochemical properties

Prior to the DSC measurements of the [C₄C₁pyrr][FTA] and M[FTA]–[C₄C₁pyrr][FTA] ($x(\text{M[FTA]}) = 0.20$; M = Li, Na, K, Rb, Cs) ILs, we confirmed the thermal behaviors of the M[FTA] single salts. Our results are in good agreement with those previously reported in the literature (Fig. S1).¹² Fig. 1 illustrates the DSC curves of the FTA-based ILs at a scan rate of 2 K min⁻¹. [C₄C₁pyrr][FTA] exhibits only glass transition behavior at approximately 170 K, indicating

that supercooling occurs under these measurement conditions. Conversely, the $[\text{C}_n\text{C}_1\text{pyrr}][\text{FSA}]$ ILs ($n = 3, 4$) easily crystallize at scan rates lower than 5 K min^{-1} .^{2,17} Thus, supercooling is likely to occur in the FTA-based ILs owing to the asymmetric structure of the FTA^- anion. All $\text{M}[\text{FTA}]-[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ ILs, except for the Li-based IL, present similar trends, and their glass transition behavior is observed in the temperature range of 180–190 K. $\text{Li}[\text{FTA}]-[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ exhibits crystallization and melting behaviors between 230 and 260 K, and its end temperature of melting is determined to be 262 K. This exceptional solidification behavior can be attributed to the presence of Li^+ cations, which interacts strongly with the FTA^- anions. In addition, according to the previous report on $\text{Li}[\text{FTA}]-[\text{C}_{201}\text{C}_1\text{pyrr}][\text{FTA}]$ ($\text{C}_{201}\text{C}_1\text{pyrr} = N\text{-methoxyethyl-}N\text{-methylpyrrolidinium}$) system,¹⁵ the IL exhibited only glass transition behavior at a scan rate of 5 K min^{-1} . Thus, the crystallization behavior is likely to be affected by scan rates. Overall, the DSC results suggest that the use of FTA-based IL electrolytes confers wide operation temperature windows to electrochemical devices.

Fig. 2 presents the Arrhenius plots of viscosities (η) for the FTA-based ILs, and the η values are summarized in Table S1. The η values of the Na-based IL and pure $[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ at 298 K are the highest (149 mPa s) and lowest (51.0 mPa s), respectively, of all FTA-based ILs. The η plots of the IL cannot be fitted with straight lines, which is typical for viscous and glass-like compounds.¹⁸ Therefore, the η plots are usually fitted with the Vogel–Tammann–Fulcher (VTF) equation, as follows:

$$\eta(T) = A_\eta T^{1/2} \exp\left(\frac{B_\eta}{T - T_{0\eta}}\right) \quad (1)$$

where T is the absolute temperature, $T_{0\eta}$ is the ideal glass transition temperature, and A_η and B_η are constants related to the frequency factor and activation energy, respectively. The VTF parameters of all FTA-based ILs are provided in Table S6.

Fig. 3 illustrates the Arrhenius plots of the ionic conductivities (σ) of the FTA-based ILs. The pure [C₄C₁pyrr][FTA] and Na-based IL exhibit the highest (4.4 mS cm⁻¹) and lowest (1.7 mS cm⁻¹) σ values at 298 K, respectively (see Table S2). The σ value of [C₄C₁pyrr][FTA] has been previously reported to be 3.5 mS cm⁻¹ at 293 K,¹⁹ which is consistent with our result (3.7 mS cm⁻¹ at 293 K). Moreover, the ionic conductivity of the [C₄C₁pyrr][FTA] IL is lower and higher than those of the [C₄C₁pyrr][FSA] (5.25 mS cm⁻¹ at 293 K²⁰) and [C₄C₁pyrr][TFSA] (2.21 mS cm⁻¹ at 293 K²¹; TFSA = bis(trifluoromethylsulfonyl)amide) counterpart ILs, respectively. The nonlinear dependence of σ on T observed in Fig. 3 can be explained using the following VTF fitting equation:

$$\sigma(T) = \frac{A_{\sigma}}{T^{1/2}} \exp\left(-\frac{B_{\sigma}}{T - T_{0\sigma}}\right) \quad (2)$$

where $T_{0\sigma}$ is the ideal glass transition temperature and A_{σ} and B_{σ} are constants related to the frequency factor and activation energy, respectively. The fitting results are summarized in Table S6.

Fig. 4 depicts the density plots of pure [C₄C₁pyrr][FTA] and the M[FTA]–[C₄C₁pyrr][FTA] ($x(\text{M[FTA]}) = 0.20$; M = Li, Na, K, Rb, Cs) ILs. Pure [C₄C₁pyrr][FTA] possess the lowest ρ , and the ρ values of the FTA-based ILs increase with the size of the alkali metal cations in the ILs. The ρ plots of all ILs can be fitted linearly. Table 3 summarizes the obtained ρ values and their fitting parameters. The ρ of pure [C₄C₁pyrr][FTA] is 1.357 g cm⁻³ at 298 K, which is higher and lower than those of [C₄C₁pyrr][FSA] (1.307 g cm⁻³ at 298 K²⁰) and [C₄C₁pyrr][TFSA] (1.395 g cm⁻³ at 298 K²¹), respectively. Such dependence of ρ on the anion species are consistent with the data previously reported for ammonium-based IL systems.¹³ Table S4 summarizes the molar concentrations of alkali metal cations ($C(\text{M}^+)$) of the M[FTA]–[C₄C₁pyrr][FTA] ILs ($(x(\text{M[FTA]}) = 0.20)$), which are calculated using their ρ values. The $C(\text{M}^+)$ values of all FTA-based ILs range

between 0.80 and 0.82 mol dm⁻³.

Table 1 summarizes the melting temperature and other physicochemical properties at 298 K of the FTA-based ILs. As mentioned above, the melting behavior was observed for only Li-based system. The η , σ , ρ , and $C(M^+)$ values of the FTA-based ILs increase as follows:

η / mPa s pure IL (51.0) < Cs (97.4) < Li (117) \approx Rb (119) < K (128) < Na (149)

σ / mS cm⁻¹ Na (1.7) < Li (2.0) < K (2.2) < Rb (2.3) < Cs (2.6) < pure IL (4.4)

ρ / g cm⁻³ pure IL (1.357) < Li (1.416) < Na (1.427) < K (1.431) < Rb (1.464) < Cs
(1.494)

$C(M^+) / \text{mol dm}^{-3}$ Cs (0.806) < Rb (0.811) < K (0.814) < Na (0.819) < Li (0.820)

Because ionic liquids consist only of cations and anions, the ion–ion interactions are considered to be the main factor that determines their ionic mobility. Typically, weaker interactions between the alkali metal cations and anions result in higher ionic mobility. Thus, the M[FTA]–[C₄C₁pyrr][FTA] ILs with larger-sized alkali metal cations having lower charge densities are anticipated to present weaker ion–ion interactions and higher σ values. Although the Na-, K-, Rb-, and Cs-based systems obey this rule, the η and σ values of the Li-based IL are lower and higher, respectively, than expected. A similar trend was reported for the M[FSA]–[C₃C₁pyrr][FSA] ILs (M = Li, Na, K).² In addition, Li[TFSA] has been previously reported to present the highest η and lowest σ of all the single M[TFSA] (M = Li, Na, K, Rb, Cs) molten salts in the temperature range of 543–573 K.²² Furthermore, Li[FSA]–PC and Li[FSA]–EC–DEC presented the lowest σ values at 298 K of all M[FSA]–PC and M[FSA]–EC–DEC (M = Li, Na, K; EC = ethylene carbonate; DEC = diethyl carbonate) organic solvent-based electrolytes.^{7,23} Therefore, the effects of the alkali metal cations on the electrolyte properties have not been entirely elucidated.

Fig. 5 shows the relationships between the molar ionic conductivities (λ) and inverse of the η

values of the FTA-based ILs, which are termed the Walden plots. The λ values are provided in Table S5. All plots lie in the slightly lower right region of the ideal KCl line, and therefore the ILs are classified as “good” ILs.²⁴ Moreover, these plots are fitted with straight lines in accordance with the fractional Walden rule, as follows:^{24–26}

$$\lambda\eta^\alpha = \text{constant} \quad (3)$$

where α is a constant ($0 < \alpha < 1$) that corresponds to the slope of the Walden plot. The α values of all ILs range between 0.91 and 0.94, which are similar to the values previously reported for other IL electrolytes (Table 2).^{2,20,27–29} When $T_0 = T_{0\eta} = T_{0\sigma}$, Eq. (3) can be expressed as:

$$\lambda\eta^\alpha = \sigma(T) \frac{M}{\rho(T)} \eta(T)^\alpha = \frac{MA\eta^\alpha A_\sigma T^{\frac{\alpha-1}{2}}}{\rho(T)} \exp\left(\frac{\alpha B_\eta - B_\sigma}{T - T_0}\right), \quad (4)$$

where M is the formula weight of the ionic liquid. Lastly, the following equation is derived from the assumption that $T^{(\alpha-1)/2}$ and $\rho(T)$ are constant in the measurement temperature range:

$$\alpha = \frac{B_\sigma}{B_\eta} \quad (5)$$

The α values of all the ILs in this study are calculated using Eq. (5), and the results are presented in Table S6. The calculated values are very close to the slopes of the Walden plots, which indicates the validity of the VTF fittings for η and σ .

The vertical intercept of the Walden plot, $C' = \log(\lambda\eta^\alpha)$, is an important factor that determines the ion transport properties of various electrolytes. Here, $C' = \log(\lambda)$ at $\eta = 100$ mPa s. Table 2 summarizes the α and C' constants of selected ILs and molten salts. First, the C' value of the Li[FTA]–[C₄C₁pyrr][FTA] IL is slightly more negative than those of the other M[FTA]–[C₄C₁pyrr][FTA] ILs in this study. However, no other apparent trends in C' are observed for the effects of the alkali metal cations on the Walden plots. Second, we compared the FTA-based ILs in this study with two common amide-based ILs with C₄C₁pyrr⁺ cations: [C₄C₁pyrr][FSA] and

[C₄C₁pyrr][TFSA]. Because the α and C' values of [C₄C₁pyrr][FSA] were reported to be 0.913 and -0.067 ,²⁰ and those of [C₄C₁pyrr][TFSA] were 0.924 and -0.180 ,²¹ respectively, the dependence of α and C' on the anion species appears to be negligible.

According to a report on single M[TFSA] molten salts,²² the α values of the Li, Na, and K salts were approximately 0.85, which were smaller than those of other room-temperature ILs. Moreover, using the Walden plot reported by Kubota et al.,²² the C' value of Li[TFSA] was -0.381 . This is distinctively more negative than those of the other M[TFSA] melts and indicates the poorer dissociation extent of the Li[TFSA] melt. Tsuzuki et al. previously reported the stable geometries of alkali metal cations and the three amide anions (FSA⁻, FTA⁻, and TFSA⁻) via *ab initio* molecular orbital calculations.³⁰ The calculated stabilization energies of the most stable geometries were more negative for the Li salts and less negative for the Cs salts, which was consistent with the trend in the charge densities of the alkali metal cations. The results reported by Tsuzuki et al. were in good agreement with those derived from the Walden plots of the single M[TFSA] melts.²² Thus, a similar trend is naturally anticipated for the single M[FTA] melts. In this study, however, no obvious trends are found in the M[FTA]–[C₄C₁pyrr][FTA] ILs, as shown in Table 2. Because the molar fractions of M[FTA] and [C₄C₁pyrr][FTA] are 0.20 and 0.80, respectively, the poorer dissociative nature of Li[FTA] appears to be diluted by the dominant organic cations, which results in the C' value of Li[FTA] being slightly more negative than those of the other M[FTA] ILs.

3.2 Electrochemical properties

Fig. 6 presents the cyclic voltammograms of pure [C₄C₁pyrr][FTA] and M[FTA]–[C₄C₁pyrr][FTA] ($x(\text{M[FTA]}) = 0.20$; M = Li, Na, K, Rb, Cs) ILs. The cathodic currents of pure

[C₄C₁pyrr][FTA] are observed in the negative potential region below -3.0 V (vs. Ag⁺/Ag) and sharply increases at approximately -3.5 V (vs. Ag⁺/Ag). This trend is consistent with that previously reported in the literature and is attributed to the reductive decomposition of the C₄C₁pyrr⁺ cation.¹⁹ In the positive potential region, the anodic currents are observed above 2.0 V (vs. Ag⁺/Ag), and are ascribed to the oxidative decomposition of the FTA⁻ anion.^{14,19} When the limit potential is defined as the point at which the absolute value of the current density reaches 0.1 mA cm⁻², the cathodic (E_{CL}) and anodic (E_{AL}) limit potentials are -2.98 and 1.96 V (vs. Ag⁺/Ag), respectively, and thus the electrochemical window (EW) is 4.94 V. In the previous study on pure [C₄C₁pyrr][FTA], EW was determined to be 5.71 V at 293 K by linear sweep voltammetry.¹⁹ Although the current density threshold was the same as our criterion (0.1 mA cm⁻²), the scan rate was as low as 1 mV s⁻¹, which was one-fifth of that used in the present study. In general, larger EW values can be obtained at lower scan rates, which in turn might give unrealistic information for practical application. Thus, we adopted a relatively strict criterion of 5 mV s⁻¹ in the present study.

Similar anodic behaviors are observed for the M[FTA]-[C₄C₁pyrr][FTA] ILs. Table 3 summarizes the electrochemical properties of all the FTA-based ILs in this study. All alkali metal-ion systems presents similar E_{AL} values (1.91 – 1.97 V (vs. Ag⁺/Ag)), which indicates that the decomposition of the FTA⁻ anion determines their anodic stability. Conversely, E_{CL} depends on the alkali metal ion species. For example, for the Li-ion system, a steep increase in the reduction current was observed from approximately -3.5 V (vs. Ag⁺/Ag) during the potential sweep in the negative direction, which corresponds to the electrodeposition of Li metal. During the potential sweep in the positive direction, the current linearly increases from negative to positive, and the intercept with the potential axis, *i.e.* the zero-current potential, is -3.48 V (vs. Ag⁺/Ag). The oxidation currents flow from this potential, which is attributed to the dissolution reaction of Li

metal. We defined the zero-current potential as the redox potential of lithium ($= E(\text{Li}^+/\text{Li})$) and cathodic limit of this electrolyte, *i.e.* $E_{\text{CL}} = E(\text{Li}^+/\text{Li})$.

The E_{CL} values of the alkali metal-ion systems are more negative than that of pure $[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ (Table 3), which indicates that the addition of $\text{M}[\text{FTA}]$ salts suppresses the decomposition of the organic $\text{C}_4\text{C}_1\text{pyrr}^+$ cation. A similar EW widening was reported for the $\text{Li}[\text{FTA}]-[\text{C}_{201}\text{C}_1\text{pyrr}][\text{FTA}]$ IL.¹⁵ The redox potentials of the alkali metals (V vs. Ag^+/Ag) increases as follows: $\text{Cs} (-3.83) < \text{Rb} (-3.71) < \text{K} (-3.67) < \text{Li} (-3.48) < \text{Na} (-3.36)$. Thus, $\text{Cs}[\text{FTA}]-[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ and $\text{Na}[\text{FTA}]-[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ present the widest (5.74 V) and narrowest (5.33 V) EWs of all $\text{M}[\text{FTA}]-[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ ILs. In one of our previous studies, we determined that the redox potentials of lithium, sodium, and potassium of the $[\text{C}_3\text{C}_1\text{pyrr}][\text{FSA}]$ ILs presented a similar trend, *i.e.* $E(\text{K}^+/\text{K})$ was more negative than $E(\text{Na}^+/\text{Na})$ and $E(\text{Li}^+/\text{Li})$ (see Table S7).²

The coulombic efficiencies of the alkali metal deposition–dissolution reactions are provided in Table 3. Although the Li-, K-, and Cs-based ILs exhibited initial coulombic efficiencies of over 70%, the coulombic efficiencies of the Na- and Rb-based ILs are as low as approximately 30%. Such poor reversibility of the Na metal deposition–dissolution reaction has been reported in previous articles on FSA-based electrolytes;² however, the origin of these behaviors has not been elucidated. Because only a few comprehensive studies on the alkali metal deposition–dissolution have been conducted, including studies on Rb- and Cs-based electrolytes, it is necessary to continue to gather information on various electrolytes.

The trends in the redox potentials of alkali metals ($E(\text{M}^+/\text{M})$) are further compared among common electrolytes based on PC, acetonitrile (MeCN), water, ethanol (EtOH), *N,N*-dimethylformamide (DMF), *N*-methylpyrrolidone (NMP) and dimethyl sulfoxide (DMSO)

solvents. Table S7 summarizes the $E(M^+/M)$ values with respect to the redox potentials of silver ($E(Ag^+/Ag)$) in these electrolytes. The potentials for aqueous and organic solvent electrolytes were thermodynamically calculated, and not determined via electrochemical measurements.¹⁰ Moreover, the redox potentials of the Ag^+/Ag couple listed in Table S7 were measured or calculated for each electrolyte. Because $E(Ag^+/Ag)$ varies depending on electrolyte, the $E(M^+/M)$ values in one electrolyte cannot be directly compared with those in other electrolytes.

Although the silver redox couple (Ag^+/Ag) is commonly used as a reference electrode for various electrochemical measurements, the comparison of $E(M^+/M)$ with $E(Li^+/Li)$ is very important for predicting and evaluating the electrolyte properties of novel batteries. Fig. 7 illustrates the redox potentials of alkali metals ($E(M^+/M)$) with respect to that of lithium ($E(Li^+/Li)$). The $E(Na^+/Na)$ values are the most positive of all $E(M^+/M)$ values for all electrolytes. For the FTA-based ILs, $E(M^+/M)$ values (V vs. Li^+/Li) increase as follows: Cs (-0.35) < Rb (-0.23) < K (-0.19) < Li (0) < Na (0.12). $E(Cs^+/Cs)$ in the FTA-based ILs is the most negative of all the $E(M^+/M)$ values for all the electrolytes we compare. As mentioned above, the $E(M^+/M)$ values ($M = K, Na, Li$) of the FSA-based ILs present the same trend as those of the FTA-based ILs. Moreover, some organic solvents, such as PC and MeCN, present a similar trend. For example, $E(M^+/M)$ values (V vs. Li^+/Li) in PC increase as follows: Cs (-0.31) < Rb (-0.16) < K (-0.09) < Li (0) < Na (0.23).

Conversely, the $E(Li^+/Li)$ values in aqueous solution and other organic solvent-based electrolytes are the most negative. The $E(M^+/M)$ values (V vs. Li^+/Li) in aqueous solution increase as follows: Li (0) < Cs (0.013) < Rb (0.097) < K (0.104) < Na (0.326). The operating voltages of the alkali metal-ion batteries is an important parameter; however, the maximum operating voltages of alkali metal-ion batteries are limited within the EWs of the electrolytes. When the E_{AL} values of

the electrolytes with different alkali metal cations are the same, the magnitude of the so-called maximum operating voltage of the alkali metal-ion batteries (V_{\max}) is directly affected by the $E(M^+/M)$ values. According to their $E(M^+/M)$ values in aqueous solutions, LIBs are sometimes considered to be the highest-voltage batteries; however, the trend in the $E(M^+/M)$ values largely depends on the electrolyte. If the $E(M^+/M)$ values in aqueous solutions are used, the V_{\max} values of the NIB and KIB are lower than that of the LIB by 0.326 and 0.104 V, respectively. In contrast, for the FTA-based ILs, the V_{\max} values of the KIB and NIB are 0.19 V higher and 0.12 V lower, respectively, than that of the LIB. As presented in Fig. 7, the $E(\text{Na}^+/\text{Na})$ and $E(\text{K}^+/\text{K})$ values are the most negative in the FTA- and FSA-based ILs. Thus, according to their V_{\max} values, these ILs are most advantageous as NIB and KIB electrolytes.

4. CONCLUSIONS

In this study, we compared FTA-based ILs with alkali metal cation charge carriers as alkali metal-ion battery electrolytes. The physicochemical properties of pure $[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ and $\text{M}[\text{FTA}]-[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ ILs ($x(\text{M}[\text{FTA}]) = 0.20$; $\text{M} = \text{Li}, \text{Na}, \text{K}, \text{Rb}, \text{Cs}$) with alkali metal-ion concentrations of approximately 0.8 mol dm^{-3} presented several trends. Most ILs, except for the Li-based ILs, presented only supercooling behavior during the DSC measurements, and that was beneficial for the construction of batteries with wide temperature operating windows. The η , σ , and ρ values of the FTA-based ILs were measured over a wide temperature range of 273–368 K. The temperature dependences of both η and σ obeyed the VTF equations. The orders of magnitude of the σ values at 298 K were explained by the charge densities of the alkali metal cations for all systems except for the Li-based system. The Walden plots of the FTA-based ILs were well fitted with the fractional Walden rule, in which the C' value of the Li-based IL was slightly lower than

those of the other alkali metal-based ILs. The obtained Walden plot parameters of the FTA-based ILs were compared with those of ILs and molten salts with other amide anions, viz. FSA⁻ and TFSA⁻. Cyclic voltammetry experiments revealed that the $E(M^+/M)$ values increased as follows: Cs < Rb < K < Li < Na, and the Cs-based IL presented the widest electrochemical window of all FTA-based ILs. Lastly, the trend in the $E(M^+/M)$ values in the FTA-based ILs was compared with those in other electrolytes. Although the trends in the $E(M^+/M)$ values in the FTA-based ILs and PC-based electrolytes were similar, the trend in aqueous solutions was entirely different. In particular, the FTA- and FSA-based ILs presented the most negative $E(Na^+/Na)$ and $E(K^+/K)$ values among the analyzed electrolytes. Thus, the use of these IL electrolytes for the development of NIBs and KIBs present significant advantages.

■ ASSOCIATED CONTENT

Supporting Information

Viscosities, ionic conductivities, densities, molar concentrations, molar ionic conductivities, Vogel–Tammann–Fulcher parameters, redox potentials of alkali metals in various electrolytes, and differential scanning calorimetry curves (PDF)

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Notes

The authors declare no competing financial interest.

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■ TABLES and FIGURES

Table 1 Melting temperature and other physicochemical properties at 298 K of [C₄C₁pyrr][FTA] (Pure IL) and M[FTA]–[C₄C₁pyrr][FTA] ionic liquids (ILs) ($x(\text{M[FTA]}) = 0.20$; M = Li, Na, K, Rb, Cs).

IL	T_m / K	η / mPa s	σ / mS cm ⁻¹	ρ / g cm ⁻³	$C(\text{M}^+)$ / mol dm ⁻³
Pure IL	n.d.	51.0	4.4	1.357	–
M = Li	262	117	2.0	1.416	0.820
M = Na	n.d.	149	1.7	1.427	0.819
M = K	n.d.	128	2.2	1.431	0.814
M = Rb	n.d.	119	2.3	1.464	0.811
M = Cs	n.d.	97.4	2.6	1.494	0.806

T_m : end temperature of melting, η : viscosity, σ : ionic conductivity, ρ : density, and $C(\text{M}^+)$: molar concentration of alkali metal cation (M^+)

Table 2 Summary of Walden plot parameters of different ionic liquids (ILs) and molten salts.

IL	α	C'	Ref.
[C ₄ C ₁ pyrr][FTA]	0.93	-0.19	
Li[FTA]-[C ₄ C ₁ pyrr][FTA]	0.94	-0.25	This study
Na[FTA]-[C ₄ C ₁ pyrr][FTA]	0.94	-0.22	
K[FTA]-[C ₄ C ₁ pyrr][FTA]	0.91	-0.18	
Rb[FTA]-[C ₄ C ₁ pyrr][FTA]	0.94	-0.18	
Cs[FTA]-[C ₄ C ₁ pyrr][FTA]	0.93	-0.21	
[C ₄ C ₁ pyrr][FSA]	0.913	-0.067	20
[C ₄ C ₁ pyrr][TFSA]	0.924	-0.180	21
Li[TFSA]	0.845	-0.381	22
Na[TFSA]	0.844	-0.118	22
K[TFSA]	0.861	0.009	22
Rb[TFSA]	0.908	-0.034	22
Cs[TFSA]	0.900	-0.070	22

Table 3 Cathodic (E_{CL}) and anodic (E_{AL}) limit potentials, electrochemical windows (EW), and coulombic efficiencies of the alkali metal deposition–dissolution cycle during the first cycle (η_{1st}) for [C₄C₁pyrr][FTA] (Pure IL) and M[FTA]–[C₄C₁pyrr][FTA] ionic liquids (ILs) ($x(M[FTA]) = 0.20$; M = Li, Na, K, Rb, Cs).

	Limit potential / V vs. Ag ⁺ /Ag		EW / V	η_{1st} / %
	E_{CL}	E_{AL}		
Pure IL	−2.98 ^a	1.96 ^a	4.94	n/a
M = Li	−3.48 ^b	1.97 ^a	5.45	76
M = Na	−3.36 ^b	1.97 ^a	5.33	30
M = K	−3.67 ^b	1.91 ^a	5.58	71
M = Rb	−3.71 ^b	1.93 ^a	5.64	29
M = Cs	−3.83 ^b	1.91 ^a	5.74	75

^aThe E_{CL} values of the pure IL and E_{AL} values of all ILs were determined as the potentials at which the current density during the cathodic and anodic sweep reaches -0.1 and 0.1 mA cm⁻², respectively.

^bThe E_{CL} values of the M[FTA]–[C₄C₁pyrr][FTA] ILs are defined as the zero-current potentials in their cyclic voltammograms. ($E_{CL} = E(M^+/M)$)

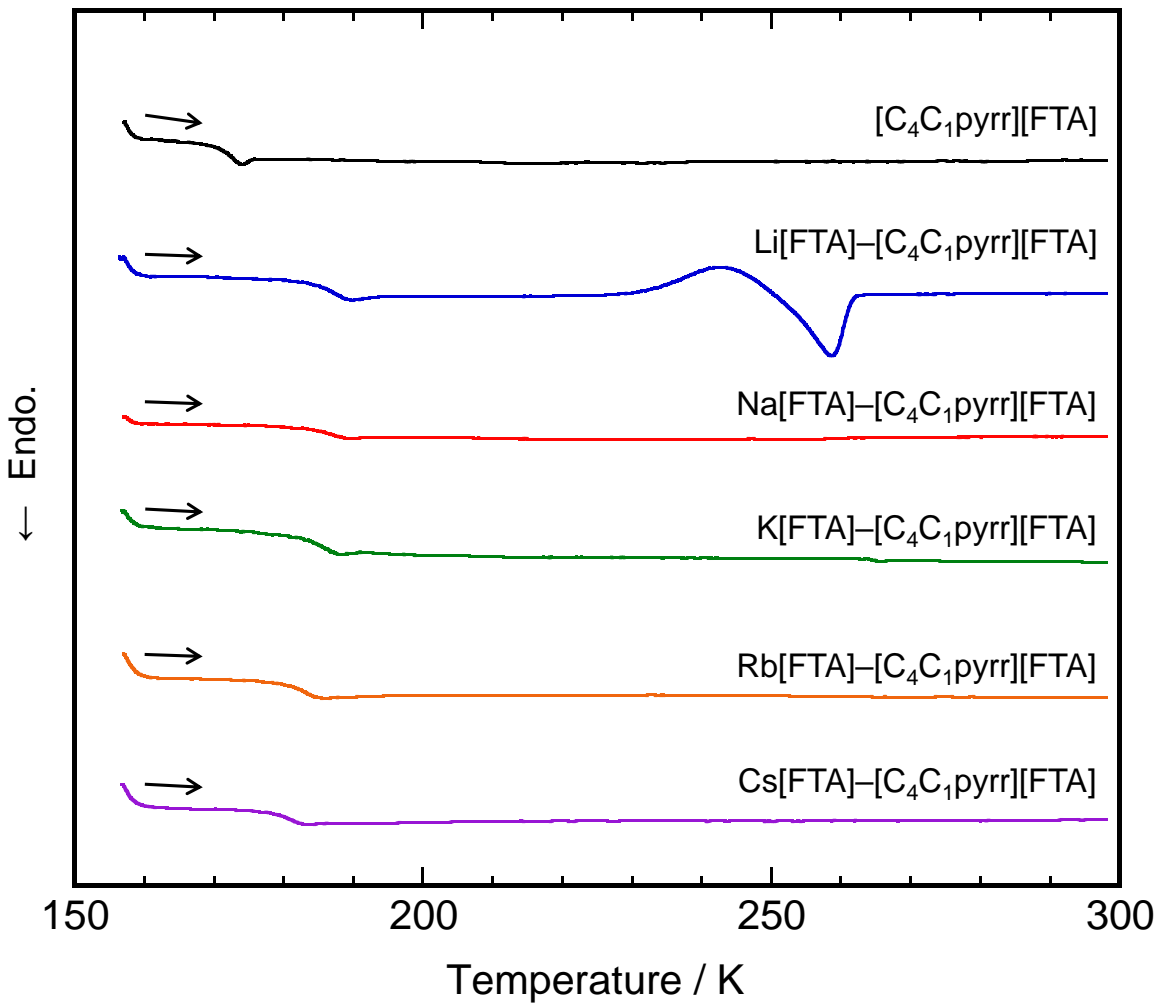


Fig. 1 Differential scanning calorimetry curves of $[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ and $\text{M}[\text{FTA}]-[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ ionic liquids ($x(\text{M}[\text{FTA}]) = 0.20$; $\text{M} = \text{Li}, \text{Na}, \text{K}, \text{Rb}, \text{Cs}$) at a scan rate of 2 K min^{-1} .

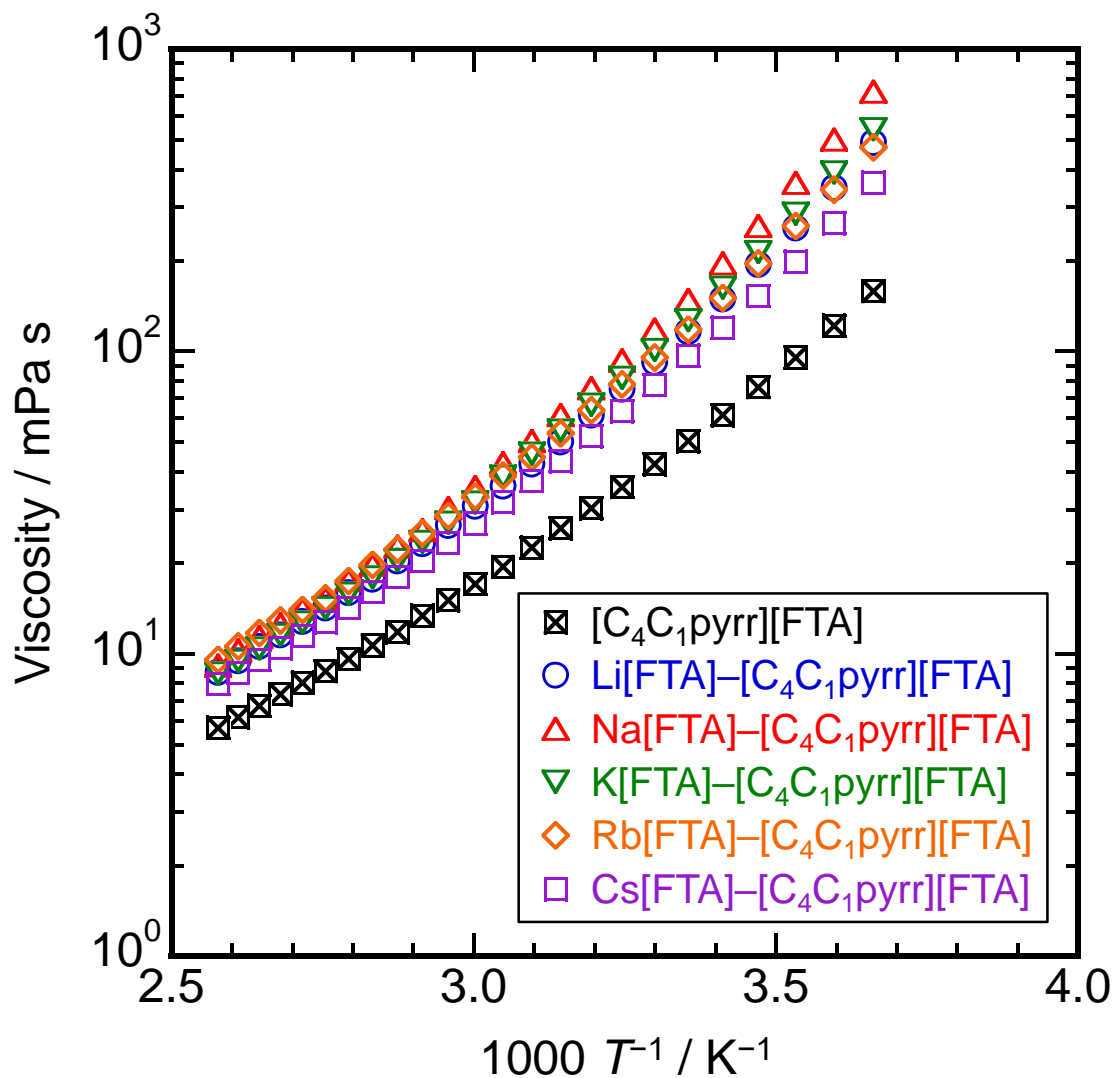


Fig. 2 Arrhenius plots of viscosities for $[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ and $\text{M}[\text{FTA}]-[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ ($x(\text{M}[\text{FTA}]) = 0.20$; $\text{M} = \text{Li}, \text{Na}, \text{K}, \text{Rb}, \text{Cs}$) ionic liquids.

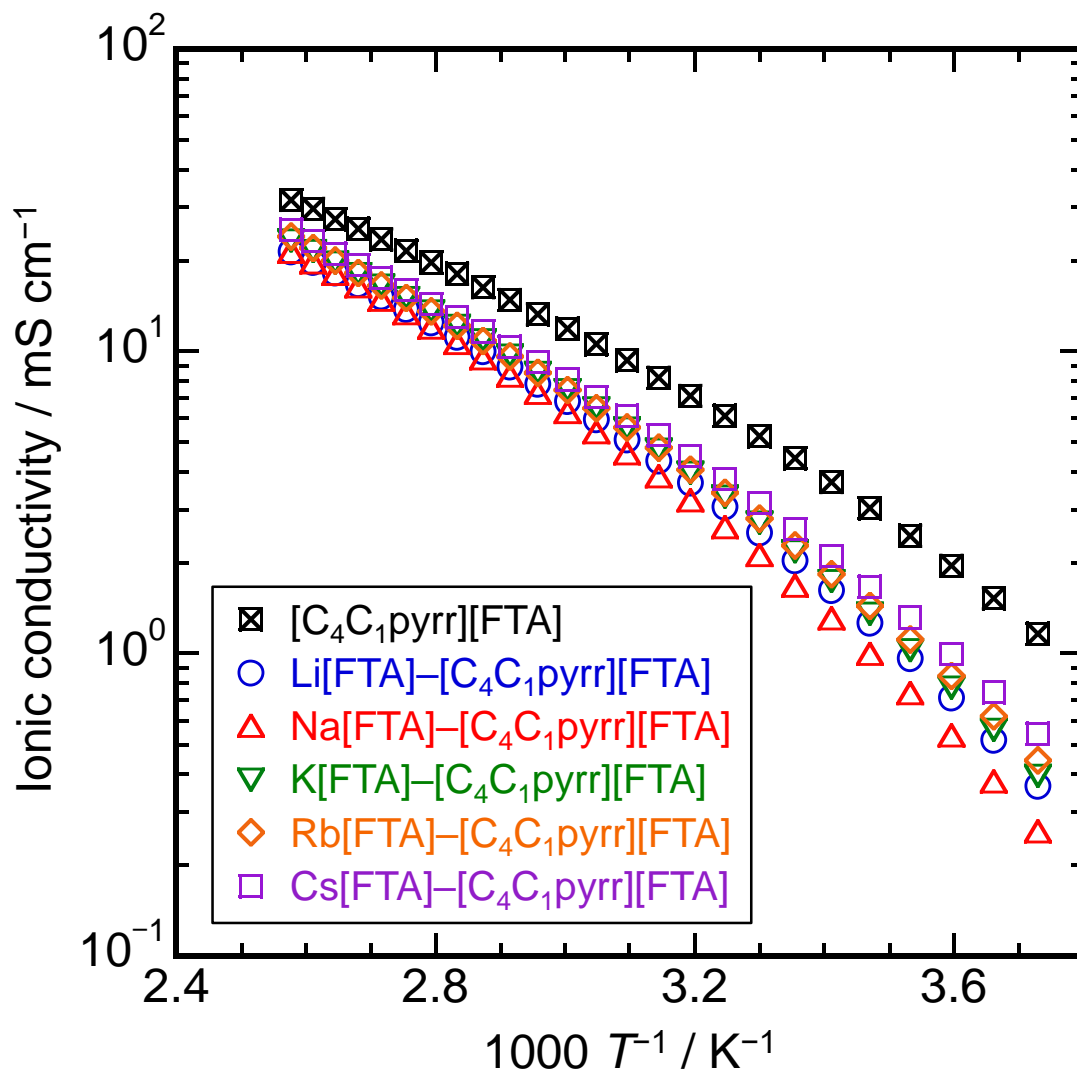


Fig. 3 Arrhenius plots of ionic conductivities for $[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ and $\text{M}[\text{FTA}]-[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ ($x(\text{M}[\text{FTA}]) = 0.20$; $\text{M} = \text{Li}, \text{Na}, \text{K}, \text{Rb}, \text{Cs}$) ionic liquids.

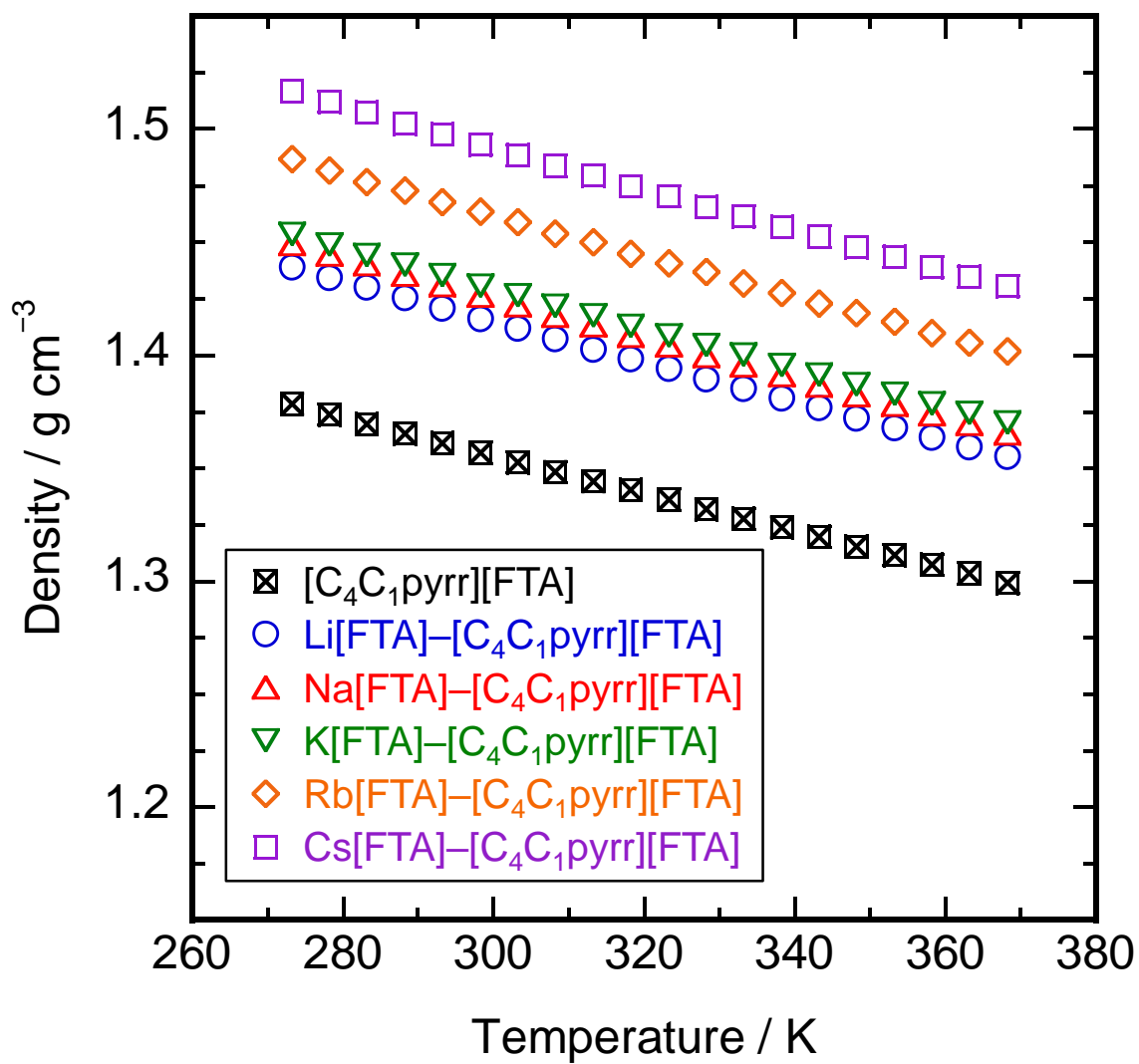


Fig. 4 Density plots of $[C_4C_1pyrr][FTA]$ and $M[FTA]-[C_4C_1pyrr][FTA]$ ($x(M[FTA]) = 0.20$; $M =$ Li, Na, K, Rb, Cs) ionic liquids.

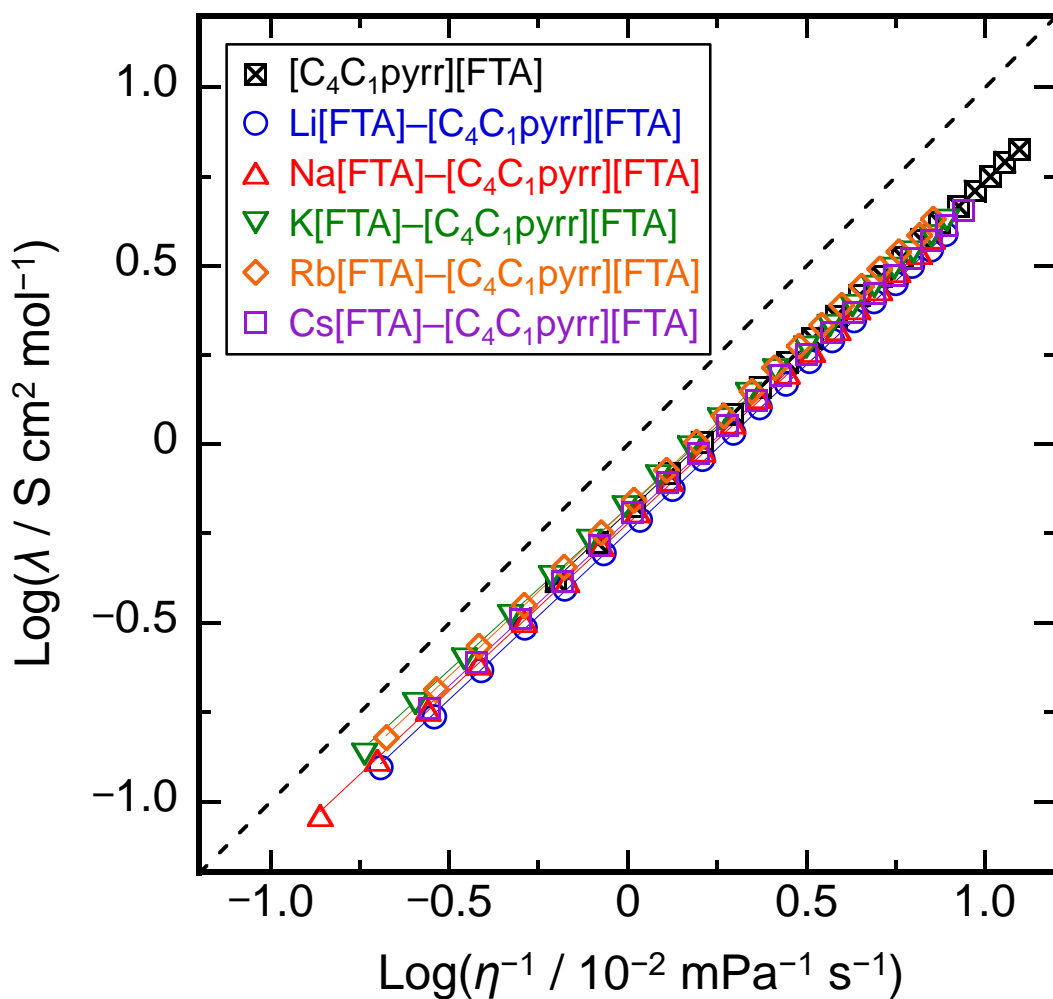


Fig. 5 Walden plots of $[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ and $\text{M}[\text{FTA}]-[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ ($x(\text{M}[\text{FTA}]) = 0.20$; $\text{M} = \text{Li}, \text{Na}, \text{K}, \text{Rb}, \text{Cs}$) ionic liquids. The ideal KCl line is indicated by a dashed line.

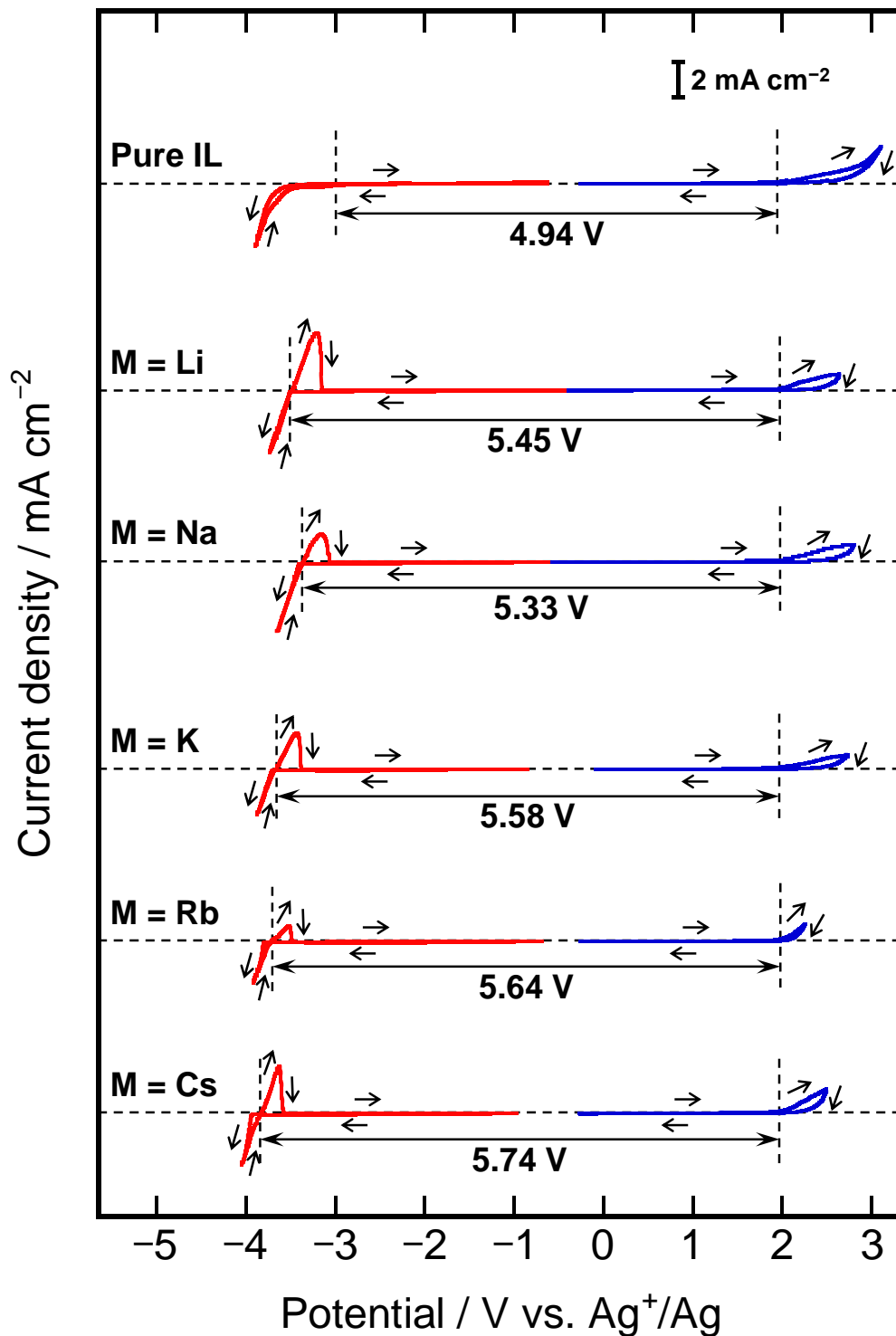


Fig. 6 Cyclic voltammograms of [C₄C₁pyrr][FTA] (Pure IL) and M[FTA]-[C₄C₁pyrr][FTA] ($x(\text{M[FTA]}) = 0.20$; M = Li, Na, K, Rb, Cs) ionic liquids (ILs) at 298 K. Working electrodes: Cu and glassy carbon disk (negative and positive potential regions, respectively). Scan rate: 5 mV s⁻¹. Cycle number: 1st. The cathodic and anodic limits of each electrolyte are indicated by vertical dashed lines. The zero-current density of each electrolyte is illustrated as a horizontal dashed line.

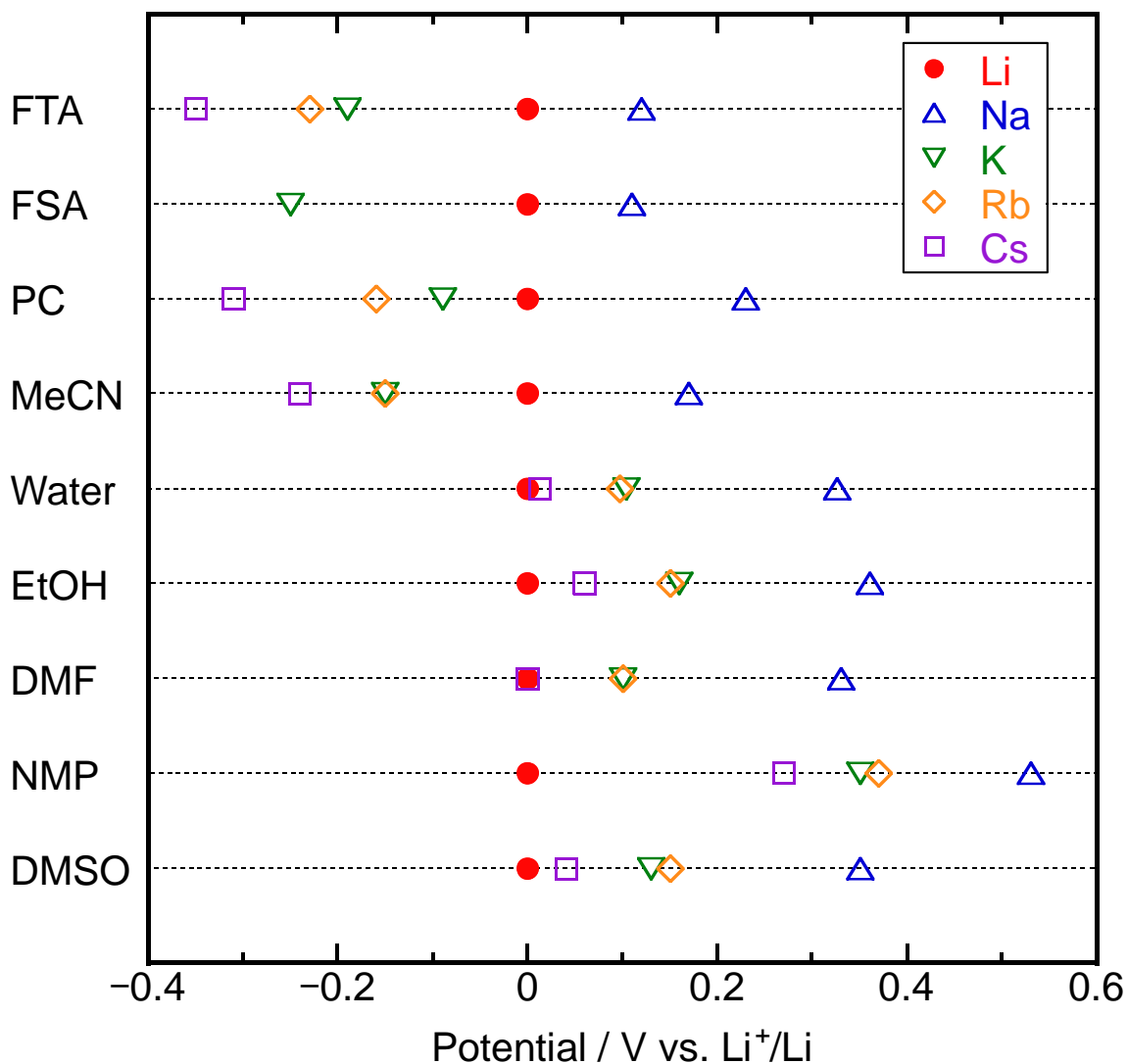
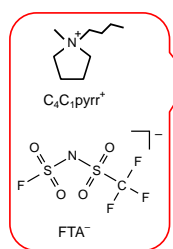
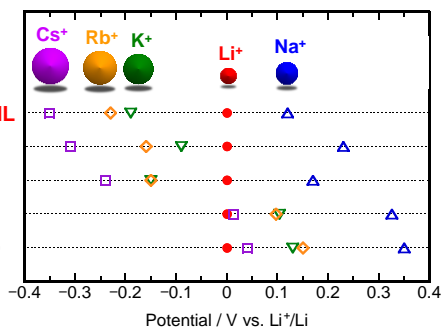


Fig. 7 Redox potentials of alkali metals ($E(M^+/M)$; M = alkali metal) in various electrolytes with respect to $E(\text{Li}^+/\text{Li})$. FTA = $\text{M}[\text{FTA}]-[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ ($C(\text{Li}^+) = 0.820 \text{ mol dm}^{-3}$, $C(\text{Na}^+) = 0.819 \text{ mol dm}^{-3}$, $C(\text{K}^+) = 0.814 \text{ mol dm}^{-3}$, $C(\text{Rb}^+) = 0.811 \text{ mol dm}^{-3}$, $C(\text{Cs}^+) = 0.806 \text{ mol dm}^{-3}$), FSA = $\text{M}[\text{FSA}]-[\text{C}_3\text{C}_1\text{pyrr}][\text{FSA}]$ ($C(\text{Li}^+) = 1.0 \text{ mol dm}^{-3}$,²⁸ $C(\text{Na}^+) = 0.98 \text{ mol dm}^{-3}$,²⁹ $C(\text{K}^+) = 0.98 \text{ mol dm}^{-3}$),² PC = propylene carbonate ($C(\text{M}^+) = 1 \text{ mol dm}^{-3}$), MeCN = acetonitrile ($C(\text{M}^+) = 1 \text{ mol dm}^{-3}$), EtOH = ethanol ($C(\text{M}^+) = 1 \text{ mol dm}^{-3}$), DMF = *N,N*-dimethylformamide ($C(\text{M}^+) = 1 \text{ mol dm}^{-3}$), NMP = *N*-methylpyrrolidone ($C(\text{M}^+) = 1 \text{ mol dm}^{-3}$), DMSO = dimethyl sulfoxide ($C(\text{M}^+) = 1 \text{ mol dm}^{-3}$).

TOC graphic



FTA-IL



Supporting Information

Comparative Study of $M[N(SO_2F)(SO_2CF_3)]-[N\text{-butyl-}N\text{-methylpyrrolidinium}][N(SO_2F)(SO_2CF_3)]$ ($M = Li, Na, K, Rb, Cs$) Ionic Liquid Electrolytes

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Table S1 Viscosities (mPa s) of [C₄C₁pyrr][FTA] (Pure IL) and M[FTA]–[C₄C₁pyrr][FTA] ionic liquids ($x(\text{M[FTA]}) = 0.20$; M = Li, Na, K, Rb, Cs).

<i>T</i> / K	Pure IL	M = Li	M = Na	M = K	M = Rb	M = Cs
273	159	492	729	547	476	362
278	122	349	505	393	345	266
283	96.0	258	364	287	261	200
288	76.6	195	262	214	196	153
293	62.0	150	196	164	151	120
298	51.0	117	149	128	119	97.4
303	42.7	92.5	119	102	96.3	77.7
308	35.9	75.1	94.2	82.2	78.2	63.5
313	30.4	61.8	76.0	66.9	64.2	52.6
318	26.1	50.6	61.9	55.2	54.0	43.7
323	22.5	42.7	50.9	46.1	44.9	37.4
328	19.5	36.1	42.9	38.7	38.9	31.7
333	17.1	31.0	35.9	31.8	33.2	27.0
338	15.1	26.7	30.4	27.2	28.7	23.4
343	13.4	23.3	25.8	23.5	25.2	20.4
348	11.9	20.4	22.7	20.5	22.2	18.0
353	10.7	17.8	19.8	18.0	19.8	16.1
358	9.7	16.0	17.6	15.9	17.5	14.2
363	8.8	14.2	15.3	14.2	15.3	12.8
368	8.0	12.9	14.1	12.8	14.0	11.5
373	7.4	11.6	12.6	11.6	13.0	10.5
378	6.8	10.6	11.4	10.5	11.8	9.6
383	6.2	9.5	10.3	9.5	10.6	8.7
388	5.7	8.7	9.2	8.7	9.6	8.0

Table S2 Ionic conductivities (mS cm^{-1}) of $[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ (Pure IL) and $\text{M}[\text{FTA}]-[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ ionic liquids ($x(\text{M}[\text{FTA}]) = 0.20$; $\text{M} = \text{Li, Na, K, Rb, Cs}$).

T / K	Pure IL	$\text{M} = \text{Li}$	$\text{M} = \text{Na}$	$\text{M} = \text{K}$	$\text{M} = \text{Rb}$	$\text{M} = \text{Cs}$
268	1.2	0.37	0.26	0.40	0.45	0.55
273	1.5	0.52	0.38	0.56	0.62	0.75
278	2.0	0.72	0.54	0.78	0.85	1.0
283	2.5	1.0	0.7	1.0	1.1	1.3
288	3.0	1.3	1.0	1.4	1.4	1.7
293	3.7	1.6	1.3	1.7	1.8	2.1
298	4.4	2.0	1.7	2.2	2.3	2.6
303	5.3	2.5	2.1	2.7	2.8	3.2
308	6.2	3.1	2.6	3.3	3.4	3.8
313	7.2	3.7	3.2	4.0	4.1	4.5
318	8.2	4.4	3.9	4.7	4.8	5.3
323	9.4	5.1	4.6	5.6	5.6	6.2
328	10.6	6.0	5.4	6.5	6.5	7.1
333	11.9	6.9	6.3	7.5	7.5	8.1
338	13.3	7.8	7.3	8.6	8.5	9.2
343	14.8	8.9	8.4	9.7	9.7	10.4
348	16.4	10.0	9.5	10.9	10.9	11.7
353	18.1	11.2	10.7	12.3	12.2	13.0
358	19.8	12.5	12.0	13.6	13.6	14.4
363	21.7	13.9	13.4	15.1	15.1	16.0
368	23.5	15.2	14.9	16.6	16.6	17.6
373	25.5	16.7	16.4	18.1	18.3	19.3
378	27.6	18.2	18.1	19.8	20.1	21.2
383	29.7	19.8	19.8	21.5	22.1	23.2
388	31.9	21.5	21.5	23.3	24.1	25.3

Table S3 Densities (g cm^{-3}) and their fitting parameters of $[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ (Pure IL) and $\text{M}[\text{FTA}]-[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ ionic liquids ($x(\text{M}[\text{FTA}]) = 0.20$; $\text{M} = \text{Li, Na, K, Rb, Cs}$).^a

T / K	Pure IL	$\text{M} = \text{Li}$	$\text{M} = \text{Na}$	$\text{M} = \text{K}$	$\text{M} = \text{Rb}$	$\text{M} = \text{Cs}$
273	1.379	1.439	1.449	1.454	1.487	1.517
278	1.374	1.435	1.445	1.449	1.482	1.512
283	1.370	1.430	1.440	1.445	1.477	1.508
288	1.366	1.426	1.436	1.440	1.473	1.503
293	1.361	1.421	1.431	1.436	1.468	1.498
298	1.357	1.416	1.427	1.431	1.464	1.494
303	1.353	1.412	1.422	1.427	1.459	1.489
308	1.349	1.407	1.418	1.422	1.454	1.484
313	1.345	1.403	1.413	1.418	1.450	1.480
318	1.340	1.399	1.409	1.414	1.445	1.475
323	1.336	1.394	1.404	1.409	1.441	1.471
328	1.332	1.390	1.400	1.405	1.437	1.466
333	1.328	1.385	1.396	1.400	1.432	1.462
338	1.324	1.381	1.391	1.396	1.428	1.457
343	1.320	1.377	1.387	1.392	1.423	1.453
348	1.316	1.373	1.383	1.388	1.419	1.448
353	1.312	1.368	1.378	1.383	1.415	1.444
358	1.308	1.364	1.374	1.379	1.410	1.439
363	1.304	1.360	1.370	1.375	1.406	1.435
368	1.300	1.356	1.366	1.371	1.402	1.431
$A_\rho \times 10^4$	-8.291	-8.811	-8.827	-8.777	-8.946	-9.103
B_ρ	1.605	1.679	1.690	1.693	1.730	1.765

^a Density values were fitted by the following equation; $\rho = A_\rho T + B_\rho$

Table S4 Molar concentrations (mol dm^{-3}) and their fitting parameters of alkali metal cations (M^+ ; $\text{M} = \text{Li, Na, K, Rb, Cs}$) in $\text{M}[\text{FTA}]-[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ ionic liquids ($x(\text{M}[\text{FTA}]) = 0.20$).^a

T / K	$\text{M} = \text{Li}$	$\text{M} = \text{Na}$	$\text{M} = \text{K}$	$\text{M} = \text{Rb}$	$\text{M} = \text{Cs}$
273	0.8336	0.8317	0.8267	0.8235	0.8189
278	0.8309	0.8290	0.8241	0.8210	0.8163
283	0.8282	0.8264	0.8215	0.8184	0.8137
288	0.8256	0.8238	0.8189	0.8158	0.8112
293	0.8229	0.8212	0.8163	0.8132	0.8086
298	0.8203	0.8186	0.8138	0.8107	0.8061
303	0.8177	0.8160	0.8112	0.8082	0.8036
308	0.8151	0.8134	0.8087	0.8057	0.8011
313	0.8125	0.8109	0.8062	0.8032	0.7987
318	0.8099	0.8083	0.8037	0.8007	0.7962
323	0.8074	0.8058	0.8012	0.7982	0.7937
328	0.8049	0.8033	0.7987	0.7957	0.7913
333	0.8023	0.8008	0.7962	0.7933	0.7889
338	0.7998	0.7983	0.7938	0.7909	0.7864
343	0.7974	0.7958	0.7913	0.7884	0.7840
348	0.7949	0.7933	0.7889	0.7860	0.7816
353	0.7924	0.7909	0.7865	0.7836	0.7793
358	0.7899	0.7884	0.7840	0.7812	0.7769
363	0.7875	0.7860	0.7816	0.7788	0.7745
368	0.7851	0.7836	0.7792	0.7764	0.7722
$A_C \times 10^4$	-5.103	-5.065	-4.990	-4.956	-4.913
B_C	0.9725	0.9697	0.9626	0.9585	0.9527

^a Molar concentration values were fitted by the following equation; $C(\text{M}^+) = A_C T + B_C$

Table S5 Molar ionic conductivities ($\text{S cm}^2 \text{mol}^{-1}$) of $[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ (Pure IL) and $\text{M}[\text{FTA}]-[\text{C}_4\text{C}_1\text{pyrr}][\text{FTA}]$ ionic liquids ($x(\text{M}[\text{FTA}]) = 0.20$; $\text{M} = \text{Li, Na, K, Rb, Cs}$).

T / K	Pure IL	$\text{M} = \text{Li}$	$\text{M} = \text{Na}$	$\text{M} = \text{K}$	$\text{M} = \text{Rb}$	$\text{M} = \text{Cs}$
273	0.41	0.12	0.091	0.14	0.15	0.18
278	0.53	0.17	0.13	0.19	0.21	0.25
283	0.67	0.23	0.18	0.25	0.27	0.32
288	0.83	0.31	0.24	0.33	0.36	0.41
293	1.01	0.39	0.32	0.43	0.45	0.52
298	1.22	0.50	0.41	0.54	0.57	0.65
303	1.45	0.62	0.52	0.67	0.70	0.79
308	1.70	0.75	0.65	0.82	0.85	0.95
313	1.98	0.91	0.80	0.99	1.02	1.13
318	2.29	1.08	0.96	1.18	1.20	1.33
323	2.62	1.27	1.15	1.39	1.41	1.55
328	2.97	1.48	1.35	1.63	1.64	1.80
333	3.35	1.71	1.58	1.88	1.89	2.06
338	3.75	1.96	1.83	2.16	2.16	2.34
343	4.19	2.23	2.10	2.46	2.46	2.65
348	4.64	2.52	2.40	2.78	2.77	2.98
353	5.13	2.83	2.71	3.12	3.11	3.34
358	5.64	3.16	3.05	3.48	3.48	3.72
363	6.19	3.52	3.42	3.86	3.87	4.12
368	6.74	3.87	3.80	4.27	4.28	4.55

Table S6 VTF parameters of viscosity and ionic conductivity, and α and C' ($= \log(\lambda\eta^\alpha)$) parameters for [C₄C₁pyrr][FTA] (Pure IL) and M[FTA]–[C₄C₁pyrr][FTA] ionic liquids ($x(\text{M[FTA]}) = 0.20$; M = Li, Na, K, Rb, Cs). Concerning the right column, the α and C' values correspond to the slopes and vertical intercepts of the Walden plots, and the B_σ/B_η values are calculated from the VTF fitting parameters.

	Viscosity			Ionic conductivity			Walden plot		
	$A_\eta \times 10^3$ / mPa s K ^{-1/2}	B_η / K	$T_{0\eta}$ / K	$A_\sigma \times 10^{-4}$ / mS cm ⁻¹ K ^{1/2}	B_σ / K	$T_{0\sigma}$ / K	α	B_σ/B_η	C' ($= \log(\lambda\eta^\alpha)$)
Pure IL	4.73	1040	137	2.79	958	136	0.93	0.92	-0.19
M = Li	6.74	977	157	2.08	900	157	0.94	0.92	-0.25
M = Na	5.98	1002	161	2.42	916	162	0.94	0.91	-0.22
M = K	8.56	927	161	1.99	852	162	0.91	0.92	-0.18
M = Rb	6.50	1029	151	2.82	973	151	0.94	0.95	-0.18
M = Cs	4.73	1086	144	3.12	1013	144	0.93	0.93	-0.21

Table S7 Summary of the redox potentials of M^+/M ($E(M^+/M)$; $M = \text{Li, Na, K, Rb, Cs}$) in various electrolytes at 298 K.

Electrolyte	$E(M^+/M) / \text{V vs. Ag}^+/\text{Ag}$					Ref.
	$E(\text{Li}^+/\text{Li})$	$E(\text{Na}^+/\text{Na})$	$E(\text{K}^+/\text{K})$	$E(\text{Rb}^+/\text{Rb})$	$E(\text{Cs}^+/\text{Cs})$	
M[FTA]– [C ₄ C ₁ pyrr][FTA]*	–3.48	–3.36	–3.67	–3.71	–3.83	This study
M[FSA]– [C ₃ C ₁ pyrr][FSA]**	–3.46	–3.35	–3.71	n/a	n/a	a
1 mol dm ^{–3} M ⁺ /PC	–3.78	–3.55	–3.87	–3.94	–4.09	b
1 mol dm ^{–3} M ⁺ /MeCN	–3.29	–3.12	–3.44	–3.44	–3.53	b
1 mol dm ^{–3} M ⁺ /Water	–3.839	–3.513	–3.735	–3.742	–3.826	b
1 mol dm ^{–3} M ⁺ /EtOH	–3.78	–3.42	–3.62	–3.63	–3.72	b
1 mol dm ^{–3} M ⁺ /DMF	–3.72	–3.39	–3.62	–3.62	–3.72	b
1 mol dm ^{–3} M ⁺ /NMP	–3.93	–3.40	–3.58	–3.56	–3.66	b
1 mol dm ^{–3} M ⁺ /DMSO	–3.64	–3.29	–3.51	–3.49	–3.60	b

PC = propylene carbonate, MeCN = acetonitrile, EtOH = ethanol, DMF = *N,N*-dimethylformamide, NMP = *N*-methylpyrrolidone, DMSO = dimethyl sulfoxide

* Values of M[FTA]–[C₄C₁pyrr][FTA] were measured at the molar concentration of M[FTA] of 0.820 mol dm^{–3} for Li[FTA], 0.819 mol dm^{–3} for Na[FTA], 0.814 mol dm^{–3} for K[FTA], 0.811 mol dm^{–3} for Rb[FTA], 0.806 mol dm^{–3} for Cs[FTA].

** Values of M[FSA]–[C₃C₁pyrr][FSA] were measured at the molar concentration of M[FSA] of 1.0 mol dm^{–3} for Li[FSA],^c 0.98 mol dm^{–3} for Na[FSA],^d and 0.98 mol dm^{–3} for K[FSA].^a

- (a) Yamamoto, T.; Matsumoto, K.; Hagiwara, R.; Nohira, T. Physicochemical and Electrochemical Properties of K[N(SO₂F)₂]–[N-Methyl-N-propylpyrrolidinium][N(SO₂F)₂] Ionic Liquids for Potassium-Ion Batteries. *J. Phys. Chem. C* **2017**, *121*, 18450–18458.
- (b) Marcus, Y. Thermodynamic Functions of Transfer of Single Ions from Water to Nonaqueous and Mixed Solvents, PART 3: Standard Potentials of Selected Electrodes. *Pure Appl. Chem.* **1985**, *57*, 1129–1132.
- (c) Yoon, H.; Best, A. S.; Forsyth, M.; MacFarlane, D. R.; Howlett, P. C. Physical properties of high Li-ion content *N*-propyl-*N*-methylpyrrolidinium bis(fluorosulfonyl)imide based ionic liquid electrolytes. *Phys. Chem. Chem. Phys.* **2015**, *17*, 4656–4663.
- (d) Matsumoto, K.; Okamoto, Y.; Nohira, T.; Hagiwara, R. Thermal and Transport Properties of Na[N(SO₂F)₂]–[N-Methyl-N-propylpyrrolidinium][N(SO₂F)₂] Ionic Liquids for Na Secondary Batteries. *J. Phys. Chem. C* **2015**, *119*, 7648–7655.

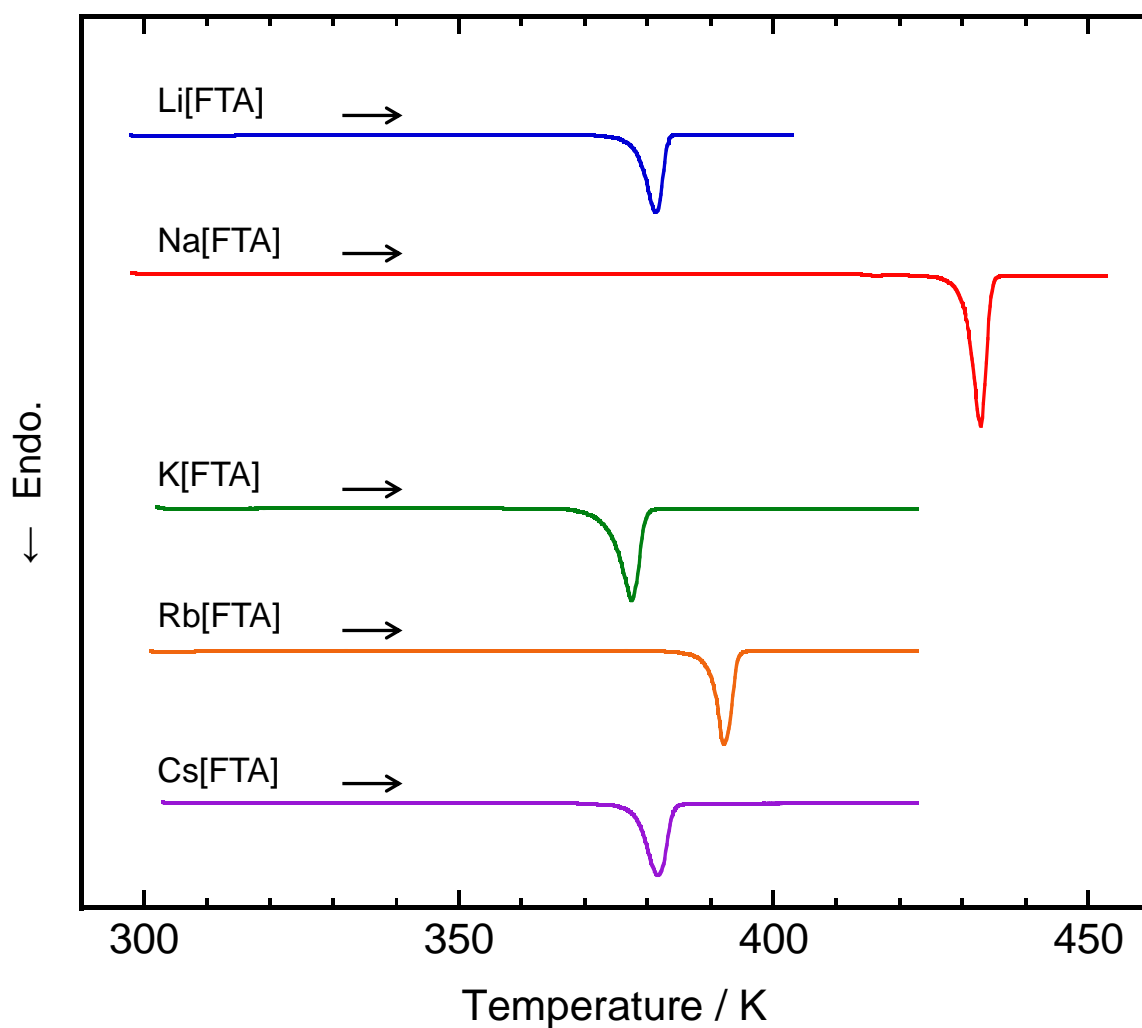


Fig. S1 DSC curves of M[FTA] salts (M = Li, Na, K, Rb, Cs). Scan rate: 2 K min⁻¹.

The onset and end temperatures of melting are found to be 378 and 383 K for Li[FTA], 430 and 435 K for Na[FTA], 373 and 380 K for K[FTA], 390 and 395 K for Rb[FTA], and 378 and 384 K for Cs[FTA], respectively. These results are almost consistent with the previous report.^e

The small deviations might be attributed to the difference of the measurement conditions.

(e) Kubota, K.; Nohira, T.; Hagiwara, R.; Matsumoto, H. Thermal Properties of Alkali (Fluorosulfonyl)(trifluoromethylsulfonyl)amides. *Chem. Lett.* **2010**, *39*, 1303–1304.