# Studies on the Oxidation of Pyrite <br> (Part 2) Kinetics of the Oxidation of Pyrite 

## By

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#### Abstract

The kinetics of the oxidation of pyrite in the atmosphere of the mixed gas of $\mathrm{O}_{2}, \mathrm{SO}_{2}$ and $\mathrm{N}_{2}$ was studied. The results obtained were summarized as follows: 1. At $700^{\circ} \sim 900^{\circ} \mathrm{C}$ where the thermal decomposition of pyrite proceeds quickly, the reaction occurs in two stages, the initial one is of the thermal decomposition of pyrite and the final one is of the oxidation of the thermal decomposition product, $\mathrm{FeS}_{1+x}$. This phenomenon is more obvious at lower partial pressure of oxygen. The rate constant of the oxidation of $\mathrm{FeS}_{1+x}$ was found to be proportional to the partial pressure of oxygen, and the activation energy of this reaction was determined to be about 8.3 kcal . 2. At $550^{\circ} \sim 650^{\circ} \mathrm{C}$, the thermal decomposition of pyrite proceeds slowly and, as a result, the following three reactions occur simultaneously, $$
\begin{aligned} & \mathrm{FeS}_{2}=\mathrm{FeS}_{1+x}+(1-x) / 2 \mathrm{~S}_{2}(\mathrm{~g}) \\ & \left.\mathrm{FeS}_{1+x}+(7 / 2)+2 x\right) \mathrm{O}_{2}=1 / 2 \mathrm{Fe}_{2} \mathrm{O}_{3}+(1+x) \mathrm{SO}_{2} \\ & \mathrm{FeS}_{2}+11 / 4 \mathrm{O}_{2}=1 / 2 \mathrm{Fe}_{2} \mathrm{O}_{3}+2 \mathrm{SO}_{2} \end{aligned}
$$


For the mol fraction of $x, y$ and $z$ respectively for $\mathrm{FeS}_{2}, \mathrm{FeS}_{1+x}$ and $\mathrm{Fe}_{2} \mathrm{O}_{3}$, the simultaneous differential equations were brought out and they were solved approximately.

We defined also the ratio of weight decrease $w$ and it was shown as a function of time $t$ by applying the solutions of the above equations. From the expression of this $w$, the rate constant of the direct oxidation of pyrite, $k_{3}$, was obtained. This rate constant, $k_{3}$, was also found to be proportional to the partial pressure of oxygen and its activation energy to be about 11.9 kcal .
3. The change of mol fraction $x, y$ and $z$ along the oxidation was computed. From
this computation, the amount of $\mathrm{FeS}_{1+x}$ formed as an intermediate product of the reaction was found to be dependent on the temperature of oxidation and the partial pressure of oxygen.
4. The calculated ratio of weight decrease $w$ coincides considerably with the observed values at lower temperatures of the oxidation, but the coincidence is not good at higher temperatures.

Since the thermal decomposition proceeds very quickly at higher temperatures, the following assumptions on the reactions fit better than the simultaneous progress of the three reactions mentioned above;
a) at the initial stage, the thermal decomposition proceeds preferentially and $\mathrm{FeS}_{1+x}$ is formed, and
b) toward the end of the thermal decomposition, the oxidation of $\mathrm{FeS}_{1+x}$ commences, followed by the decomposition.

## 1. Introduction

Studies on the mechanism of oxidation of pyrite is important for the efficient production of sulphuric acid, for researches on the recovery of valuable metal components in the pyrite cinder and for smelting of sulphide minerals. In this report (Part 2), researches on the kinetics of the oxidation of pyrite between $550^{\circ}$ and $900^{\circ} \mathrm{C}$ are described.

## 2. Premises on the atmosphere in the roasters

In the oxidizing roasting of pyrite with air, the partial pressure of oxygen gradually decreases and the partial pressure of sulphur dioxide increases along with the progress of the oxidation.

Assuming that the oxidation of pyrite can be expressed by

$$
\mathrm{FeS}_{2}+11 / 4 \mathrm{O}_{2}=1 / 2 \mathrm{Fe}_{2} \mathrm{O}_{3}+2 \mathrm{SO}_{2}
$$

then, for 1 mol of $\mathrm{FeS}_{2}$,
volume of $\mathrm{O}_{2}$ combined with S is $22.4 \times 2=44.8(l)$ and
volume of $\mathrm{O}_{2}$ combined with Fe is $22.4 \times 3 / 4=16.8(l)$.
Therefore,
the total volume of $\mathrm{O}_{2}$ required for the oxidation is

$$
22.4 \times 11 / 4=61.6(l)
$$

Now, assuming further that, when 1 mol of $\mathrm{FeS}_{2}$ is oxidized with $a(l)$ of air (where $a \geq 61.6 / 0.201(l)$ ), a gas, whose concentration of oxygen is $x(\%)$ and that of sulphur dioxide is $y(\%)$, is generated, we have the following equations,

$$
\begin{aligned}
& 44.8 /(a-16.8)=y / 100 \\
& (0.208 a-61.6) /(a-16.8)=x / 100
\end{aligned}
$$

Hence,

$$
\begin{equation*}
931.8-58.1 y=44.8 x \tag{1}
\end{equation*}
$$

In similar way, the following relations between $x$ and $y$ are derived;
for $\mathrm{FeS}_{2}+\mathrm{O}_{2}=\mathrm{FeS}+\mathrm{SO}_{2}$,

$$
\begin{equation*}
20.8-y=x \tag{2}
\end{equation*}
$$

for $\mathrm{FeS}_{2}+8 / 3 \mathrm{O}_{2}=1 / 3 \mathrm{Fe}_{3} \mathrm{O}_{4}+2 \mathrm{SO}_{2}$,

$$
\begin{equation*}
931.8-35.7 y=22.4 x \tag{3}
\end{equation*}
$$

and for $\mathrm{FeS}+7 / 4 \mathrm{O}_{2}=1 / 2 \mathrm{Fe}_{2} \mathrm{O}_{3}+\mathrm{SO}_{2}$,

$$
\begin{equation*}
465.9-35.7 y=22.4 x \tag{4}
\end{equation*}
$$

Eqs. (1) $\sim(4)$ are indicated by the straight lines in the $\mathrm{O}_{2}-\mathrm{SO}_{2}-\mathrm{N}_{2}$ triangular diagram of Fig. 1. The observed composition of the gas in the multiple hearths furnaces ${ }^{1)}$ when pyrite is roasted are also plotted in this figure. It is found that these observed values are biased and scattered in the lower part of the lines of Eqs.


Fig. 1.
(1)~(4). This bias of the observed values is considered to be caused by (a) formation of $\mathrm{SO}_{3}$ by the reaction of $\mathrm{SO}_{2}+1 / 2 \mathrm{O}_{2}=\mathrm{SO}_{3}$ in addition to the above reactions of the oxidation, (b) presence of $\mathrm{H}_{2} \mathrm{O}$ due to the moisture of air and the ore ${ }^{2)}$, (c) difficulties in sampling of gas under negative pressure, and so forth.

When the gas in the roaster is assumed to be the mixture of $\mathrm{O}_{2}, \mathrm{SO}_{2}$ and $\mathrm{N}_{2}$, the composition of the gas changes with the progress of the oxidation, from the composition of $20.8 \% \mathrm{O}_{2}$ and $79.2 \% \mathrm{~N}_{2}$ (air) upwards along the lines in Fig. 1.

In the ordinary roaster of pyrite, the thermal decomposition of pyrite is considered to occur preferentially in the initial stage of roasting and the final product of the oxidation is assumed to be $\mathrm{Fe}_{2} \mathrm{O}_{3}$. Therefore, in the roaster of counter-current type, such as the Herreshoff furnace in which air and the ore move in the inverse direction, it is supposed that the composition of the gas changes initially along the line of $\mathrm{FeS}+7 / 4 \mathrm{O}_{2}=1 / 2 \mathrm{Fe}_{2} \mathrm{O}_{3}+\mathrm{SO}_{2}$ moving upwards from left to right, and at a certain point where the thermal decomposition of pyrite ceases, the composition leaves off the line and it moves along the line of $\mathrm{FeS}_{2}+11 / 4 \mathrm{O}_{2}=1 / 2 \mathrm{Fe}_{2} \mathrm{O}_{3}+2 \mathrm{SO}_{2}$. Further, in the roasters of co-current type such as the flash-roasters in which air and the ore move in the same direction, the change of the composition of the gas is supposed to be followed by the line of $\mathrm{FeS}_{2}+\mathrm{O}_{2}=\mathrm{FeS}+\mathrm{SO}_{2}$ in the initial stage of the oxidation, to be followed by the line of $\mathrm{FeS}_{2}+11 / 4 \mathrm{O}_{2}=1 / 2 \mathrm{Fe}_{2} \mathrm{O}_{3}+2 \mathrm{SO}_{2}$ in the final stage.

However, it is impossible to fix a point in Fig. 1, where the composition of gas transits from one line to the other because this point varies according to various roasting conditions. Moreover, by the oxidation in the roasters, $\mathrm{Fe}_{3} \mathrm{O}_{4}, \mathrm{FeSO}_{4}$ and others are formed besides $\mathrm{Fe}_{2} \mathrm{O}_{3}$. Therefore, the circumstances vary somewhat from the abovementioned considerations. In our study the composition of the gas was assumed to change along the line of $\mathrm{FeS}_{2}+11 / 4 \mathrm{O}_{2}=1 / 2 \mathrm{Fe}_{2} \mathrm{O}_{3}+2 \mathrm{SO}_{2}$ for the most part. By this assumption, the following compositions of the gas shown in Table 1 were obtained by Eq. (1). In the studies hereafter, the oxidation of pyrite in the atmosphere of these compositions was investigated.

Table 1.

| $\mathrm{O}_{2}$ <br> $(\%)$ | $\mathrm{SO}_{2}$ <br> $(\%)$ | $\mathrm{N}_{2}$ <br> $(\%)$ |
| :---: | :---: | :---: |
| 20.8 | 0 | 79.2 |
| 15 | 4 | 81 |
| 10 | 8 | 28 |
| 5 | 12 | 83 |
| 3 | 14 | 83 |
| 1 | 15 | 84 |

## 3. The oxidation of pyrite at $700^{\circ} \sim 900^{\circ} \mathrm{C}$

The thermal decomposition of pyrite proceeds rapidly above $700^{\circ} \mathrm{C}$. At this temperature of $700^{\circ} \sim 900^{\circ} \mathrm{C}$, the weight change of the sample by the oxidation was measured with the thermobalance of the previous report ${ }^{3}$. The conditions of the measurements were as follows;
weight of sample; 400 mg ,
particle size of the sample; 200~250 mesh,
composition of gas mixture; mixed gas of $\mathrm{O}_{2}, \mathrm{SO}_{2}$ and $\mathrm{N}_{2}$ whose composition was shown in Table 1.
rate of flow of gas; $200 \mathrm{cc} / \mathrm{min}$..
Results were shown in Fig. 2, 3 and 4. A knick point of the weight change curve was found in the oxidation at the low partial pressure of oxygen. This means that the reaction occurs in two stages, separately. That is, the rapid decrease of the weight in the initial stage of the reaction is due mainly to the thermal decomposition and the comparatively slow decrease that follows it is due to the oxidation of $\mathrm{FeS}_{1+x}$ which is a product of the thermal decomposition. This reaction of the oxidation of $\mathrm{FeS}_{1+x}$ is written by the following equation;

$$
\mathrm{FeS}_{1+x}+(7 / 2+2 x) \mathrm{O}_{2}=1 / 2 \mathrm{Fe}_{2} \mathrm{O}_{3}+(1+x) \mathrm{SO}_{2}
$$



Fig. 2.


Fig. 3.


Fig. 4.
On the reaction of this kind, G.-M. Schwab ${ }^{4)}$ suggested the following equation of the reaction kinetics;

$$
-d y / d t=k_{2} y^{\frac{1}{2}}
$$

where $y$ is the mol fraction of $\mathrm{FeS}_{1+x}$ at time $t$, and $k_{2}$ is the rate constant of the reaction. Thence we obtain,

$$
1-y^{\frac{1}{2}}=k_{2} t / 2
$$

using the initial condition of $y=1$ at $t=0$.
A good linearity was obtained between $\left(1-y^{\frac{1}{2}}\right)$, which were computed from Figs. $2 \sim 4$, and time $t$. The rate constants $k_{2}$ were obtained from the slope of these lines. The relation between the rate constant $k_{2}$ thus obtained and the partial pressure of oxygen in the atmosphere, $p_{2}$ is shown in Fig. 5. As is clear from this figure, $k_{2}$ is found to be proportional to the partial pressure of oxygen. However, at a low partial




Fig. 5.
pressure of oxygen, especially at 0.01 atm . of oxygen, this proportionality does not exist, and the values of $k_{2}$ deviate somewhat from these lines. This is considered to be caused by the formation of $\mathrm{Fe}_{3} \mathrm{O}_{4}$ as an intermediate product by the following reaction,

$$
\begin{aligned}
& \mathrm{FeS}_{1+x}+2 / 3 \mathrm{SO}_{2}=1 / 3 \mathrm{Fe}_{3} \mathrm{O}_{4} \\
& \quad+(5 / 6+x / 2) \mathrm{S}_{2}(\mathrm{~g}) .
\end{aligned}
$$

This formation of $\mathrm{Fe}_{3} \mathrm{O}_{4}$ as an intermediate product will be discussed later in Part 3.

The logarithms of the rate constants $k_{2}$ were shown in Fig. 6, plotted against the reciprocals of the absolute temperature. Almost equal values of the slopes of these lines were obtained independently of the partial pressure of oxygen. An activation energy of 8.3 kcal


Fig. 6. was obtained for the reaction by Ergun's method of computation ${ }^{55}$, and this goes to show that this value is apparently attributable to the diffusion phenomenon.

## 4. The oxidation of pyrite at $550^{\circ} \sim 650^{\circ} \mathrm{C}$

At the temperature of $550^{\circ} \mathrm{C}, 600^{\circ} \mathrm{C}$ and $650^{\circ} \mathrm{C}$, the weight change of the sample due to the oxidation was measured with the thermobalance. The conditions of the measurements were same as in 3. The results obtained are shown in Fig. 7, 8 and 9. In the curves of weight change of these figures, the knicks as observed in the oxidation at higher temperature were not found.

Above $700^{\circ} \mathrm{C}$, the thermal decomposition of pyrite proceeds very quickly and, consequently, the rate constants of the oxidation of $\mathrm{FeS}_{1+x}, k_{2}$, could be determined with considerable precision. On the other hand, at the temperature of between $550^{\circ} \mathrm{C}$ and $650^{\circ} \mathrm{C}$ where the direct sulphatization of pyrite can be neglected, the rate of the thermal decomposition becomes relatively small and, therefore, the direct oxidation of pyrite, which has remained undecomposed, occurs simultaneously with the thermal decomposition and the oxidation of $\mathrm{FeS}_{1+x}$, which is the product of the thermal


|  |  | $\mathrm{O}_{2}$ | $\mathrm{SO}_{2}$ | $\mathrm{~N}_{2}$ |
| :---: | :---: | :---: | :---: | :---: |
|  |  | $(\%)$ | $(\%)$ | $(\%)$ |
| Curve (1) |  | 20.8 | 0 | 79.2 |
| $"$ | $(2)$ | 15 | 4 | 81 |
| $"$ | $(3)$ | 10 | 8 | 82 |
| $"$ | $(4)$ | 5 | 12 | 83 |
| $"$ | $(5)$ | 3 | 14 | 83 |
| $"$ | $(6)$ | 1 | 15 | 84 |

Fig. 7.


|  |  | $\mathrm{O}_{2}$ | $\mathrm{SO}_{2}$ | $\mathrm{~N}_{2}$ |
| :---: | :---: | :---: | :---: | :---: |
|  |  | $(\%)$ | $(\%)$ | $(\%)$ |
| Curve (1) |  | 20.8 | 0 | 79.2 |
| $"$ | $(2)$ | 15 | 4 | 81 |
| $"$ | $(3)$ | 10 | 8 | 82 |
| $"$ | $(4)$ | 5 | 12 | 83 |
| $"$ | $(5)$ | 3 | 14 | 83 |
| $"$ | $(6)$ | 1 | 15 | 84 |

Fig. 8.


|  |  | $\mathrm{O}_{2}$ | $\mathrm{SO}_{2}$ | $\mathrm{~N}_{2}$ |
| :---: | :---: | :---: | :---: | :---: |
|  |  | $(\%)$ | $(\%)$ | $(\%)$ |
| Curve (1) |  | 20.8 | 0 | 79.2 |
| $"$ | $(2)$ | 15 | 4 | 81 |
| $"$ | $(3)$ | 10 | 8 | 82 |
| $"$ | $(4)$ | 5 | 12 | 83 |
| $"$ | $(5)$ | 3 | 14 | 83 |
| $"$ | $(6)$ | 1 | 15 | 84 |

Fig. 9.
decomposition. Eventually, the following three reactions occur simultaneously at this temperature range of $550^{\circ} \sim 650^{\circ} \mathrm{C}$;

$$
\begin{align*}
& \mathrm{FeS}_{2}=\mathrm{FeS}_{1+x}+(1-x) / 2 \mathrm{~S}_{2}(\mathrm{~g})  \tag{6}\\
& \mathrm{FeS}_{1+x}+(7 / 2+2 x) \mathrm{O}_{2}=1 / 2 \mathrm{Fe}_{2} \mathrm{O}_{3}+(1+x) \mathrm{SO}_{2}  \tag{7}\\
& \mathrm{FeS}_{2}+11 / 4 \mathrm{O}_{2}=1 / 2 \mathrm{Fe}_{2} \mathrm{O}_{3}+2 \mathrm{SO}_{2} \tag{8}
\end{align*}
$$

and
If we assume concerning these reactions that the thermal decomposition is followed by the equation of the first order reaction ${ }^{3)}$ and the oxidation of $\mathrm{FeS}_{1+x}$ and $\mathrm{FeS}_{2}$ is followed by the empirical equation of Eq. (4) suggested by G.-M. Schwab, we then have the following simultaneous differential equations for the change of the mol fraction of $\mathrm{FeS}_{2}, \mathrm{FeS}_{1+x}$ and $1 / 2 \mathrm{Fe}_{2} \mathrm{O}_{3}$,

$$
\begin{align*}
-\frac{d x}{d t} & =k_{1} x+k_{3} x^{\frac{1}{2}}  \tag{9}\\
\frac{d y}{d t} & =k_{1} x-k_{2} y^{\frac{1}{2}}  \tag{10}\\
\frac{d z}{d t} & =k_{2} y^{\frac{1}{2}}+k_{3} x^{\frac{1}{2}} \tag{11}
\end{align*}
$$

where
$x$ : mol fraction of $\mathrm{FeS}_{2}$ at time $t$,
$y: \quad, \quad, \quad$ of $\mathrm{FeS}_{1+x}$ at time $t$,
$z: \quad, \quad, \quad$ of $1 / 2 \mathrm{Fe}_{2} \mathrm{O}_{3}$ at time $t$,
$k_{1}$ : the rate constant of the reaction (6),
$\begin{array}{lllll}k_{2}: & " & " & " & \text { (7) and } \\ k_{3}: & " & " & " & (8) .\end{array}$
The following conditions exist with the mol fraction $x, y$ and $z$;
(a) $x=1$ and $y, z=0$ at $t=0$, and $x, y=0$ and $z=1$ at $t \rightarrow \infty$,
(b) from Eqs. (9), (10) and (11),
$\frac{d}{d t}(x+y+z)=0, \quad$ thereafter, $x+y+z=$ const. $=1$,
(c) $x \geqq 0, y \geq 0$ and $z \geqq 0$.

These simultaneous differential equations can be solved approximately as follows.
At first, from Eq. (9), we obtain,

$$
\frac{d u}{d t}=-\frac{1}{2}\left(k_{1} u+k_{3}\right)
$$

where $x=u^{2}$. Hence
where

$$
\begin{gathered}
u=1-(1+\mu)\left(1-e^{-\frac{k_{1} t}{2}}\right)=1-(1+\mu) T^{2} \\
k_{3} / k_{1}=\mu \quad \text { and } \quad 1-e^{-\frac{k_{1} t}{2}}=T^{2}
\end{gathered}
$$

Then we have,

$$
\begin{equation*}
x=u^{2}=\left\{1-(1+\mu) T^{2}\right\}^{2} \tag{12}
\end{equation*}
$$

When $u=x^{\frac{1}{2}}=0$ in Eq. (12),

$$
T^{2}=\frac{1}{1+\mu}
$$

or

$$
t=-\frac{2}{k_{1}} \ln \frac{\mu}{1+\mu}=t_{0}
$$

That is, when $t=t_{0}, x$ becomes zero. Or, in other words, for

$$
\begin{align*}
0<t<t_{0}=-\frac{2}{k_{1}} \ln \frac{\mu}{1+\mu} \\
x=\left\{1-(1+\mu) T^{2}\right\}^{2} . \tag{13}
\end{align*}
$$

Subsequently, from Eq. (10), we obtain,

$$
\begin{equation*}
2 v \frac{d v}{d t}=k_{1} x-k_{2} v \tag{14}
\end{equation*}
$$

where $y=v^{2}$.
On the other hand, since $\frac{d T}{d t}=\frac{k_{1}}{4} \frac{\left(1-T^{2}\right)}{T}$ by the differentiation of $1-e^{-\frac{k_{1} t}{2}}=T^{2}$, we can write

$$
\begin{aligned}
& 2 v \frac{d v}{d t}=2 v \frac{d v}{d T} \frac{d T}{d t} \\
& \quad=\frac{k_{1}}{2} \frac{\left(1-T^{2}\right)}{T} v \frac{d v}{d T} .
\end{aligned}
$$

Here, we express $v$ as a power series of $T$ as follows,

$$
v=a_{1} T+a_{2} T^{2}+a_{3} T^{3}+\cdots .
$$

then

$$
\begin{aligned}
v \frac{d v}{d T} & =\left(a_{1} T+a_{2} T^{2}+a_{3} T^{3}+\cdots\right)\left(a_{1}+2 a_{2} T+3 a_{3} T^{2}+\cdots\right) \\
& =\sum_{N=1,3}, \cdots(N+1)\left(a_{1} a_{N}+a_{2} a_{N-1}+\cdots+a_{\frac{N-1}{2}} a_{\frac{N+3}{2}}+\frac{1}{2} a_{\frac{N+1}{2}}^{2}\right) T^{N} \\
& +\sum_{N=2,4, \cdots}(N+1)\left(a_{1} a_{N}+a_{2} a_{N-1}+\cdots+a_{\frac{N}{2}} a_{\frac{N}{2}+1}\right) T^{N} .
\end{aligned}
$$

Substituting Eq. (13) and above equations of $v$ and $v \frac{d v}{d t}$ in Eq. (14), we obtain,

$$
\begin{aligned}
& \sum_{N=1,3}(N+1)\left(a_{1} a_{N}+a_{2} a_{N-1}+\cdots+a_{\frac{N-1}{2}} \frac{a_{N+3}}{2}+\frac{1}{2} a_{\frac{N+1}{2}}^{2}\right)\left(T^{N-1}-T^{N+1}\right) \\
& +\sum_{N=2,4}(N+1)\left(a_{1} a_{N}+a_{2} a_{N-1}+\cdots+a_{\frac{N}{2}} \frac{a_{\frac{N}{2}+1}}{2}\right)\left(T^{N-1-} T^{N+1}\right) \\
& =2\left\{1-(1+\mu) T^{2}\right\}^{2}-2 \nu\left(a_{1} T+a_{2} T^{2}+a_{3} T^{3}+\cdots\right) .
\end{aligned}
$$

where

$$
k_{2} / k_{1}=\nu
$$

By rearranging the above equation, we have

$$
\begin{aligned}
& a_{1}{ }^{2}\left(1-T^{2}\right)+4\left(a_{1} a_{3}+\frac{1}{2} a_{2}{ }^{2}\right)\left(T^{2}-T^{4}\right)+6\left(a_{1} a_{5}+a_{2} a_{4}+\frac{1}{2} a_{3}{ }^{2}\right)\left(T^{4}-T^{6}\right)+\cdots \\
& +3 a_{1} a_{2}\left(T-T^{3}\right)+5\left(a_{1} a_{4}+a_{2} a_{3}\right)\left(T^{3}-T^{5}\right)+7\left(a_{1} a_{6}+a_{2} a_{5}+a_{3} a_{4}\right)\left(T^{5}-T^{7}\right)+\cdots \\
& =2\left\{1-2(1+\mu) T^{2}+(1+\mu)^{2} T^{4}\right\}-2 \nu\left(a_{1} T+a_{2} T^{2}+a_{3} T^{3}+\cdots\right) .
\end{aligned}
$$

The coefficients of the $T^{i}$ terms of both sides of the equation are compared and $a_{1}$, $a_{2}, \cdots a_{5}$ are obtained as follows;

$$
\begin{aligned}
& a_{1}=\sqrt{2} \\
& a_{2}=-\frac{2}{3} \nu \\
& a_{3}=\frac{\sqrt{2}}{2}\left(\frac{\nu^{2}}{9}-\frac{1}{2}-\mu\right) \\
& a_{4}=\frac{2}{15} \nu\left(\frac{\nu^{2}}{9}-\frac{7}{2}-\mu\right) \\
& a_{5}=\frac{\sqrt{2}}{2}\left\{\frac{1}{12} \mu^{2}+\frac{1}{6} \mu\left(\frac{1}{15} \nu^{2}-\frac{3}{2}\right)-\frac{1}{16}+\frac{17}{180} \nu^{2}+\frac{1}{540} \nu^{4}\right\}
\end{aligned}
$$

For $N \geqq 6, a_{N}$ are represented by the following general expression,
$N$ : odd

$$
\begin{aligned}
a_{N}=\frac{1}{(N+1) a_{1}}\{ & (N-1)\left(a_{1} a_{N-2}+a_{2} a_{N-3}+\cdots+\frac{1}{2} a_{\frac{N-1}{2}}^{2}\right) \\
& \left.-(N+1)\left(a_{2} a_{N-1}+a_{3} a_{N-2}+\cdots+\frac{1}{2} a_{\frac{N+1}{2}}^{2}\right)-2 \nu a_{N-1}\right\}
\end{aligned}
$$

$N$ : even

$$
\begin{aligned}
a_{N}=\frac{1}{(N+1) a_{1}}\{ & (N-1)\left(a_{1} a_{N-2}+a_{2} a_{N-3}+\cdots+a_{\frac{N}{2}-1} a_{\frac{N}{2}}\right) \\
& \left.-(N+1)\left(a_{2} a_{N-1}+a_{3} a_{N-2}+\cdots+a_{\frac{N}{2}} a_{\frac{N}{2}+1}\right)-2 \nu a_{N-1}\right\} .
\end{aligned}
$$

Then using $a_{i}$, thus obtained, in $y^{\frac{1}{2}}=v=a_{1} T+a_{2} T^{2}+\cdots$, we have,

$$
\begin{align*}
y^{\frac{1}{2}}=v= & \sqrt{2} T-\frac{2}{3} \nu T^{2}+\frac{\sqrt{2}}{2}\left(\frac{\nu^{2}}{9}-\frac{1}{2}-\mu\right) T^{3}-\frac{2}{15} \nu\left(\mu+\frac{7}{2}-\frac{\nu^{2}}{9}\right) T^{4} \\
& +\frac{\sqrt{2}}{2}\left\{\frac{1}{12} \mu^{2}+\frac{1}{6} \mu\left(\frac{1}{15} \nu^{2}-\frac{3}{2}\right)-\frac{1}{16}+\frac{17}{180} \nu^{2}+\frac{1}{540} \nu^{4}\right\} T^{5}+\cdots . \tag{15}
\end{align*}
$$

As shown above, at $t=t_{0}=-\frac{2}{k_{1}} \ln \frac{\mu}{1+\mu}$ where $x=0, T^{2}=1 /(1+\mu)$. Therefore, from Eq. (15), $v\left(=v_{0}\right)$ and $y\left(=y_{0}\right)$ at $t=t_{0}$ are,

$$
\begin{aligned}
y_{0}^{\frac{1}{2}}=v_{0} & =\left(\frac{2}{1+\mu}\right)^{\frac{1}{2}}-\frac{2}{3} \frac{\nu}{(1+\mu)}+\frac{\sqrt{2}}{2}\left(\frac{\nu^{2}}{9}-\frac{1}{2}-\mu\right) \frac{1}{(1+\mu)^{\frac{3}{2}}}-\frac{2}{15} \nu\left(\mu+\frac{7}{2}-\frac{\nu^{2}}{9}\right) \frac{1}{(1+\mu)^{2}} \\
& +\frac{\sqrt{2}}{2}\left\{\frac{1}{12} \mu^{2}+\frac{1}{6} \mu\left(\frac{1}{15} \nu^{2}-\frac{3}{2}\right)-\frac{1}{16}+\frac{17}{180} \nu^{2}+\frac{1}{540} \nu^{4}\right\} \frac{1}{(1+\mu)^{\frac{5}{2}}}+\cdots
\end{aligned}
$$

As $x=0$, at $t=t_{0}$, from Eq. (10), we have,

$$
\frac{d y}{d t}=k_{2} y^{\frac{1}{2}}
$$

Hence,

$$
v=y_{0}^{\frac{1}{2}}-\frac{k_{2}}{2}\left(t-t_{0}\right)
$$

where $y=v^{2}$. From $y=0$ in the above equation, we obtain,

$$
t-t_{0}=\frac{2}{k_{2}} y_{0}^{\frac{1}{2}}=t_{1}
$$

Therefore at $t=t_{0}+t_{1}, y=0$.
In summary, for $0<t<t_{0}$, Eq. (25) is fitted, and
for $t_{0}<t<t_{0}+t_{1}=2\left(\frac{1}{k_{2}} y_{0}^{\frac{7}{2}}-\frac{1}{k_{1}} \ln \frac{\mu}{1+\mu}\right)$

$$
\begin{equation*}
y^{\frac{1}{2}}=v=y_{0}^{\frac{1}{2}}-\frac{k_{2}}{2}\left(t-t_{0}\right) \tag{16}
\end{equation*}
$$

These above-mentioned solutions of the simultaneous differential equations of Eq. (9) $\sim(11)$ are summarized in Table 2.

Now, we define the ratio of weight decrease of the sample by the reactions, $w^{6}$, as follows;

$$
\begin{equation*}
w=\frac{W_{0}-W_{t}}{W_{\mathrm{FeS}_{2}}} \tag{17}
\end{equation*}
$$

where $W_{0}$ : initial weight of the sample
$W_{t}$ : weight of the sample at time $t$
$W_{\mathrm{FeS}_{2}}$ : weight of $\mathrm{FeS}_{2}$ component in the initial sample.
On the other hand, $w$ is also represented as follows,

$$
\begin{equation*}
w=\frac{M_{x}-\left(x M_{x}+y M_{y}+z M_{z}\right)}{M_{x}} \tag{18}
\end{equation*}
$$

where $M_{x}$ : molecular weight of $\mathrm{FeS}_{2}$

$$
\begin{array}{lll}
M_{y}: & " & , \\
M_{z}: & " & \text { of } \mathrm{FeS}_{1+x} \\
& , \quad \text { of } 1 / 2 \mathrm{Fe}_{2} \mathrm{O}_{3}
\end{array}
$$

and $x, y$ and $z$ are the mol fractions of $\mathrm{FeS}_{2}, \mathrm{FeS}_{1+x}$ and $1 / 2 \mathrm{Fe}_{2} \mathrm{O}_{3}$ at time $t$, respectively.
From Eq. (18), we have

$$
w=y m_{y}+z m_{z}
$$

where $m_{y}=1-M_{y} / M_{x}$, and $m_{z}=1-M_{z} / M_{x}$.

Table 2.

$$
\begin{aligned}
& t=0 \quad x=1, y=0, z=0 \\
& 0<t<t_{0} \quad x=\left\{1-(1+\mu) T^{2}\right\}^{2} \\
& y=\left[\sqrt{2} T-\frac{2}{3} \nu T^{2}+\frac{\sqrt{2}}{2}\left(\frac{\nu^{2}}{9}-\frac{1}{2}-\mu\right) T^{3}-\frac{2}{15} \nu\left(\mu+\frac{7}{2}-\frac{\nu^{2}}{9}\right) T^{4}\right. \\
& \left.+\frac{\sqrt{2}}{2}\left\{\frac{1}{12} \mu^{2}+\frac{1}{6} \mu\left(\frac{1}{15} \nu^{2}-\frac{3}{2}\right)-\frac{1}{16}+\frac{17}{180} \nu^{2}+\frac{1}{540} \nu^{4}\right\} T^{5}+\cdots\right]^{2} \\
& z=1-(x+y) \\
& t=t_{0}=-\frac{2}{k_{1}} \ln \frac{\mu}{1+\mu} \\
& x=0 \\
& y=y_{0}=\left[\left(\frac{2}{1+\mu}\right)^{\frac{1}{2}}-\frac{2}{3} \frac{\nu}{(1+\mu)}+\frac{\sqrt{2}}{2}\left(\frac{\nu^{2}}{9}-\frac{1}{2}-\mu\right) \frac{1}{(1+\mu)^{3 / 2}}-\frac{2}{15} \nu\left(\mu+\frac{7}{2}-\frac{\nu^{2}}{9}\right) \frac{1}{(1+\mu)^{2}}\right. \\
& \left.+\frac{\sqrt{2}}{2}\left\{\frac{1}{12} \mu^{2}+\frac{1}{6} \mu\left(\frac{1}{15} \nu^{2}-\frac{3}{2}\right)-\frac{1}{16}+\frac{17}{180} \nu^{2}+\frac{1}{540} \nu^{4}\right\} \frac{1}{(1+\mu)^{5 / 2}}+\cdots\right]^{2} \\
& z=1-y_{0} \\
& t_{0}<t<t_{0}+t_{1} \\
& x=0 \\
& y=\left\{y_{0}{ }^{\frac{1}{2}}-\frac{k_{2}}{2}\left(t-t_{0}\right)\right\}^{2} \\
& z=1-y \\
& t \geqq t_{0}+t_{1}=2\left(\frac{y_{0} \frac{1}{2}}{k_{2}}-\frac{1}{k_{1}} \ln \frac{\mu}{1+\mu}\right) \\
& x=0, y=0, z=1 \\
& \text { where } \quad \mu=\frac{k_{3}}{k_{1}}, \mu=\frac{k_{2}}{k_{1}} \text { and } T^{2}=1-e^{-\frac{k_{1} t}{2}}
\end{aligned}
$$

With the condition, $x+y+z=1, z$ is eliminated from the above expression as follows, for $0<t<t_{0}$

$$
w=m_{z}(1-x)+\left(m_{y}-m_{y}\right) y
$$

In this expression of $w$, Eqs. (13) and (15) are substituted, and we have

$$
\begin{align*}
w & =2\left(m_{y}+m_{z} \mu\right) T^{2}+\frac{4 \sqrt{2}}{3} \nu\left(m_{y}-m_{z}\right) T^{3} \\
& +\left\{m_{y}\left(\frac{2}{3} \nu^{2}-1-2 \mu\right)-m_{z}\left(\mu^{2}+\frac{2}{3} \nu^{2}\right)\right\} T^{4}  \tag{19}\\
& -\frac{2 \sqrt{2}}{15} \nu\left(m_{y}-m_{z}\right)\left(\frac{\nu^{2}}{3}-\frac{9}{2}-3 \mu\right) T^{5}+\cdots
\end{align*}
$$

Because in Eq. (19), the terms of higher order can be neglected when $t$ tends to become zero, $w$ can then be approximated by the following expression,

$$
\begin{equation*}
w \fallingdotseq 2\left(m_{y}+m_{z} \mu\right) T^{2} \tag{20}
\end{equation*}
$$

The observed values of $w$ computed from the results of the measurements are shown in Figs. $10 \sim 12$, plotted against $T^{2}$. The slope of the tangents of these curves drawn at the origin gives $2\left(m_{y}+m_{z} \mu\right)$ of Eq. (20). As $m_{y}$ and $m_{z}$ can be obtained from the molecular weight of $\mathrm{FeS}_{2}, \mathrm{FeS}_{1+x}$ and $\mathrm{Fe}_{2} \mathrm{O}_{3}$, and $\mu$ is the ratio of $k_{3} / k_{1}$ of which $k_{1}$ is already known, we are able to compute $k_{3}$, the rate constant of the reaction (8).
$k_{3}$ thus obtained, was plotted in Fig. 13, against the partial pressure of oxygen, $p_{O_{2}}$ (atm.). From this figure, it was found that $k_{3}$ was nearly proportional to $p_{O_{2}}$, as in the case of $k_{2}$ in 3.

In Fig. 14, the logarithms of $k_{3}$ were plotted against the reciprocals of the absolute temperature. Calculating by Ergun's method, an activation energy of 11.9 kcal was obtained for the reaction (8). This value of the activation energy is attributable to the diffusion phenomenon.


Fig. 10.


Fig. 11.


Fig. 12.


Fig. 13.


Fig. 14.

## 5. Change of the mol fraction of $\mathrm{FeS}_{2}, \mathrm{FeS}_{1+x}$ and $\mathrm{Fe}_{2} \mathrm{O}_{3}$ by the oxidation

Previously, the rate constant $k_{1}$ of the thermal decomposition of pyrite was determined in Part $1^{3}$. Now, the rate constants of the oxidation of $\mathrm{FeS}_{1+x}$ and $\mathrm{FeS}_{2}, k_{2}$ and $k_{3}$ respectively, were obtained in the preceding sections. The logarithms of these rate constants were summarized in Fig. 15 against the reciprocals of the absolute


Fig. 15.
temperature. In this figure, the thick lines represent the values at the temperature where the measurements were made, and they are prolonged toward both sides with thin broken lines. Further, for the lines of $k_{2}$ and $k_{3}$, the common value of the slopes calculated with Ergun's method were adopted, and their intercepts were obtained on the assumption of the proportionality of the rate constants to the partial pressure of oxygen.

On the presumptions that the reactions in the atmosphere of the mixed gas of $\mathrm{O}_{2}, \mathrm{SO}_{2}$ and $\mathrm{N}_{2}$ at $600^{\circ} \sim 800^{\circ} \mathrm{C}$ proceed according to the reactions (6), (7) and (8), and that the values determined in Fig. 15 can be used as the rate constants of these
reactions, the change of the mol fraction of $\mathrm{FeS}_{2}, \mathrm{FeS}_{1+x}$ and $\mathrm{Fe}_{2} \mathrm{O}_{3}$ can be computed with the equations of Table 2. Of the solution of Table 2, $y$ and $z$ were approximate solutions, therefore, in the compution of $y$, the terms below $T^{7}$ were employed and those of higher order were omitted. The results obtained are shown in Fig. 16, 17, 18 and 19.


Fig. 16.


Fig. 17.


Fig. 18.


Fig. 19.

From these results of computation, it was shown that at a fixed partial pressure of oxygen, the amount of $\mathrm{FeS}_{1+x}$ formed was larger when the temperature was higher and that, at a fixed temperature, it was also larger when the partial pressure of oxygen is lower. The maximum values of the computed mol fraction of $\mathrm{FeS}_{1+x}$ formed in the oxidation, $y_{\text {max }}$, are shown in Fig. 20.


Fig. 20.

## 6. The ratio of weight decrease $\boldsymbol{w}$

The ratio of weight decrease by the reactions of oxidation is shown as a function of $t$ in Eq. (19). Among the constants in this equation, $k_{1}, k_{2}, k_{3}$ could be determined from the results of Fig. 15, and $M_{x}, M_{y}, M_{z}$ from the molecular weight of the reaction components.

Or, in another way, $w$ can be computed from the equation,

$$
w=m_{z}(1-x)+\left(m_{y}-m_{z}\right) y
$$

using the results of computation of $x$ and $y$ in the previous section.
In these two ways of determination, $M_{x}$ and $M_{z}$ can be obtained immediately from the chemical formula of $\mathrm{FeS}_{2}$ and $\mathrm{Fe}_{2} \mathrm{O}_{3}$. However, the molecular weight, $M_{y}$, of $\mathrm{FeS}_{1+x}$ varies after the coefficient $(1+x)$ of the formula. Since it was conceivable from the results of Part $1^{3)}$ that the composition of $\mathrm{FeS}_{1+\boldsymbol{x}}$ formed in the intermediate stage of the oxidation is near the upper limit of solubility of sulphur in $\mathrm{FeS}_{1+x}$, the formula of $\mathrm{FeS}_{1.14}$ was used in the computation of the molecular weight.

The calculated values, $w_{\text {calc., }}$, and the observed values, $w_{\text {obs. }}$, which were measured with the thermobalance are shown in Fig. 21, 22, 23 and 24. The coincidence of both values was found fairly good in the case of $600^{\circ} \mathrm{C}$ and $650^{\circ} \mathrm{C}$, but at higher temperatures, for example of $700^{\circ} \mathrm{C}$ or $800^{\circ} \mathrm{C}$, they do not coincide well. At such a temperature as $800^{\circ} \mathrm{C}$, the thermal decomposition proceeds so quickly that the reaction may


Fig. 21.


Fig. 22.


Fig. 23.


Fig. 24.
be considered to occur in the following two separate stages rather than in the simultaneous progress of the reactions of (6), (7) and (8);
a) in the initial stage, the thermal decomposition proceeds very quickly and $\mathrm{FeS}_{1+x}$ is formed, and
b) toward the end of the thermal decomposition, the oxidation of $\mathrm{FeS}_{1+x}$ commences, followed by the decomposition.

After this assumption, we have the following differential equations in place of the Eqs. (9)~(11).
a) for $0<t<t_{0}$

$$
x+y=1, z=0, \text { and } x ; 1 \rightarrow 0.01, y ; 0 \rightarrow 0.99
$$

$$
\begin{equation*}
-\frac{d x}{d t}=k_{1} x, \quad \frac{d y}{d t}=k_{1} x \tag{21}
\end{equation*}
$$

b) for $t_{0}<t<t_{0}+t_{1}$

$$
x=0, y+z=1, \text { and } y ; 0.99 \rightarrow 0, z ; 0 \rightarrow 1
$$

$$
\begin{equation*}
-\frac{d y}{d t}=k_{2} y^{\frac{1}{2}}, \frac{d z}{d t}=k_{2} y^{\frac{1}{2}} . \tag{22}
\end{equation*}
$$

In these equations, the initial stage of the reaction was assumed to be the stage of decrement of the mol fraction of $\mathrm{FeS}_{2}$ from 1 to 0.01 .

From Eqs. (21) and (22), we obtain,

$$
t=0,
$$

$$
x=1, \quad y=0, \quad z=0
$$

$0<t<t_{0}$

$$
x=e^{-k_{1} t}, \quad y=1-e^{-k_{1} t}, \quad z=0
$$

$t=t_{0}=-\ln \frac{0.01}{k_{1}}$

$$
x=0.01, \quad y=0.99, \quad z=0
$$

$t_{0}<t<t_{0}+t_{1}$

$$
x=0, \quad y=\left\{1-\frac{k_{2}}{2}\left(t-t_{0}\right)\right\}^{2}, \quad z=1-y
$$

$t=t_{0}+t_{1}$

$$
x=0, \quad y=0, \quad z=1
$$

$t_{0}+t_{1}<t$

$$
x=0, \quad y=0, \quad z=1 .
$$

$w$ was computed with this solution, and $w_{\text {calc., }}^{\prime}$, thus obtained was also plotted in Fig. 24 with the dot-dash line. They coincide better with the observed values, $w_{\text {obs. }}$, than the calculated values, $w_{\text {calc. }}$, of $w$ from the Eqs. (9) $\sim(11)$.

## 7. Summary

Studies were carried out on the kinetics of the oxidation of pyrite in the atmosphere of the mixed gas of $\mathrm{O}_{2}, \mathrm{SO}_{2}$ and $\mathrm{N}_{2}$. The results obtained were summarized as follows.

1. At $700^{\circ} \sim 900^{\circ} \mathrm{C}$ where the thermal decomposition of pyrite proceeds quickly, a knick point was observed in the curve of weight change by the oxidation measured with the thermobalance. This knick point was more obvious at lower partial pressure of oxygen. The reaction occurred separately in two stages, and the initial stage was the thermal decomposition of pyrite and the final stage was the oxidation of the thermal decomposition product, $\mathrm{FeS}_{1+x}$.

With the empirical equation of the reaction kinetics suggested by G.--M. Schwab, the rate constant of the oxidation of $\mathrm{FeS}_{1+x}$, was calculated. This rate constant, $k_{2}$, was found to be proportional to the partial pressure of oxygen. The activation energy of this reaction was almost constant independent of the partial pressure of oxygen, and it was determined to be about 8.3 kcal .
2. At $550^{\circ} \sim 650^{\circ} \mathrm{C}$, the thermal decomposition of pyrite proceeds slowly and, as a result, the following three reactions are considered to proceed simultaneously;

$$
\begin{aligned}
& \mathrm{FeS}_{2}=\mathrm{FeS}_{1+x}+(1-x) / 2 \mathrm{~S}_{2}(\mathrm{~g}) \\
& \mathrm{FeS}_{1+x}+(7 / 2+2 x) \mathrm{O}_{2}=1 / 2 \mathrm{Fe}_{2} \mathrm{O}_{3}+(1+x) \mathrm{SO}_{2} \text { and } \\
& \mathrm{FeS}_{2}+11 / 4 \mathrm{O}_{2}=1 / 2 \mathrm{Fe}_{2} \mathrm{O}_{3}+2 \mathrm{SO}_{2}
\end{aligned}
$$

Of these three reactions, it is assumed that the thermal decomposition of pyrite is followed by the equation of first order reaction, and the oxidation of $\mathrm{FeS}_{1+x}$ and $\mathrm{FeS}_{2}$ is followed by the empirical equation suggested by G.-M. Schwab. On these assumptions, we formulated the simultaneous differential equations on the mol fraction of $\mathrm{FeS}_{2}, \mathrm{FeS}_{1+x}$ and $\mathrm{Fe}_{2} \mathrm{O}_{3}$ and obtained the approximate solutions, in which the mol fractions, $x, y$ and $z$ were shown as a function of time $t$. Further, with the relations between these mol fractions and the ratio of weight decrease, $w$ was also shown as a function of time $t$. From the slope of the tangents drawn at the origin in the diagram of observed $w$ vs. $T^{2}\left(=1-e^{-\frac{k_{1} t}{2}}\right)$, the rate constant $k_{3}$ of the following reaction was obtained ;

$$
\mathrm{FeS}_{2}+11 / 4 \mathrm{O}_{2}=1 / 2 \mathrm{Fe}_{2} \mathrm{O}_{3}+2 \mathrm{SO}_{2} .
$$

This rate constant, $k_{3}$, was also found to be proportional to the partial pressure of oxygen. An activation energy of about 11.9 kcal was obtained for this reaction.
3. The rate constant of the thermal decomposition of pyrite, $k_{1}$, the rate constant of the oxidation of $\mathrm{FeS}_{1+x}, k_{2}$ and the rate constant of the oxidation of $\mathrm{FeS}_{2}$, $k_{3}$ were substituted in the solutions of the above-mentioned simultaneous differential
equations, and the change of the mol fraction of $\mathrm{FeS}_{2}, \mathrm{FeS}_{1+x}$ and $\mathrm{Fe}_{2} \mathrm{O}_{3}$ along the oxidation was calculated. The results of computation showed that the amount of $\mathrm{FeS}_{1+x}$ formed at the intermediate stage of the oxidation became larger at higher temperatures when the partial pressure of oxygen was fixed, and that it became larger at lower partial pressures of oxygen when the temperature was fixed.
4. The ratio of weight decrease $w$ was shown as a function of time $t$, and it was compared with the observed values measured with the thermobalance. At the temperature of $600^{\circ} \mathrm{C}$ and $650^{\circ} \mathrm{C}$, both values coincided considerably, but at higher temperatures, their coincidence was not good.

At such a high temperature as $800^{\circ} \mathrm{C}$, the following assumptions fit in better with the results of the measurements than the simultaneous progress of the above-mentioned three reactions;
a) in the initial stage of the reaction, the thermal decomposition proceeds very quickly and $\mathrm{FeS}_{1+x}$ is formed, and
b) toward the end of the thermal decomposition, the oxidation of $\mathrm{FeS}_{1+x}$ commences, followed by the decomposition.

## References

1) These observed values were cited from the roasting tests in the multiple hearths furnaces. (K. Nishihara and Y. Kondo, Mem. of Faculty of Eng., Kyoto Univ., 14, 145, (1952).)
2) H. H. Kellogg, J. of Metals, 8, Tr. AIME, 1105, (1956).
3) K. Nishihara and Y. Kondo, Mem. of Faculty of Eng., Kyoto Univ., 20, 285 (1958).
4) G.-M. Schwab and J. Philinis, J. Am. Chem. Soc., 69, 2588, (1947).
5) S. Ergun, Ind. and Eng. Chem., 48, 2063, (1956).
6) K. Niwa et al, J. Japan Inst. of Metals, 18, 1, (1954).
